

Chapter 3 Polymer Solutions

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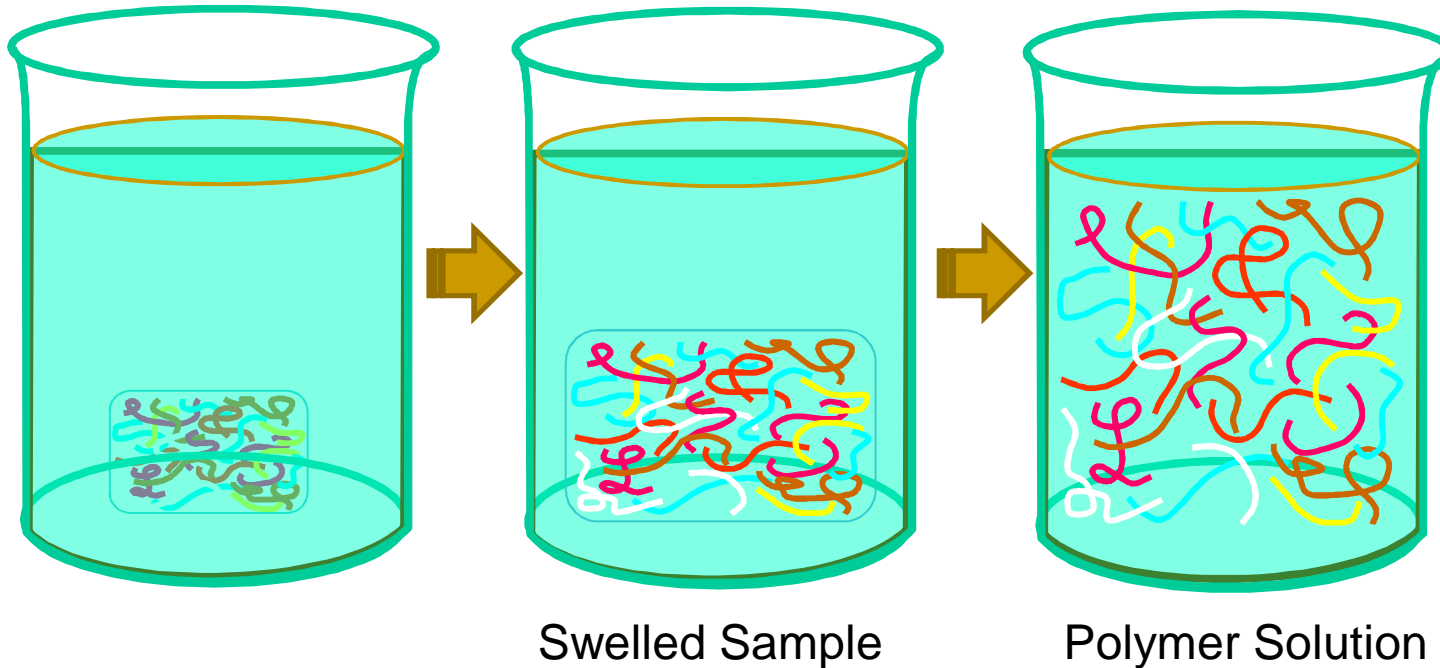
3.7 Thermodynamics of Gels

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3.9 Hydrodynamics of Polymer Solutions

Chapt. 3 Polymer Solutions

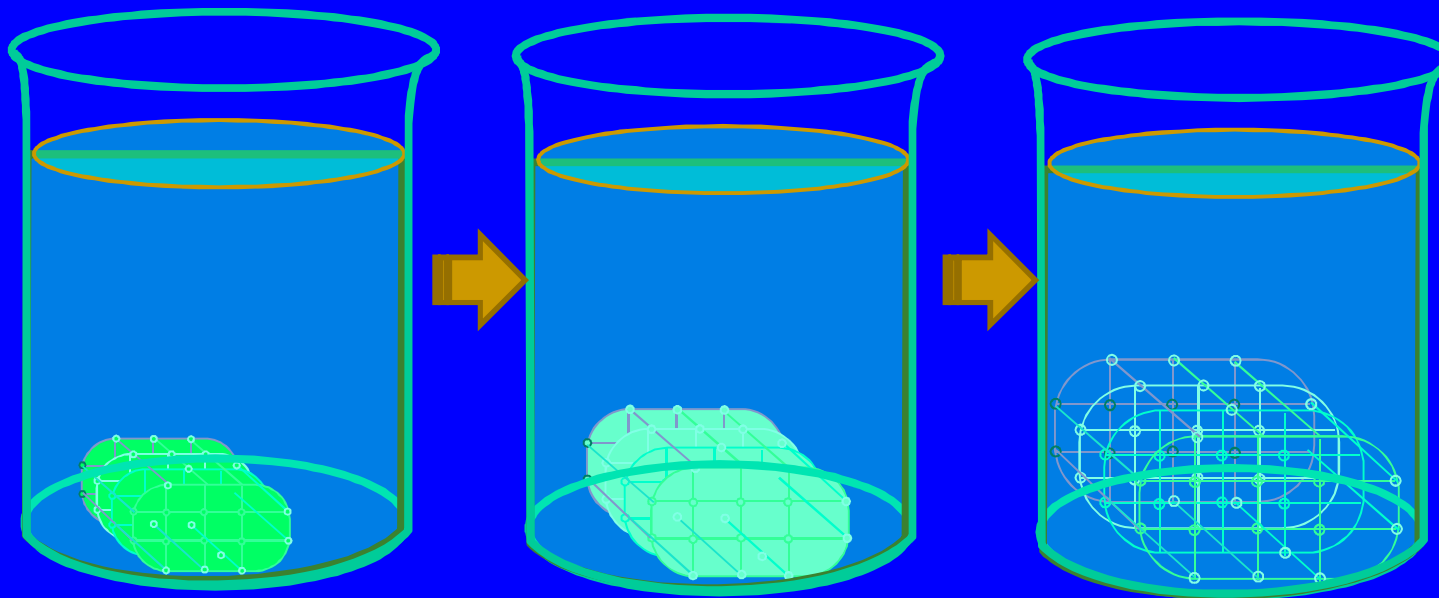
➤ The solution process (linear Polymer)



- This process is usually slower compared with small molecules, and strongly dependent on the chemical structures and condensed states of the samples.

先溶胀，后溶解

Crosslinked polymers: only can be swelled

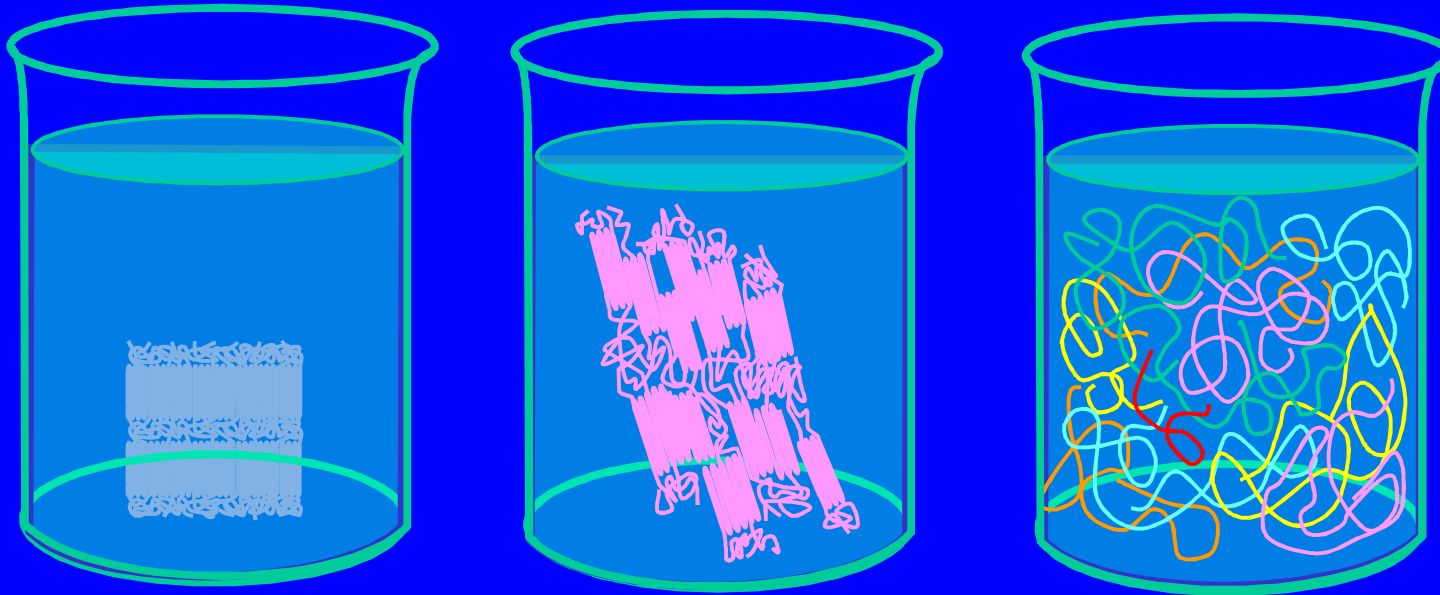


有溶胀，无溶解

Crystalline polymers

Crystalline PE: dissolve at the temperature approached to its melting temperature.

Crystalline Nylon 6,6: dissolved at room temperature by using the solvent with strong hydrogen bonds.



先熔融，后溶解

3.1 Interactions in Polymer System

van der Waals interactions

1. electrostatic interaction

Keesom force $E_K = -\frac{2}{3} \frac{\mu_1^2 \mu_2^2}{r^6 k_B T}$ between permanent charges

2. Induction (polarization) interaction

Debye force $E_D = \frac{-(\alpha_1 \mu_2^2 + \alpha_2 \mu_1^2)}{r^6}$ between a permanent multipole on one molecule with an induced multipole on another

3. Dispersion interaction

London force $E_L = -\frac{3}{2} \left(\frac{I_1 I_2}{I_1 + I_2} \right) \left(\frac{\alpha_1 \alpha_2}{r^6} \right)$ between any pair of molecules, including non-polar atoms, arising from the interactions of instantaneous multipoles.

μ : Dipole moment α : Polarizability $\alpha_\mu = \frac{\mu^2}{3k_B T}$ I : Ionization energy

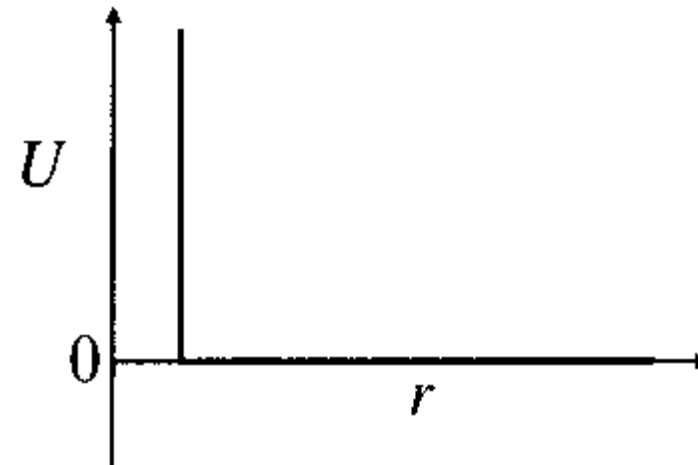
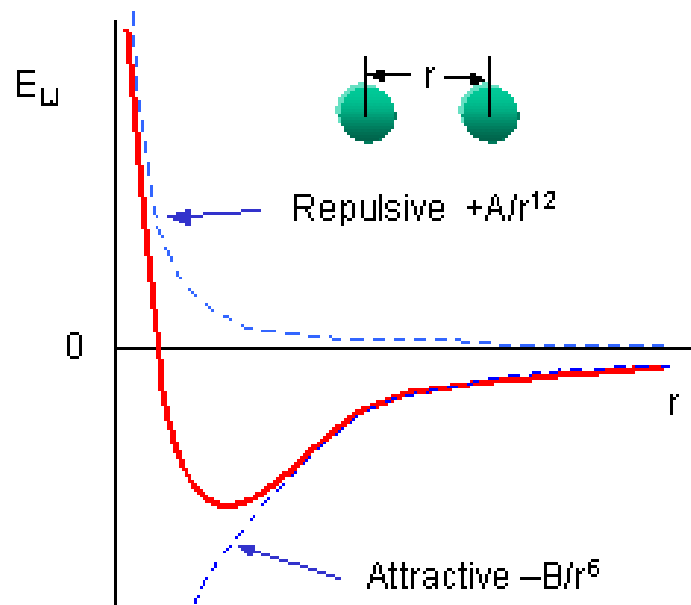
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- **Long-range Coulomb interactions**
see 3.8

$$U(r) = \frac{Q_1 Q_2 e^2}{4\pi\epsilon_0 k_B T r}$$

- **Hydrogen bond interactions**

The Lennard-Jones or Hard Core Potential

- The L-J (6-12) Potential is often used as an approximate model for a total (repulsion plus attraction) van der Waals force as a function of distance.



$$U_{LJ} = \frac{A}{r^{12}} - \frac{B}{r^6}$$

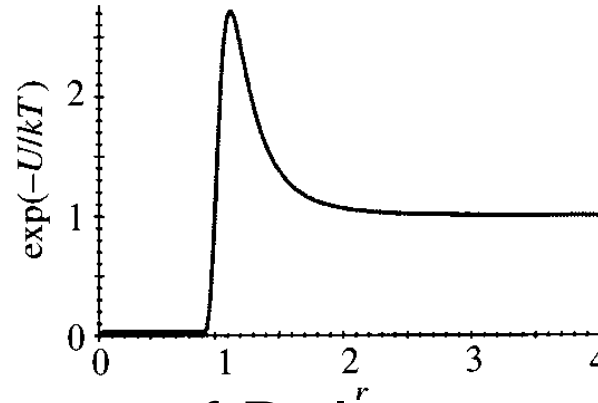
$$U = 0 \quad r > r_0$$

$$U = \infty \quad r \leq r_0$$

Mayer f -Function and Excluded Volume

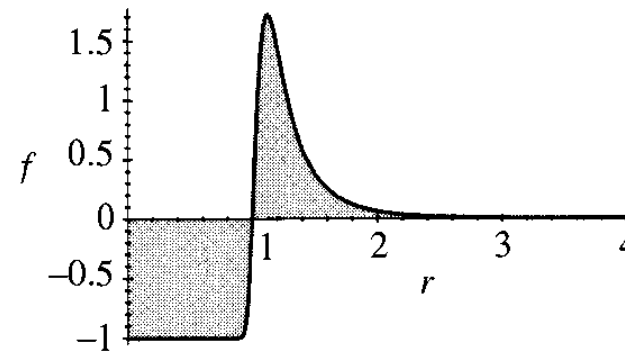
The Probability $P(r)$ of finding two monomers at distance r :

Boltzmann factor
$$P(r) \propto \exp[-U(r)/(k_B T)]$$



Mayer f -function: difference of Boltzmann factor for two monomers at r and at ∞

$$f(r) = \exp(-U(r)/k_B T) - 1$$



Exclude Volume v :

$$v = - \int f(r) d^3r = \int (1 - \exp[-U(r)/(k_B T)]) d^3r$$

3.2 Criteria (判据) of Polymer Solubility

➤ Gibbs free energy of mixing

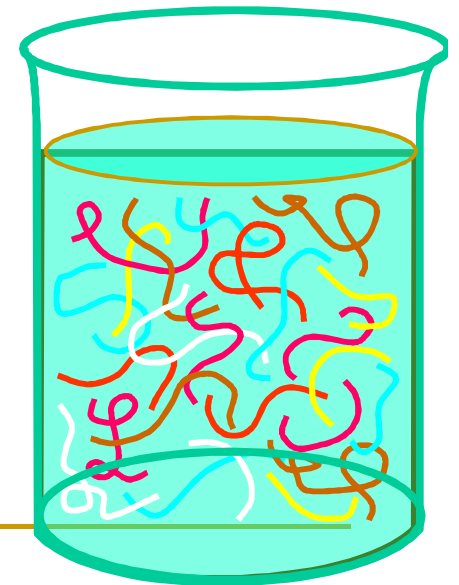
$$\Delta G_{mix} = \Delta H_{mix} - T \Delta S_{mix} \quad \text{➤ Solubility occurs only when the } \Delta G_{mix} \text{ is negative.}$$

$$\Delta S_{mix} > 0$$

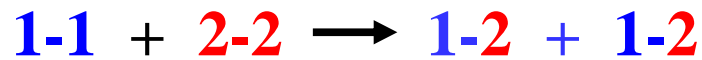
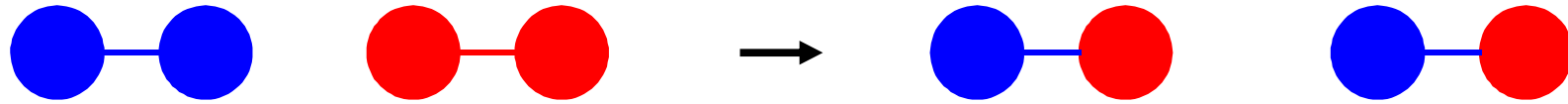
Entropy of mixing for ideal solution

$$\Delta S_{mix}^i = -k (N_1 \ln X_1 + N_2 \ln X_2) > 0$$

$$\Delta H_{mix} ???$$



1. Hildebrand enthalpy of mixing (混合焓)



1: solvent; 2: polymer

$$\Delta H_{mix} = \left(\frac{\Delta E_1}{v_1} + \frac{\Delta E_2}{v_2} - 2 \sqrt{\frac{\Delta E_1 \Delta E_2}{v_1 v_2}} \right) P_{12}$$

$(\Delta E/v)$ cohesive energy density

(摩尔内聚能密度)

P_{12} total pairs of [1-2]

$$\Delta H_{mix} = \left(\left(\frac{\Delta E_1}{v_1} \right)^{1/2} - \left(\frac{\Delta E_2}{v_2} \right)^{1/2} \right)^2 n_2 \bar{V}_2 \phi_1 \left(\frac{V_m}{V_m} \right)$$

$$\frac{n_2 \bar{V}_2}{V_m} = \phi_2 \quad \frac{n_1 \bar{V}_1}{V_m} = \phi_1$$

$$= \left(\left(\frac{\Delta E_1}{v_1} \right)^{1/2} - \left(\frac{\Delta E_2}{v_2} \right)^{1/2} \right)^2 n_1 \bar{V}_1 \phi_2 \left(\frac{V_m}{V_m} \right) = V_m \phi_1 \phi_2 \left(\left(\frac{\Delta E_1}{v_1} \right)^{1/2} - \left(\frac{\Delta E_2}{v_2} \right)^{1/2} \right)^2$$

$$= V_m \phi_1 \phi_2 [\delta_1 - \delta_2]^2$$

$\delta = (\Delta E/v)^{1/2}$: solubility parameter
(溶度参数)

2. Huggin's Enthalpy of mixing

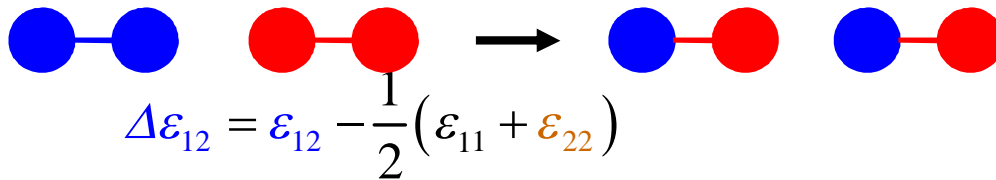
Different pairs in solution:

solvent-solvent molecule: [1-1], ϵ_{11}

solute-solute segment: [2-2], ϵ_{22}

solvent-solute: [1-2], ϵ_{12}

Mixing process: $\frac{1}{2}[1-1] + \frac{1}{2}[2-2] = [1-2]$



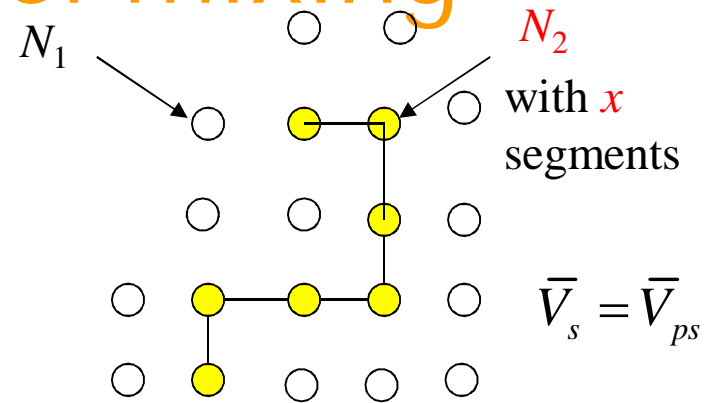
$$\Delta H_{mixing} = P_{12} \Delta\epsilon_{12} \quad \boxed{P_{12} \text{ total pairs of [1-2]}}$$

$$P_{12} = \left[\underbrace{(Z-2)x}_{\text{cells surrounding a polymer}} + \underbrace{2}_{\text{number of polymers}} \right] \phi_1 N_2 = (Z-2) N_1 \phi_2$$

cells surrounding a polymer

number of polymers

volume fraction of solvent ~ Possibility of the cell occupied by solvent.



$$\phi_1 = \frac{N_1}{N_1 + xN_2} = \frac{\bar{V}_s N_1}{V_m} \quad \text{and} \quad \phi_2 = \frac{xN_2}{N_1 + xN_2} = \frac{xN_2 \bar{V}_s}{V_m}$$

$$\Delta H_{mixing} = (Z-2) N_1 \phi_2 \Delta\epsilon_{12} = (Z-2) x N_2 \phi_1 \Delta\epsilon_{12}$$

$$\Delta H_{mixing} = kT \chi N_1 \phi_2 = RT \chi n_1 \phi_2$$

$$= \frac{V_m}{\bar{V}_s} kT \chi \phi_1 \phi_2 = V_m \phi_1 \phi_2 [\delta_1 - \delta_2]^2 / \tilde{N}$$

$$\chi = \frac{(Z-2) \Delta\epsilon_{12}}{kT} = \frac{\bar{V}_s (\delta_1 - \delta_2)^2}{RT}$$

Flory-Huggins parameter:
(interaction parameter)

另类导法

$$H_{11} = \frac{1}{\bar{V}_s} \int \varepsilon_{11} \phi_1^2(r) dr = \frac{\varepsilon_{11}}{\bar{V}_s} \int \phi_1(r) (1 - \phi_2(r)) dr$$

$$= \frac{\varepsilon_{11}}{\bar{V}_s} \int \phi_1(r) dr - \frac{\varepsilon_{11}}{\bar{V}_s} \int \phi_1(r) \phi_2(r) dr = \frac{V_m}{\bar{V}_s} (\varepsilon_{11} \phi_1 - \varepsilon_{11} \phi_1 \phi_2)$$

$$H_{22} = \varepsilon_{22} \phi_2^2 \frac{V_m}{\bar{V}_s} = \varepsilon_{22} \phi_2 (1 - \phi_1) \frac{V_m}{\bar{V}_s} = \frac{V_m}{\bar{V}_s} (\varepsilon_{22} \phi_2 - \varepsilon_{22} \phi_1 \phi_2)$$

$$H_{12} = \frac{V_m}{\bar{V}_s} \varepsilon_{12} \phi_1 \phi_2$$

$$\Delta H_{mixing} = H_{12} - \frac{1}{2} (H_{11} + H_{22}) = \frac{V_m}{\bar{V}_s} \left(\varepsilon_{12} - \frac{1}{2} (\varepsilon_{11} + \varepsilon_{22}) \right) \phi_1 \phi_2 + const.$$

$$= \frac{V_m}{\bar{V}_s} \chi \phi_1 \phi_2 + const.$$

另类导法

$$H_{11} = \frac{1}{2\bar{V}_s} \int \varepsilon_{11} \phi_1^2(r) dr = \frac{\varepsilon_{11}}{2\bar{V}_s} \int \phi_1(r) (1 - \phi_2(r)) dr$$

$$= \frac{\varepsilon_{11}}{2\bar{V}_s} \int \phi_1(r) dr - \frac{\varepsilon_{11}}{2\bar{V}_s} \int \phi_1(r) \phi_2(r) dr = \frac{V_m}{2\bar{V}_s} (\varepsilon_{11} \phi_1 - \varepsilon_{11} \phi_1 \phi_2)$$

$$H_{22} = \varepsilon_{22} \phi_2^2 \frac{V_m}{2\bar{V}_s} = \varepsilon_{22} \phi_2 (1 - \phi_1) \frac{V_m}{2\bar{V}_s} = \frac{V_m}{2\bar{V}_s} (\varepsilon_{22} \phi_2 - \varepsilon_{22} \phi_1 \phi_2)$$

$$H_{12} = \frac{V_m}{\bar{V}_s} \varepsilon_{12} \phi_1 \phi_2$$

$$\phi_1 = \frac{\bar{V}_s N_1}{V_m}$$

$$H_{11}^0 = \varepsilon_{11} \frac{V_s^0}{2\bar{V}_s} = \varepsilon_{11} \frac{N_1}{2}$$

$$\Delta H_{\text{mixing}} = H_{12} + (H_{11} + H_{22}) - (H_{11}^0 + H_{22}^0)$$

$$\phi_2 = \frac{x N_2 \bar{V}_s}{V_m}$$

$$H_{22}^0 = \varepsilon_{22} \frac{V_p^0}{2\bar{V}_s} = \varepsilon_{22} \frac{x N_2}{2}$$

$$= \frac{V_m}{\bar{V}_s} \left(\varepsilon_{12} - \frac{1}{2} (\varepsilon_{11} + \varepsilon_{22}) \right) \phi_1 \phi_2 = \frac{V_m}{\bar{V}_s} kT \chi \phi_1 \phi_2$$

$$V_s^0 + V_p^0 = V_m \quad 12$$

3.3 Thermodynamics of Polymer Solutions

链构象保持不变

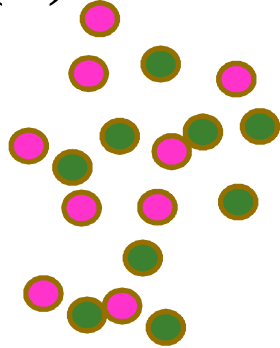
$\Delta S_{conf} = 0 ?$

$$S_{conf}(\mathbf{h}, N_g) = -\frac{3}{2} k_B \frac{\mathbf{h}^2}{N_g l^2} + C$$

与溶剂混合会产生各种排列组合状态, 即混合熵 $\Delta S_m > 0$

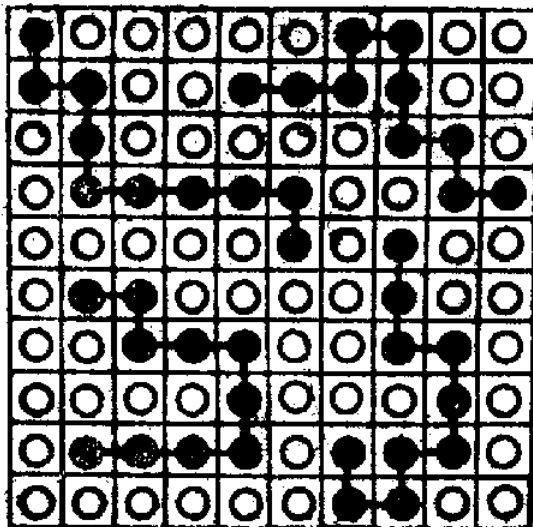
3.3 Thermodynamics of Polymer Solutions

(1) Entropy of mixing for ideal solution



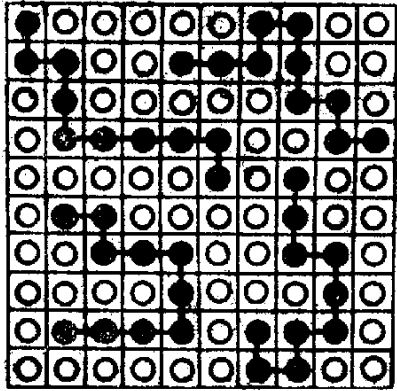
$$\Delta S_{mix}^i = -k (N_1 \ln X_1 + N_2 \ln X_2)$$

(2) Entropy of mixing for polymer solutions



- The lattice model assumes that the volume is unchanged during mixing.
- Each repeating unit of the polymer (segment) occupies one position in the lattice and so does each solvent molecule.
- The mixing entropy is strongly influenced by the chain connectivity of the polymer component.

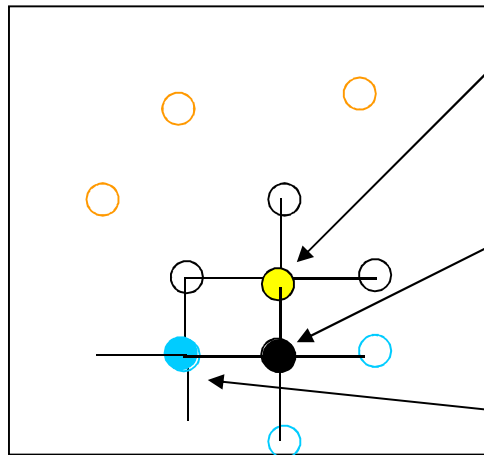
Flory-Huggins theory (Lattice Model (格子模型))



体系中有 N_1 个溶剂分子 + N_2 个链段数为 x 的高分子

$$\text{总格子数: } N = N_1 + xN_2 \quad \phi_1 = \frac{N_1}{N_1 + xN_2} \quad \phi_2 = \frac{xN_2}{N_1 + xN_2}$$

已有 j 个高分子放入, 剩下 $N - xj$ 个空格, 求第 $j+1$ 个高分子的放置方式 W_{j+1} ???



1. 放置第 $j+1$ 个高分子的第1个链段的概率

$$N - xj$$

2. 放置第 $j+1$ 个高分子的第2个链段的概率

$$Z(N - xj - 1) / N$$

3. 放置第 $j+1$ 个高分子的第3个链段的概率

$$(Z - 1)(N - xj - 2) / N \quad \dots$$

x. 放置第 x 个链段的概率

$$(Z - 1)(N - xj - x + 1) / N$$

Entropy of mixing from FH theory

$$W_{j+1} = \underbrace{(N - xj)}_{1^{\text{st}}} \times \underbrace{Z \left(\frac{N - xj - 1}{N} \right)}_{2^{\text{nd}}} \times \underbrace{(Z - 1) \left(\frac{N - xj - 2}{N} \right)}_{3^{\text{rd}}} \times \underbrace{(Z - 1) \left(\frac{N - xj - 3}{N} \right)}_{4^{\text{th}}} \cdots \underbrace{(Z - 1) \left(\frac{N - xj - x + 1}{N} \right)}_{x^{\text{th}} \text{ segment}}$$

$Z \approx Z - 1$

$$W_{j+1} = \left(\frac{Z - 1}{N} \right)^{x-1} \frac{(N - xj)!}{(N - xj - x)!}$$

总方式

$$\begin{aligned} \Omega &= \frac{1}{N_2!} \prod_{j=0}^{N_2-1} W_{j+1} = \frac{1}{N_2!} \left(\frac{Z - 1}{N} \right)^{N_2(x-1)} \frac{N!}{\underbrace{(N - x)!}_{1^{\text{st}}}} \frac{\cancel{(N - x)!}}{\underbrace{(N - 2x)!}_{2^{\text{st}}}} \cdots \frac{\cancel{(N - xN_2 + x)!}}{\underbrace{(N - xN_2)!}_{N_2^{\text{st}} \text{ chain}}} \\ &= \frac{1}{N_2!} \left(\frac{Z - 1}{N} \right)^{N_2(x-1)} \frac{N!}{(N - xN_2)!} \end{aligned}$$

Entropy of solution:

$$S_{\text{solution}} = k \ln \Omega = k \left[N_2(x - 1) \ln \left(\frac{Z - 1}{N} \right) + \ln N! - \ln N_2! - \ln(N - xN_2)! \right]$$

Entropy of mixing from FH theory

Using Stirling's approximation ($\ln x! \approx x \ln x - x$), we have:

$$S_{solution} = -k \left[N_1 \ln \frac{N_1}{N_1 + xN_2} + N_2 \ln \frac{N_2}{N_1 + xN_2} - N_2(x-1) \ln \frac{Z-1}{e} \right]$$

Entropy of the pure solvent and pure polymer:

$$S_{polymer} = kN_2 \left[\ln x + (x-1) \ln \frac{Z-1}{e} \right] \quad (N_1 = 0) \quad \text{and} \quad S_{solvent} = 0$$

Therefore,

$$\Delta S_{mixing} = S_{solution} - (S_{solvent} + S_{polymer}) \quad \Delta S_{conf} = 0$$

$$= -k \left[N_1 \ln \frac{N_1}{N_1 + xN_2} + N_2 \ln \frac{xN_2}{N_1 + xN_2} \right]$$

where

$$\phi_1 = \frac{N_1}{N_1 + xN_2} = \frac{n_1}{n_1 + xn_2} = \frac{N_1 \bar{V}_s}{V_m} = \frac{\tilde{N} n_1 \bar{V}_s}{V_m} \quad \phi_2 = \frac{xN_2}{N_1 + xN_2} = \frac{xn_2}{n_1 + xn_2} = \frac{xN_2 \bar{V}_s}{V_m} = \frac{\tilde{N} x n_2 \bar{V}_s}{V_m}$$

$$\Delta S_{mixing} = -k [N_1 \ln \phi_1 + N_2 \ln \phi_2] = -R [n_1 \ln \phi_1 + n_2 \ln \phi_2]$$

$$= -k \frac{V_m}{\bar{V}_s} \left[\phi_1 \ln \phi_1 + \frac{\phi_2}{x} \ln \phi_2 \right]$$

Free Energy of FH Theory

Huggins Enthalpy: $\Delta H_{mixing} = kT \chi N_1 \phi_2 = RT \chi n_1 \phi_2 = \frac{V_m}{\bar{V}_s} kT \chi \phi_1 \phi_2$

$$\phi_1 = \frac{x_1 N_1}{x_1 N_1 + x_2 N_2} = \frac{x_1 n_1}{x_1 n_1 + x_2 n_2} = \frac{x_1 N_1 \bar{V}_s}{V_m} = \frac{\tilde{N} x_1 n_1 \bar{V}_s}{V_m} \quad \phi_2 = \frac{x_2 N_2}{x_1 N_1 + x_2 N_2} = \frac{x_2 n_2}{x_1 n_1 + x_2 n_2} = \frac{x_2 N_2 \bar{V}_s}{V_m} = \frac{\tilde{N} x_2 n_2 \bar{V}_s}{V_m}$$

Gibbs Free Energy $\Delta G_{mixing} = \Delta H_{mixing} - T \Delta S_{mixing}$

$$\Delta G_{mixing} = kT (N_1 \ln \phi_1 + N_2 \ln \phi_2 + \chi x_1 N_1 \phi_2) \quad \text{分子数}$$

$$= RT (n_1 \ln \phi_1 + n_2 \ln \phi_2 + \chi x_1 n_1 \phi_2) \quad \text{摩尔数}$$

$$= kT \frac{V_m}{\bar{V}_s} \left(\frac{\phi_1}{x_1} \ln \phi_1 + \frac{\phi_2}{x_2} \ln \phi_2 + \chi \phi_1 \phi_2 \right) \quad \text{通式}$$

$$\Delta F_m = \frac{\bar{V}_s}{V_m} \frac{\Delta G_m}{kT} = \left(\frac{\phi_1}{x_1} \ln \phi_1 + \frac{\phi_2}{x_2} \ln \phi_2 + \chi \phi_1 \phi_2 \right)$$

For Polymer Solutions $x_1=1$

Chemical potentials (化学位):

$$\Delta\mu_1 = \left[\frac{\partial(\Delta G_m)}{\partial n_1} \right]_{T,P,n_2} = RT \left[\ln \phi_1 + \left(1 - \frac{1}{x}\right) \phi_2 + \chi \phi_2^2 \right] \quad \text{(for solvent)}$$

$$= \frac{\bar{V}_s}{V_m} \left(\Delta G_m - \phi_2 \frac{\partial \Delta G_m}{\partial \phi_2} \right) = RT \left(\Delta F_m - \phi_2 \frac{\partial \Delta F_m}{\partial \phi_2} \right)$$

$$\Delta F_m = \frac{\bar{V}_s}{V_m} \frac{\Delta G_m}{kT} = \left(\phi_1 \ln \phi_1 + \frac{\phi_2}{x} \ln \phi_2 + \chi \phi_1 \phi_2 \right)$$

$$\Delta\mu_2 = \left[\frac{\partial(\Delta G_m)}{\partial n_2} \right]_{T,P,n_1} = RT \left[\ln \phi_2 - (x-1) \phi_1 + x \chi \phi_1^2 \right] \quad \text{(for polymer)}$$

$$= \frac{\bar{V}_s}{V_m} \left(\Delta G_m - \phi_1 \frac{\partial \Delta G_m}{\partial \phi_1} \right) = RT \left(\Delta F_m - \phi_1 \frac{\partial \Delta F_m}{\partial \phi_1} \right)$$

In the case of $\phi_2 \ll 1$, $\ln \phi_1 = \ln(1 - \phi_2) \approx -\phi_2 - \frac{1}{2} \phi_2^2 \dots$

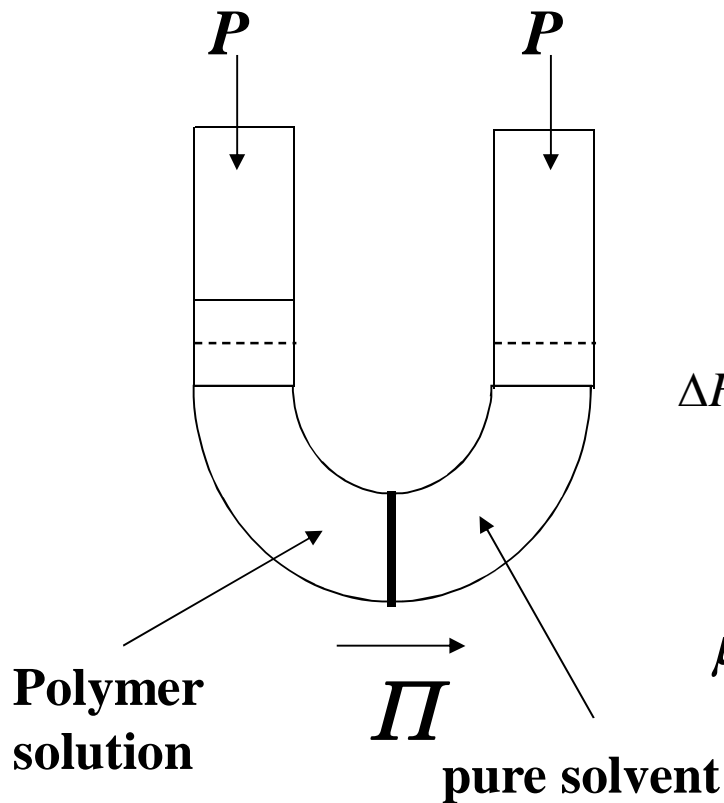
$$\Delta\mu_1 = RT \left[-\frac{1}{x} \phi_2 + \left(\chi - \frac{1}{2} \right) \phi_2^2 + w \phi_2^3 \right] \quad \chi=1/2, \text{ 有热效应的“理想溶液” ???}$$

$\chi < 1/2$, good solvent
 $\chi = 1/2$, theta Θ solvent
 $\chi > 1/2$, poor solvent

Osmotic pressure (渗透压):

$$\mu_s(\phi_2, P + \Pi, T) = \mu_s(0, P, T)$$

$$G(n_p, n_s, P, T) = G_m + PV_m = G_m + P(n_p x + n_s) \bar{V}_s$$



$$\mu_s(\phi_2, P, T) = \frac{\partial}{\partial n_s} [G(n_p, n_s, P, T)]_{T, P, n_p}$$

$$= \mu_s^0 + \left[\frac{\partial(\Delta G_m)}{\partial n_s} \right]_{T, P, n_p} + P \bar{V}_s$$

$$\Delta F_m = \frac{\bar{V}_s}{V_m} \frac{\Delta G_m}{kT} \quad \left[\frac{\partial(\Delta G_m)}{\partial n_s} \right]_{T, P, n_p} = RT \left(\Delta F_m - \phi_2 \frac{\partial \Delta F_m}{\partial \phi_2} \right)$$

$$\mu_s(\phi_2, P, T) = \mu_s^0 + RT \left(\Delta F_m - \phi_2 \frac{\partial \Delta F_m}{\partial \phi_2} \right) + P \bar{V}_s$$

$$\therefore \mu_s(\phi_2, P + \Pi, T) = \mu_s(0, P, T)$$

$$V_m = (n_p x + n_s) \bar{V}_s$$

$$\therefore \Pi = \frac{RT}{\bar{V}_s} \left(\phi_2 \frac{\partial \Delta F_m}{\partial \phi_2} - \Delta F_m \right)$$

Osmotic pressure (渗透压):

$$\Pi = \frac{RT}{\bar{V}_s} \left(\phi_2 \frac{\partial \Delta F_m}{\partial \phi_2} - \Delta F_m \right) = -\frac{\Delta \mu_1}{\bar{V}_s} = \frac{RT}{\bar{V}_s} \left[\frac{1}{x} \phi_2 + \left(\frac{1}{2} - \chi \right) \phi_2^2 \right]$$

$$\Delta F_m = \frac{\bar{V}_s}{V_m} \frac{\Delta G_m}{kT} = \left(\phi_1 \ln \phi_1 + \frac{\phi_2}{x} \ln \phi_2 + \chi \phi_1 \phi_2 \right)$$

$$A_{2\phi} = \frac{\left(\frac{1}{2} - \chi \right)}{\bar{V}_s} \quad \text{second Virial coefficient}$$

$$\boxed{\phi = \frac{c}{\rho_2}, \quad \rho_2 = \frac{M}{x\bar{V}_s}} \quad \Pi = RT \left[\frac{c}{M} + A_2 c^2 \right] \quad A_{2c} = \frac{\left(\frac{1}{2} - \chi \right)}{\bar{V}_1 \rho_2^2}$$

当 $\phi_2 \ll 1/x(0.5-\chi)$ 或 $\chi=1/2$

$$\Pi = \frac{RT}{\bar{V}_s} \left[\frac{1}{x} \phi_2 \right]$$

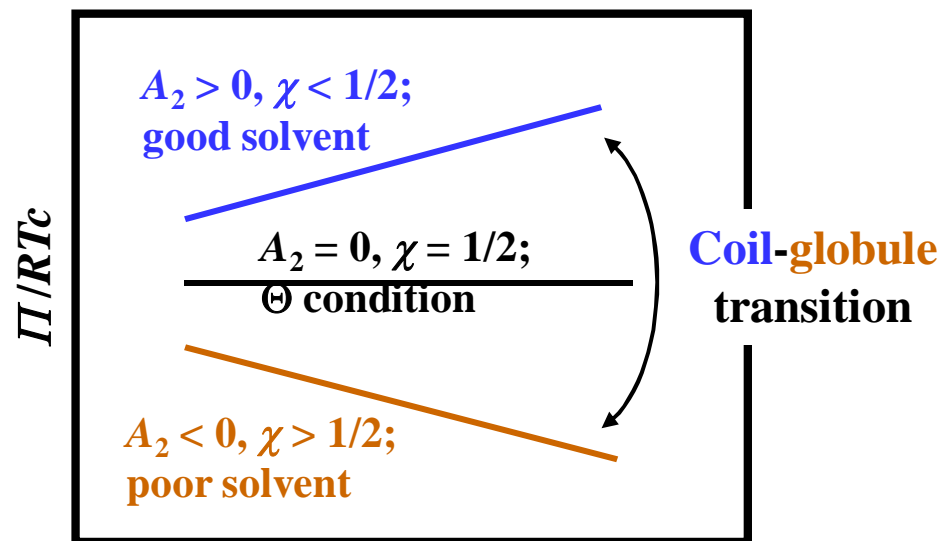
当 $\phi_2 \gg 1/x$, 即 $\phi_2^2 \gg \phi_2/x$

~~$\Pi \sim \phi_2^2$~~ ???

Polymer Shapes in Dilute Solutions

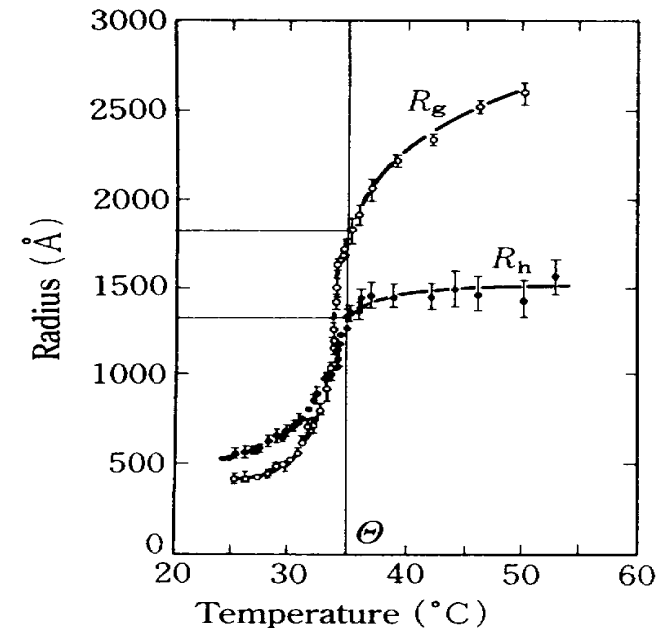
➤ Expanded, unperturbed, and collapsed chains

$$\Pi = \frac{RT}{\bar{V}_1} \left[\frac{1}{x} \phi_2 + \left(\frac{1}{2} - \chi \right) \phi_2^2 \right]$$



concentration

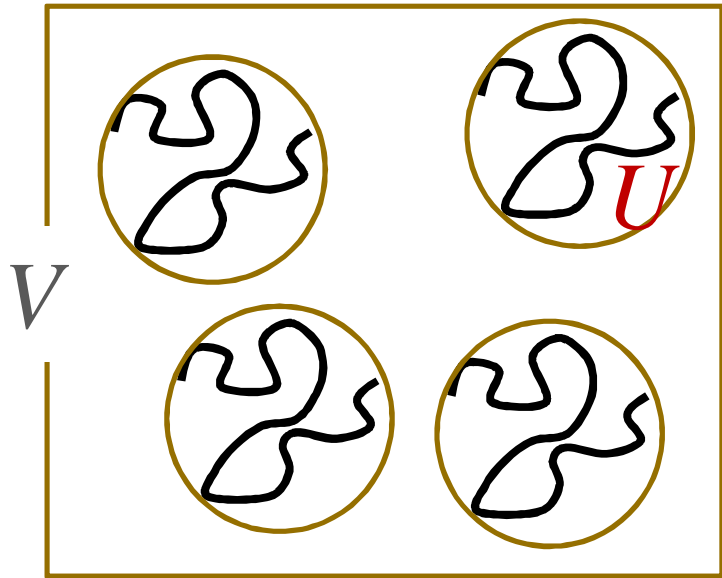
$$\chi \sim 1/kT !!!$$



The coil-globule transition in a solution of polystyrene in cyclohexane. The radius of gyration R_g and the hydrodynamic radius R_h of the polymer show a dramatic change as temperature passes through the Θ temperature. (Sun, S.T.; etc. *J. Chem. Phys.* 1980, 73, 5971.)

3.4 Chain Conformations in Dilute Solutions

(1) Flory-Krigbaum's Theory



有 N_2 个体积为 U 的“刚球”
 两两刚球都不发生重叠的总概率

$$\Omega \approx (1 - U/V)^0 (1 - U/V)^1 \dots (1 - U/V)^{(N_2-1)}$$

$$\approx \left(1 - \frac{U}{V}\right)^{N_2(N_2-1)/2} \approx \left(1 - \frac{U}{V}\right)^{N_2^2/2}$$

or $\Omega \approx \prod_{i=0}^{N_2-1} \left(1 - \frac{iU}{V}\right)$

$$\Delta F \approx -T \Delta S = -kT \ln \Omega \quad \ln \left(1 - \frac{iU}{V}\right) \approx -\frac{iU}{V} \quad \Pi = -\frac{\Delta \mu_1}{\tilde{V}_1} = -\frac{\partial \Delta F}{\partial V}$$

$$= -kT \left[N_2 \ln V - \frac{N_2^2 U}{2V} \right] = RT \left[\frac{c}{M} + \frac{\tilde{N}U}{2M^2} c^2 \right]$$

$$U \sim R_g^3 \sim T ??$$

A_2

3.4 Chain Conformations in Dilute Solutions

(2) Flory 稀溶液理论

ideal chain

$$W_0(h, x) = \left(\frac{3}{2\pi xl^2} \right)^{3/2} \exp\left(-\frac{3h^2}{2xl^2} \right) 4\pi h^2$$

real chain in solutions

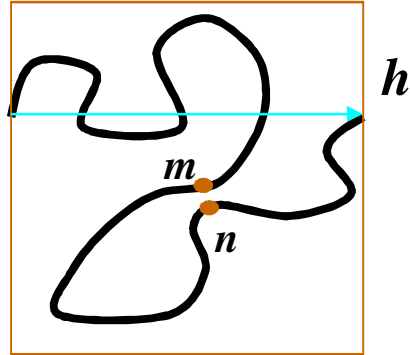
$$W(h, x) = W_0(h, x) \underbrace{\Omega(h)}_{\text{体积排除修正}} \exp\left(-\frac{\bar{E}(h)}{kT} \right) \text{能量权重修正}$$

体积排除修正：只统计单元间不发生重叠的构象状态，因为一旦发生了重叠，此构象就不能存在。

能量权重修正：每种构象的实现概率还与实现此构象状态的能级有关，能级越高，则实现的概率相应降低；能级越低，则反之。

体积排除修正

(1) $\Omega(h)$



链包含的体积 h^3 链段的体积 $v_c = l^3$

一个链段占有的体积分数 v_c/h^3 $\phi_2 = \frac{xv_c}{h^3}$

其他链段不与之发生重叠的概率 $(1 - v_c/h^3)$

整条链两两链段都不发生重叠的总概率

$$\Omega(h) \approx 1 \left(1 - \frac{v_c}{h^3}\right) \left(1 - 2\frac{v_c}{h^3}\right) \dots = \prod_{i=0}^{x-1} \left(1 - i\frac{v_c}{h^3}\right)$$

第一个 第二个 第三个

$$\approx \exp \left[\ln \prod_{i=0}^{x-1} \left(1 - i\frac{v_c}{h^3}\right) \right] = \exp \left[\sum_{i=0}^{x-1} \ln \left(1 - i\frac{v_c}{h^3}\right) \right]$$

$$\ln \left(1 - \frac{iu}{V}\right) \approx -\frac{iu}{V} \approx \exp \left[-\frac{v_c}{h^3} \sum_{i=0}^{x-1} i \right] = \exp \left[-\frac{v_c x^2}{2h^3} \right]$$

溶液中真实单链构象的径向分布函数 $W(h, x)$

(2) $E(h)$ $\frac{H}{kT} = \frac{V_m}{\bar{V}_s} \chi \phi_1 \phi_2$ $V_m \approx h^3$ $\bar{V}_s = v_c$ $\phi_2 = \frac{xv_c}{h^3}$

$$\begin{aligned} \frac{\bar{E}(h)}{kT} &= \frac{h^3}{v_c} \chi (1 - \phi_2) \phi_2 = \frac{h^3}{v_c} \chi \phi_2 - \frac{h^3}{v_c} \chi \phi_2^2 = x\chi - \frac{h^3}{v_c} \chi \frac{x^2 v_c^2}{h^6} \\ &= const - \chi \frac{x^2 v_c}{h^3} \end{aligned}$$

$$W(h, x) = W_0(h, x) \Omega(h) \exp\left(-\frac{\bar{E}(h)}{kT}\right)$$

$$W(h, x) \propto h^2 \exp\left[-\frac{3h^2}{2xl^2} - \frac{x^2 v_c}{2 h^3} (1 - 2\chi)\right]$$

**链内两体
相互作用
能的总和**

包括了链段的排斥体积和溶剂-链段相互作用

当 $\chi=1/2$, 理想高斯链

当 $\chi < 1/2$, ???

1. Polymer chain in good solvents – method I

$$W(h, x) \propto h^2 \exp\left[-\frac{3h^2}{2xl^2} - \frac{x^2}{2} \frac{v_c}{h^3} (1-2\chi)\right] \quad \frac{\partial W(h, x)}{\partial h} = 0$$

$$\frac{\partial W(h, x)}{\partial h} = \exp\left[-\frac{3h^2}{2xl^2} - \frac{x^2}{2} \frac{v_c}{h^3} (1-2\chi)\right] \left\{ 2h + h^2 \left[-\frac{3h}{xl^2} + \frac{3x^2}{2} \frac{v_c}{h^4} (1-2\chi) \right] \right\}$$

$$1 - \frac{3h^*{}^2}{2xl^2} + \frac{3x^2}{4} \frac{v_c}{h^*{}^3} (1-2\chi) = 0 \quad \rightarrow \quad \left(\frac{h^*}{h_0^*}\right)^5 - \left(\frac{h^*}{h_0^*}\right)^3 = \frac{9\sqrt{6}}{16} \frac{v_c}{l^3} x^{1/2} (1-2\chi)$$

$W_0(h, x)$ 的极值 $h_0^* = (2xl^2/3)^{1/2}$

最可几尺寸 \approx 根均方尺寸

$$h^* \propto h_0^* \left(\frac{x^{1/2} v_c (1-2\chi)}{l^3} \right)^{1/5} \propto x^\nu \left[\frac{v_c (1-2\chi)}{l^3} \right]^{1/5} l \propto x^\nu \tau^{1/5} \quad \begin{matrix} \tau = 1-2\chi \\ u = v_c (1-2\chi) = v_c \tau \end{matrix}$$

$$\chi < 1/2, \nu = 3/5$$

$$\chi = 1/2, \nu = 1/2$$

$$\chi > 1/2, \nu = ??$$

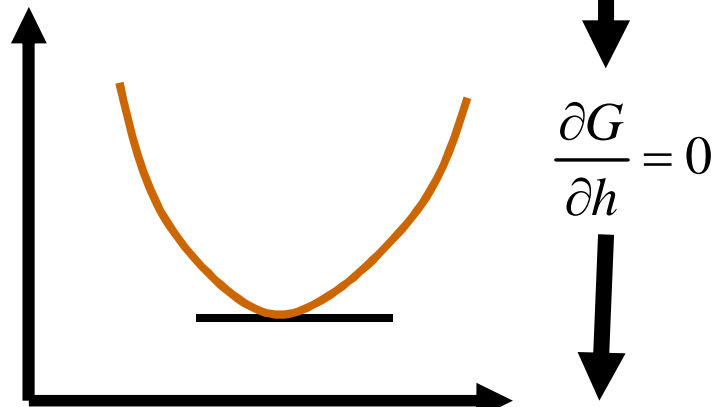
1. Polymer chain in good solvents - method II

单链自由能: $G \sim -k_B T \ln \Phi \quad \Phi(h, x) \propto \exp \left[-\frac{3h^2}{2xl^2} - \frac{x^2 v_c}{2 h^3} (1 - 2\chi) + \dots \right]$

$$G \sim k_B T \left(\frac{3h^2}{2xl^2} + \frac{x^2 v_c}{2h^3} (1 - 2\chi) + \dots \right)$$

$$\phi_2 = \frac{xv_c}{h^3} \quad \chi < 1/2$$

$$G / k_B T \approx \left(\frac{3}{2xl^2 h} + \frac{\left(\frac{1}{2} - \chi\right)}{v_c} \phi_2^2 + w \phi_2^3 \right) h^3$$



$$\frac{\partial G}{\partial h} = 0$$

$$h \propto x^{3/5} (1 - 2\chi)^{1/5}$$

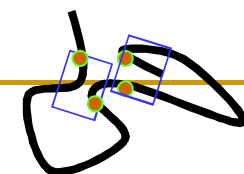
conformation entropy

second Virial coefficient

+ two body interaction:
excluded volume repulsion

solvent-segment interaction

Two body interactions are important in good solvents!



⊖ Temperature & ⊖ Solvents

$$\chi=1/2$$



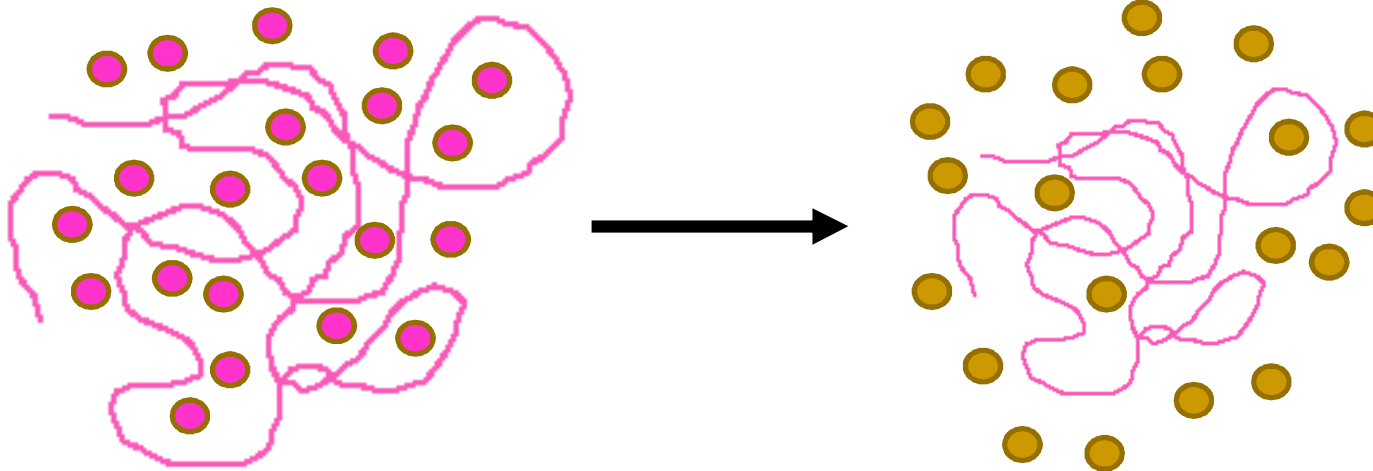
$$h^2 \sim N^1$$

$$\chi_{\theta} = \frac{(Z-2)\Delta\epsilon_{12}}{kT_{\theta}} = \frac{\bar{V}_s(\delta_1 - \delta_2)^2}{RT_{\theta}} = \frac{1}{2}$$

⊖ Solution

$$T_{\theta} = \frac{2(Z-2)\Delta\epsilon_{12}}{k} = \frac{2\bar{V}_s}{R}(\delta_1 - \delta_2)^2$$

⊖ Temperature



T

T_{θ}

Excluded Volume

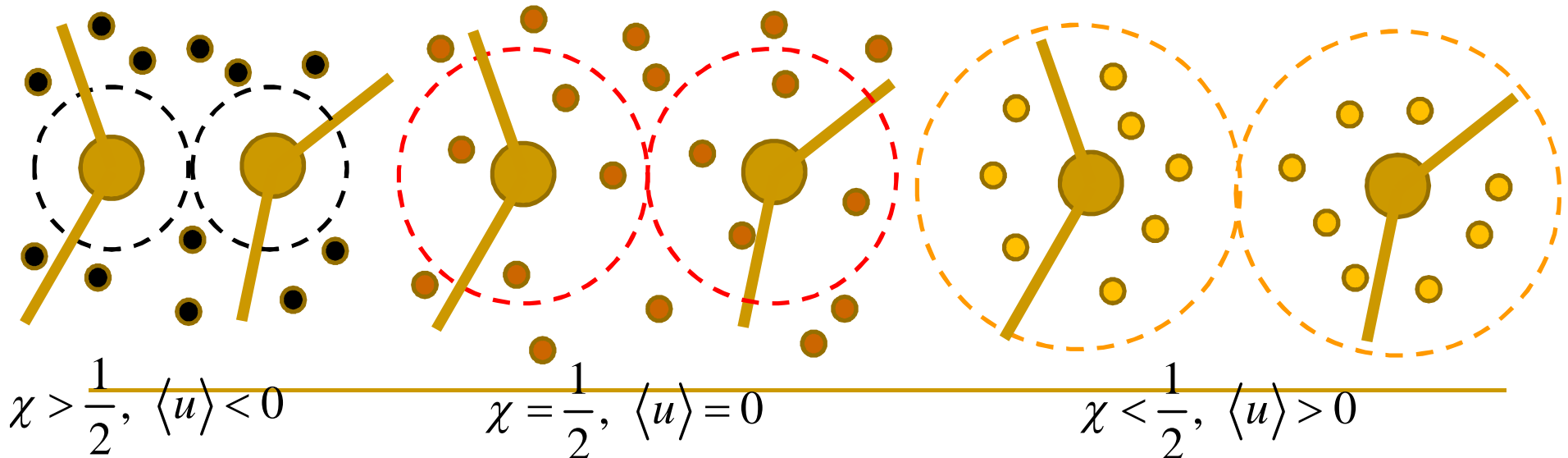
$$T_\theta = \frac{2(Z-2)\Delta\varepsilon_{12}}{k} = \frac{2V_s}{R}(\delta_1 - \delta_2)^2 \quad \Theta \text{ Temperature}$$

$$1 - 2\chi = 1 - \frac{\chi}{1/2} = \left(1 - \frac{T_\theta}{T}\right) = \tau \quad \tau \text{ 参考温度}$$

排除体积

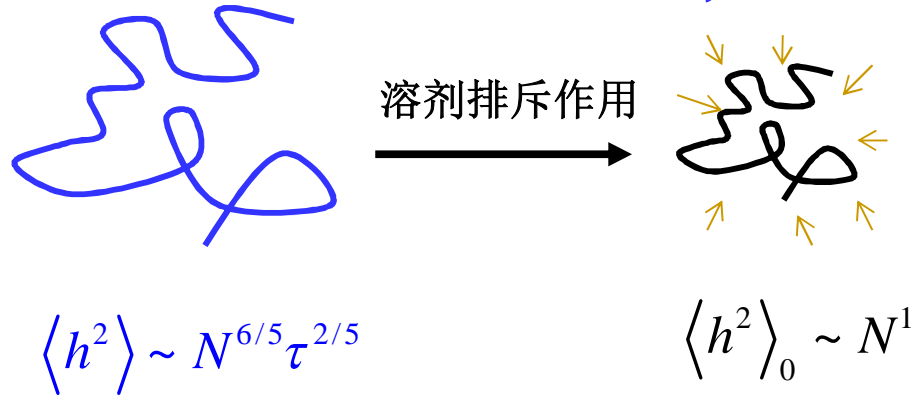
$$u = v_c (1 - 2\chi) \approx l_e^3 \tau$$

$$h^* \propto x^v (1 - 2\chi)^{1/5} \propto x^v \tau^{1/5}$$



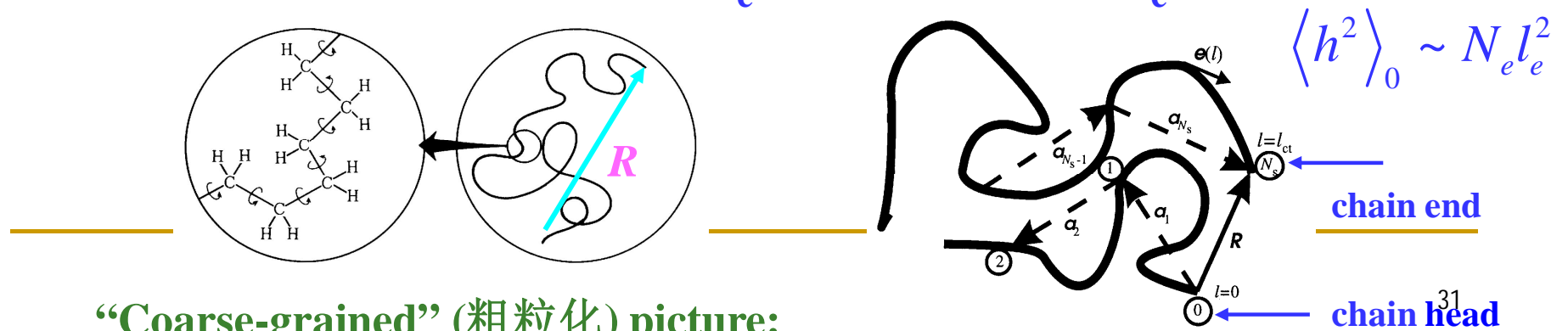
When does the freely jointed chain works

(1) 调节溶剂-链节的作用屏蔽掉体积排除效应和链节-链节相互作用 \longrightarrow 达到 Θ 温度的溶液, 测得无扰尺寸 $\langle h^2 \rangle_0 \sim N$



(2) 降低高分子链的分辨率-消除局部刚性和旋转不自由

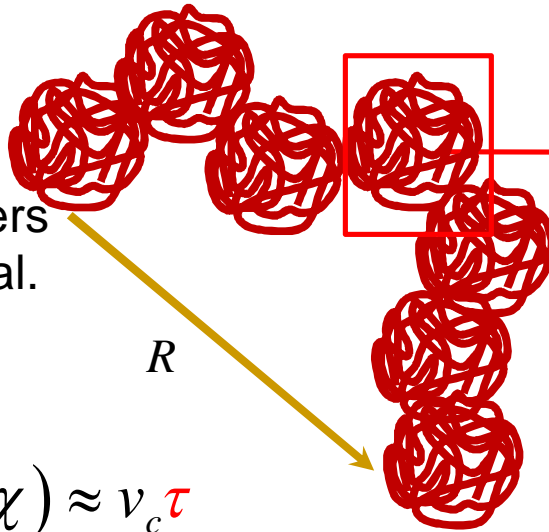
将链重新划分成有效链节数 N_e 和有效链节长度 l_e



“Coarse-grained” (粗粒化) picture:

Crossover from Gaussian to Swollen

Each polymer chain can be divided into many blobs. Polymers within blobs are ideal.



Thermal Blob $\xi_T = g_T^{1/2} l$

Number of Segments in a Chain: x

Number of Segments in a Blob: g_T

Numbers of Blob in a Chain: x/g_T

$$u = v_c (1 - 2\chi) \approx v_c \tau$$

$$R \propto \xi_T \left(\frac{x}{g_T} \right)^{3/5} = g_T^{1/2} \left(\frac{x}{g_T} \right)^{3/5} l = g_T^{-1/10} x^{3/5} l \quad = x^{3/5} \left(\frac{u}{l^3} \right)^{1/5} l$$

$$g_T = \left(\frac{u}{l^3} \right)^{-2}$$

$$\bar{E} \approx k_B T g_T^2 \frac{|u|}{\xi_T^3} \approx k_B T$$

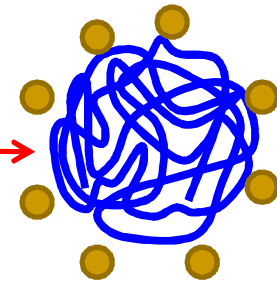
$$\xi_T = \left(\frac{u}{l^3} \right)^{-1} l = \frac{l^4}{u}$$

2. Polymer chain in poor solvents-Method I: blob model

Globule:



Blobs:



Blob size:

$$\xi_T = g_T^{1/2} l$$

Interaction Energy in a blob:

$$\bar{E} \approx k_B T g_T^2 \frac{|u|}{\xi_T^3} \approx k_B T$$

Excluded Volume:

$$u \approx l^3 (1 - 2\chi) \approx l^3 \tau$$

$$g_T = \left(\frac{u}{l^3} \right)^{-2} = |\tau|^{-2} \quad \xi_T = \left(\frac{u}{l^3} \right)^{-1} l = l |\tau|^{-1}$$

In a Globule: Blobs are densely packed

$$R_{glob}^3 = \xi_T^3 \left(\frac{N}{g_T} \right) \quad R_{glob}^3 \approx l^3 |\tau|^{-1} N$$

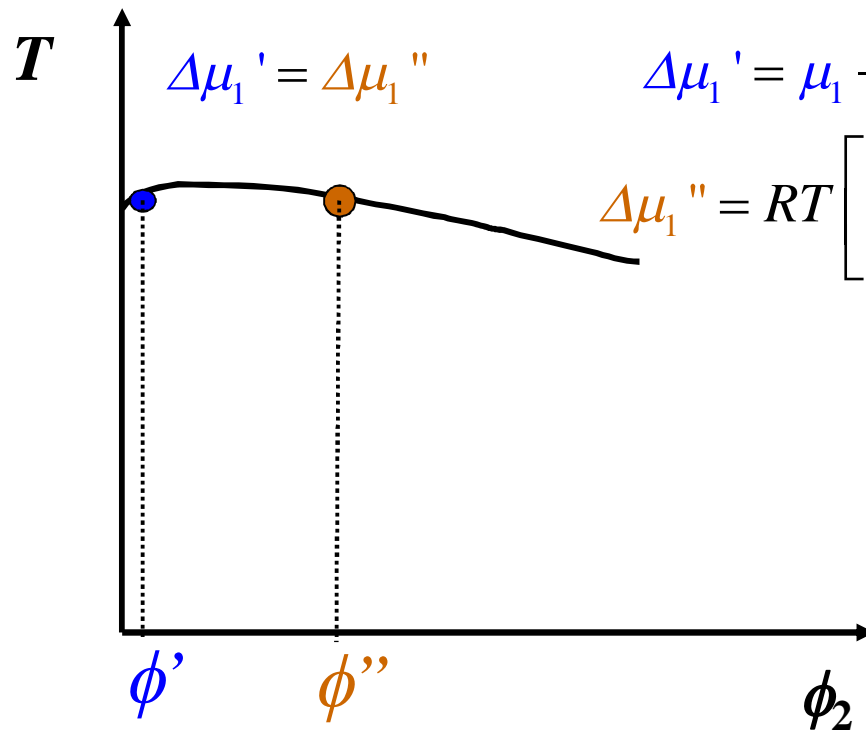
$$R_{glob} \approx N^{1/3} l |\tau|^{-1/3}$$

Interaction Energy
in a globule:

$$F_{int} = -k_B T \frac{N}{g_T} = -k_B T N \tau^2$$

2. Polymer chain in poor solvents-Method II: chemical potential

$$\Delta\mu_1 = RT \left[-\frac{1}{x} \phi_2 + \left(\chi - \frac{1}{2} \right) \phi_2^2 + w\phi_2^3 \right]$$



$$\Delta\mu_1' = \Delta\mu_1''$$

$$\Delta\mu_1' = \mu_1 - \mu_1^0 \approx 0 \Big|_{\phi_2' \rightarrow 0}$$

$$\Delta\mu_1'' = RT \left[-\frac{1}{x} \phi_2'' + \left(\chi - \frac{1}{2} \right) \phi_2''^2 + w\phi_2''^3 \right] = 0, \quad x \rightarrow \infty$$

$$w=1/3$$

$$\phi_2'' \sim 3 \left(\chi - \frac{1}{2} \right)$$

In Polymer rich Phase:

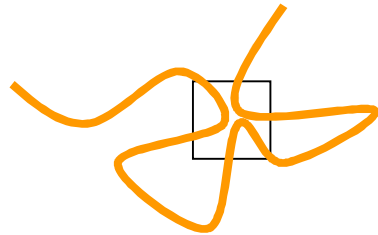
$$\text{Concentration in Coil: } \phi_{in} = \frac{xv_c}{h^3} \approx \phi_2''$$

$$h \sim v_c^{1/3} x^{1/3} \left(\chi - 1/2 \right)^{-1/3} \sim x^{1/3} l |\tau|^{-1/3}$$

2. Polymer chain in poor solvents-Method III: three body interactions

$$\chi > 1/2$$

$$h \ll h_0$$



$$W(h, x) \propto \exp \left[-\frac{3h^2}{2xl^2} - \frac{x^2 v_c}{2h^3} (1 - 2\chi) + \dots \right]$$

$$G \sim k_B T \left(\frac{3h^2}{2xl^2} + \frac{x^2 v_c}{2h^3} (1 - 2\chi) + ??? \right) \quad \phi_2 = xv_c/h^3$$

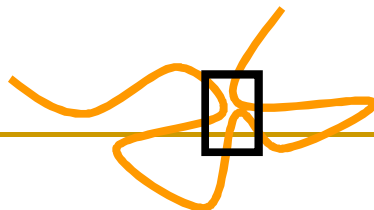
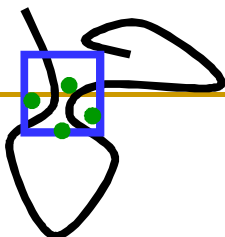
$$G / k_B T \sim \left[\frac{\left(\frac{1}{2} - \chi \right)}{v_c} \phi_2^2 + w \phi_2^3 \right] h^3 = \left[\frac{\left(\frac{1}{2} - \chi \right)}{v_c} \left(\frac{xv_c}{h^3} \right)^2 + w \left(\frac{xv_c}{h^3} \right)^3 \right] h^3$$

second Virial coefficient
two body interaction:
excluded volume repulsion
solvent-segment interaction

+ third Virial coefficient
three body repulsion

$G=0$

$$h^3 \sim x (-\tau)^{-1} v_c$$



Three body interactions
become important

Flory Formula in Dilute Solutions

$$G \approx k_B T \left(\frac{R^2}{Nl^2} + u \frac{N^2}{R^3} + w \frac{N^3}{R^6} \right)$$

$$R \approx h$$

$$u = v_c (1 - 2\chi)$$

N : Number of Segments in a chain

l : Length of the Kuhn Segment

In good solvents

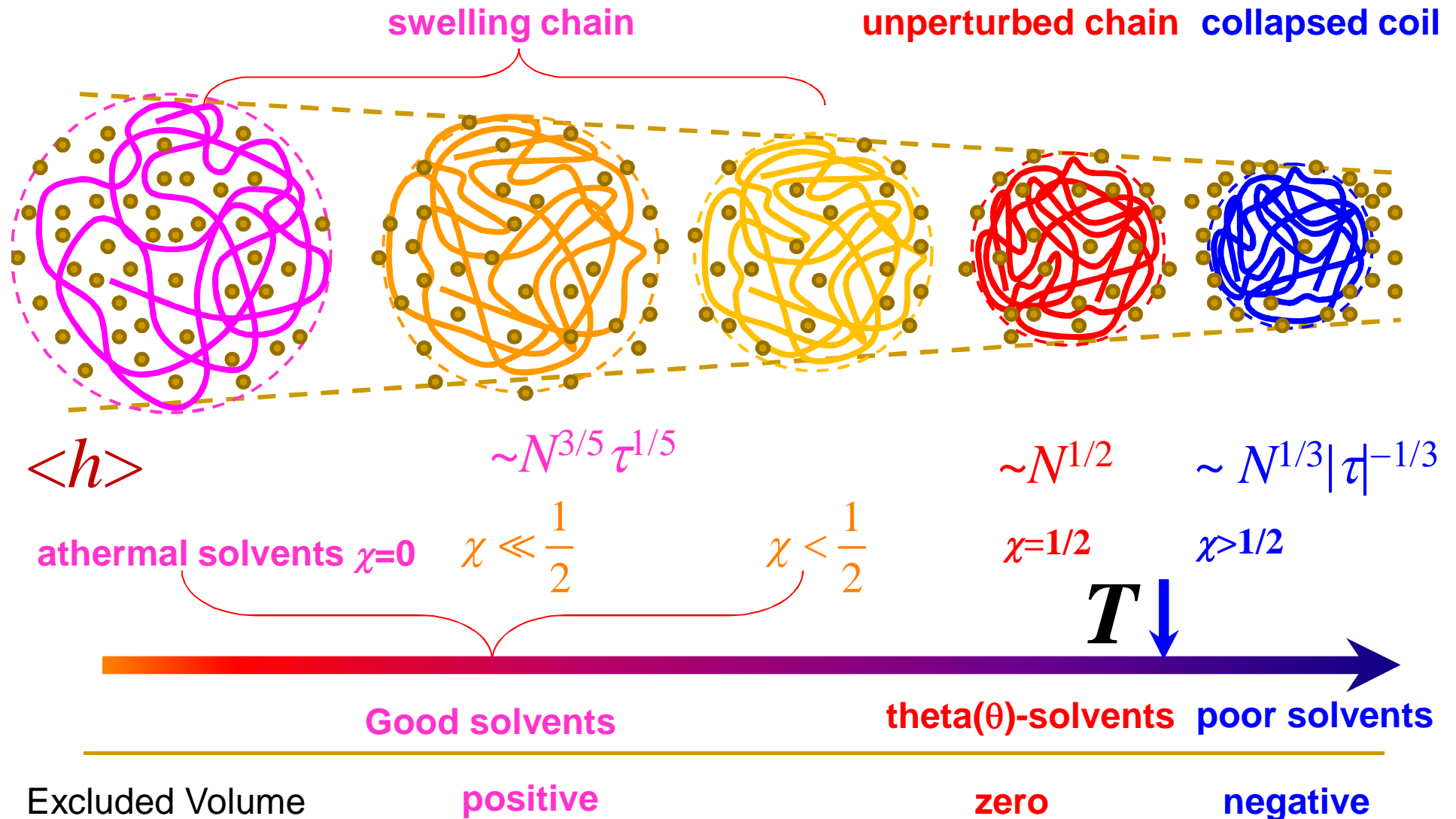
$$G \approx k_B T \left(\frac{R^2}{Nl^2} + u \frac{N^2}{R^3} \right)$$

In poor solvents

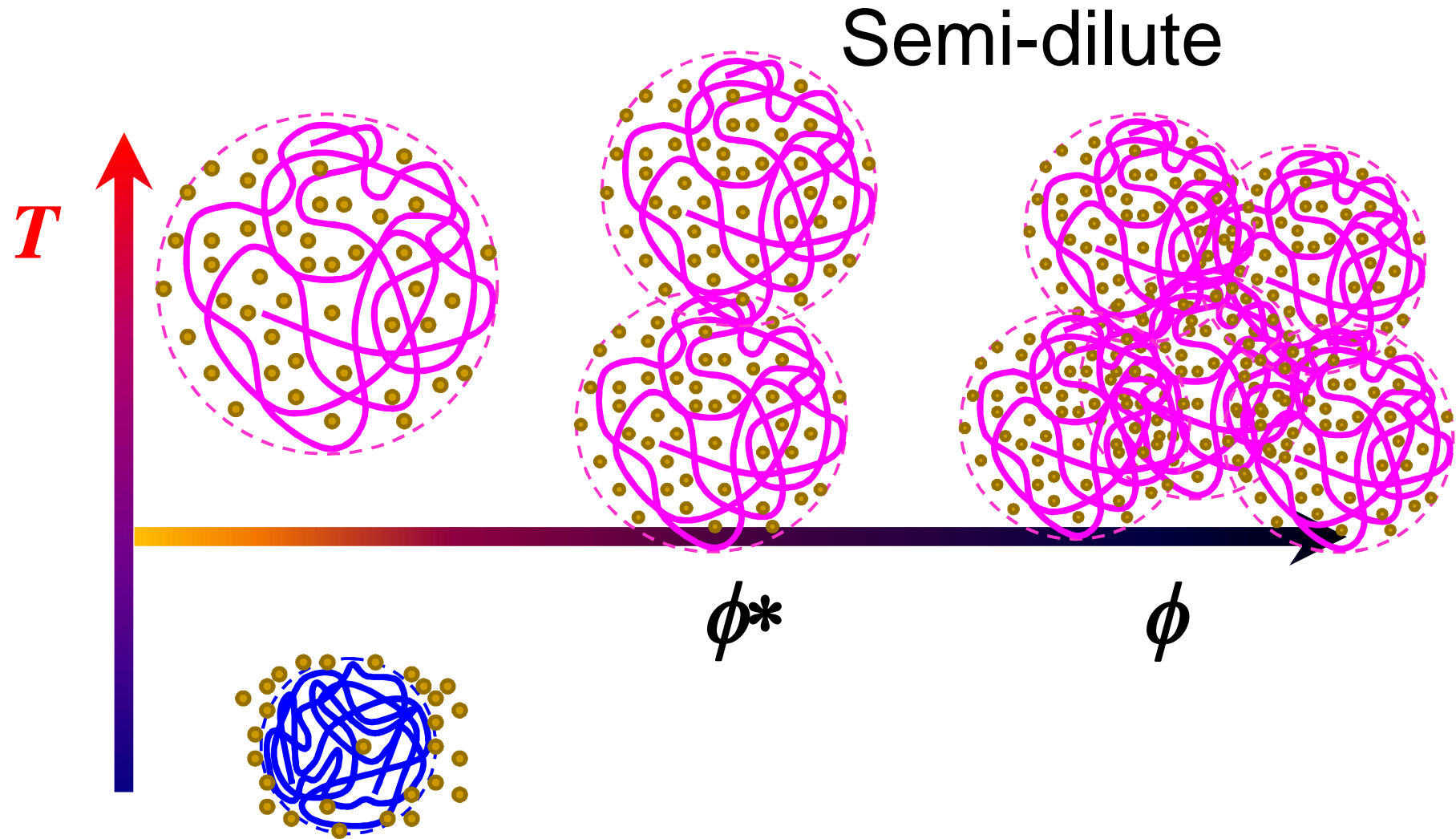
$$G \approx k_B T \left(u \frac{N^2}{R^3} + w \frac{N^3}{R^6} \right)$$

Polymer Shapes in Dilute Solutions

Coil-globule transition



From dilute to concentrated

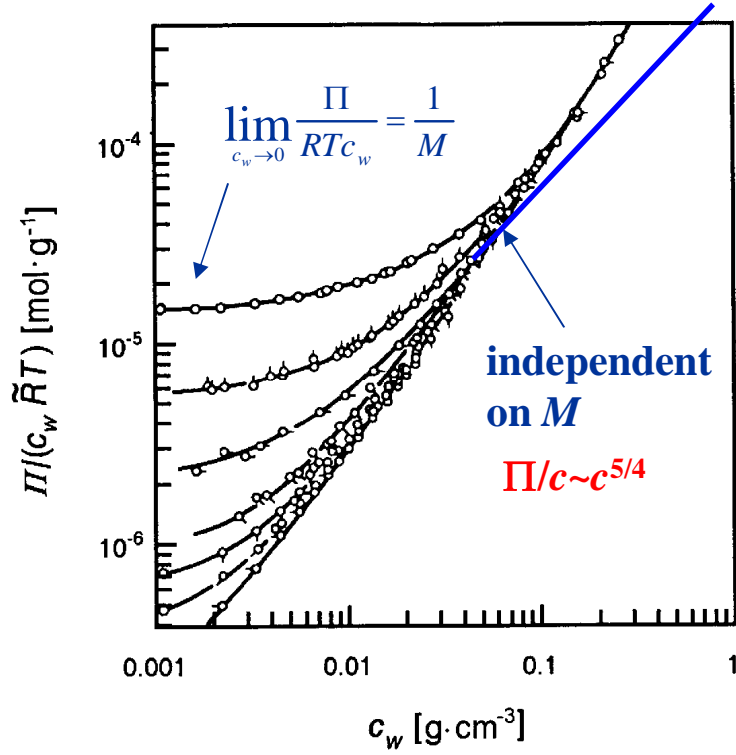


Anomalous phenomenon in Semi-Dilute Polymer Solution

$$\Pi = \frac{RT}{\bar{V}_1} \left[\frac{1}{x} \phi_2 + \left(\frac{1}{2} - \chi \right) \phi_2^2 \right]$$

$$\phi_2 = \frac{c}{\rho_2} \quad \rho_2 = \frac{M}{x \bar{V}_1} \quad \phi_2 = \frac{cx \bar{V}_1}{M}$$

$$\frac{\Pi}{c} = \frac{RT}{\bar{V}_1} \left[\frac{\bar{V}_1}{M} + \left(\frac{1}{2} - \chi \right) \frac{c}{\rho_2^2} \right] = RT \left[\frac{1}{M} + \left(\frac{1}{2} - \chi \right) \frac{c}{\bar{V}_1 \rho_2^2} \right]$$



Osmotic pressure measured for samples of poly(α -methylstyrene) dissolved in toluene (25 °C). Molecular weight vary between $M = 7 \times 10^4$ (uppermost curve) and $M = 7.47 \times 10^6$ (lowest curve). (Noda, I.; et al. *Macromolecules* 1981, 14, 668.)

$$\phi_2 \ll 1$$

$$\phi_2^2 \gg \phi_2 / x$$

$$\Pi/c \sim c^0$$

~~$$\Pi/c \sim c^1$$~~

~~$$\Pi/c \sim c^{5/4} \quad ???$$~~

需要寻找新的理论手段!

高分子链的重要标度指数

$$\langle R_{RW}^2 \rangle \sim N^1 \quad \longrightarrow \quad \Phi(\mathbf{h}, N) = \left(\frac{3}{2\pi Nl^2} \right)^{3/2} \exp\left(-\frac{3\mathbf{h}^2}{2Nl^2} \right)$$

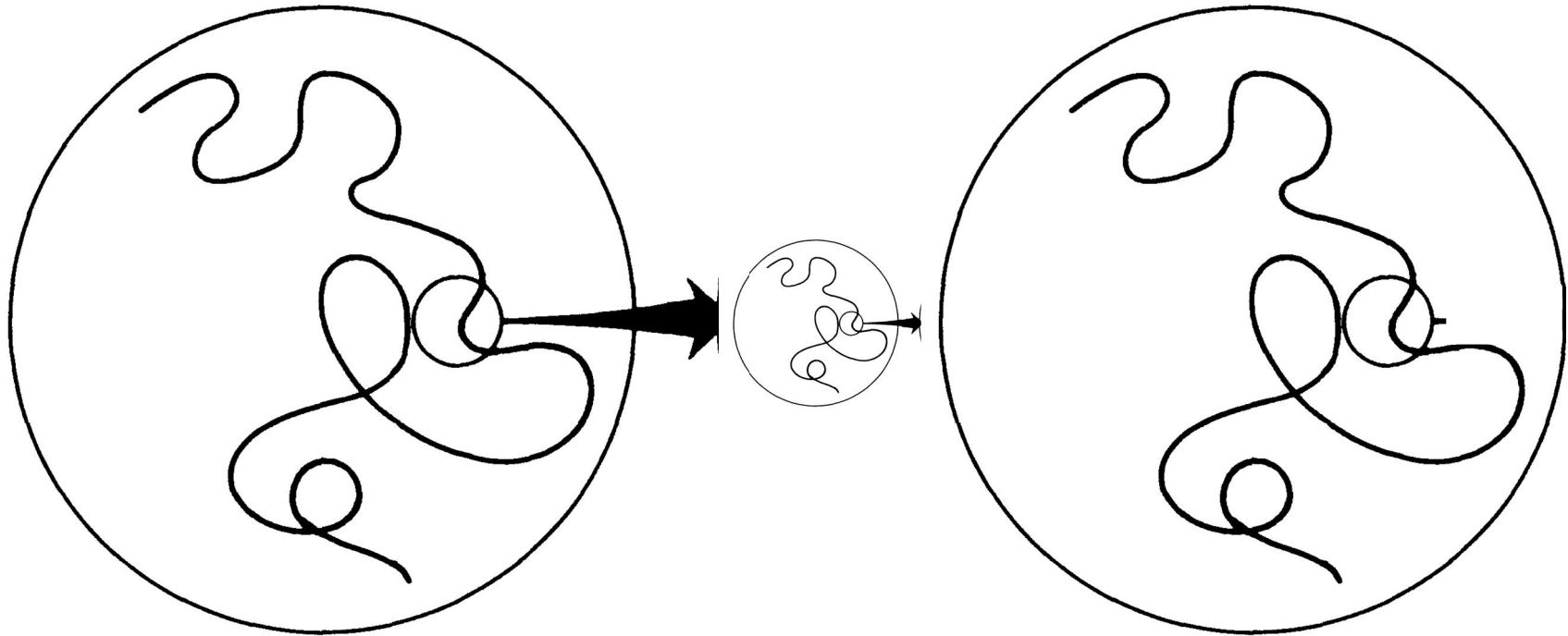
$$\langle R_{SAW}^2 \rangle \sim N^{2\nu} \sim N^{6/5} \quad \longrightarrow \quad ??? \quad \boxed{}$$

高分子的绝大多数性质与 R_g 有关

$$\langle R_g \rangle \sim N^\nu$$

能否利用 R_g 与 N 的指数去估算高分子的一些重要性质？

自相似与标度律-对高斯链模型的补充



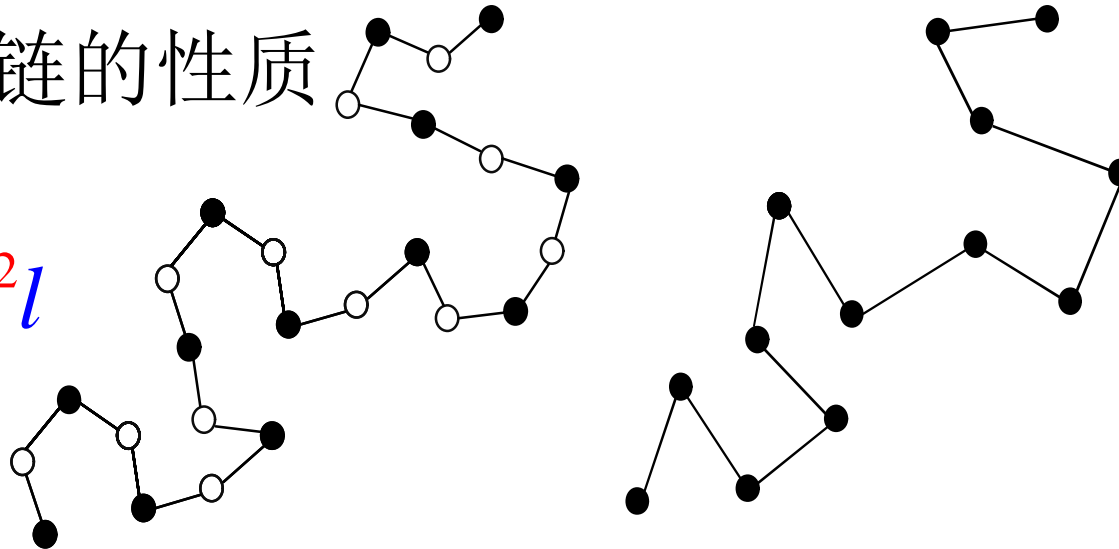
高分子链具有自相似性

如何利用这个自相似性??

3.5 Scaling Law(标度律)- (1) 链的性质

(1a) 理想链的性质

$$h \approx N^{1/2} l$$



$$N \rightarrow N / g \quad l \rightarrow l \sqrt{g}$$

$$h \approx R_g = F(l, N)$$

$$F(l, N) = F(\sqrt{g} l, N / g)$$

标度函数:

$$F(l, N) = \text{const.} \times \sqrt{g} l (N / g)^{a=1/2} = \text{const.} \times \sqrt{N} l$$

(1b) 真实链的性质

$$h \approx N^{\nu} l$$

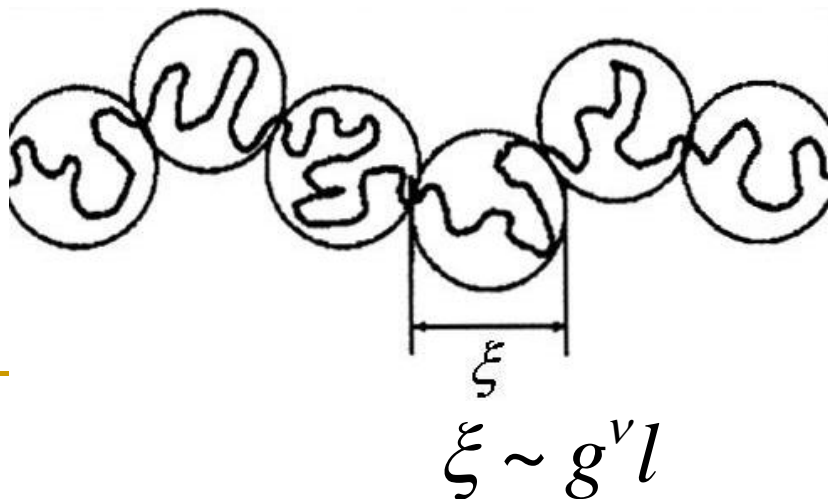
$$N \rightarrow N / g$$

$$l \rightarrow l g^{\nu}$$

$$v-a=0, a=v$$

$$h = F(l g^{\nu}, N / g) = \text{const.} \times l g^{\nu} (N / g)^{a=?} = \text{const.} \times N^{\nu} l$$

Blob Model



Numbers of blobs: $n=N/g$

Energy of each blob \approx

Thermal fluctuation energy $k_B T$

$$h = F(l, N) = F(\xi, N / g)$$

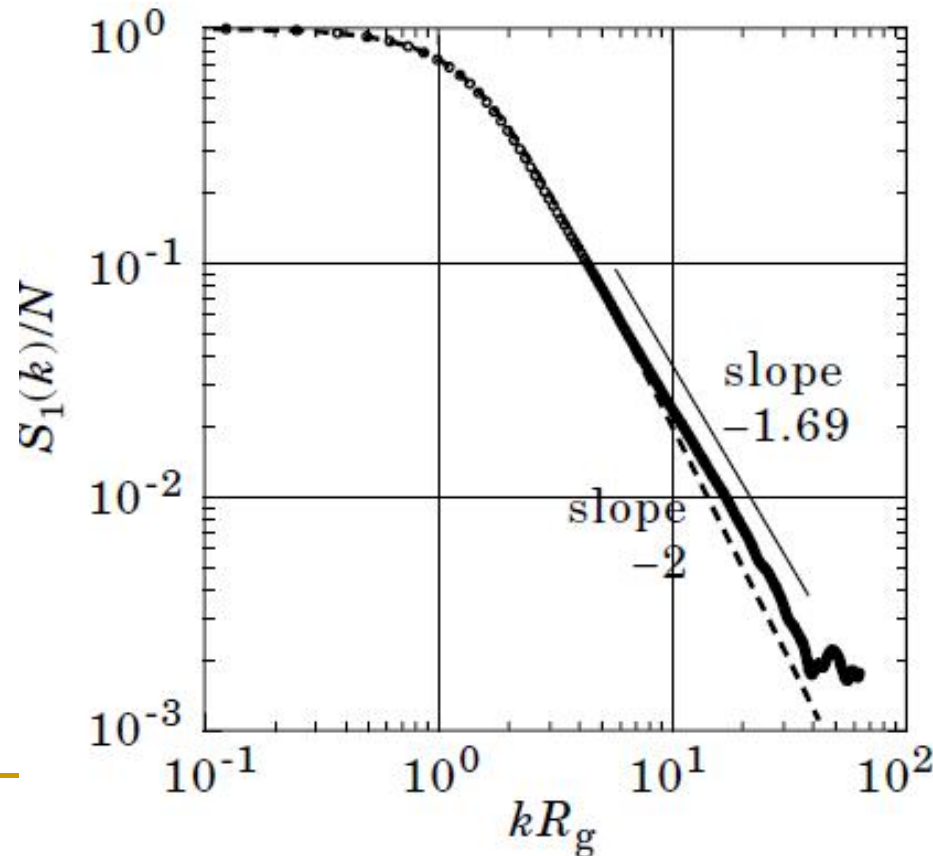
$$G \sim k_B T n = k_B T \frac{N}{g}$$

(2) 高分子链散射函数的标度律

$$g(\mathbf{k}) = Np(\mathbf{k}) = \frac{N}{1 + k^2 \langle R_g^2 \rangle / 2}$$

$$R_g \sim l$$
$$= F(kR_g, N) = F(kl, N)$$

l 链段长度



(2) 高分子链散射函数的标度律

$$g(\mathbf{k}) = \int d\mathbf{r} \exp(-i\mathbf{k} \cdot \mathbf{r}) \Psi(\mathbf{r}) \quad \text{无量纲} \quad \text{散射矢量} \quad k \propto 1/\lambda$$

$$= F(k, l, N) \propto N$$

大的 \mathbf{k} , 小 \mathbf{r} 部分的贡献大

$$g(\mathbf{k}) = F(kl, N) \quad g(\mathbf{k}) \rightarrow g(\mathbf{k}) / g$$

$$F(klg^{\nu}, N/g) = \frac{1}{g} F(kl, N) \quad \text{如果: } g = N$$

$$g(\mathbf{k}) = F(kl, N) = NF(klN^{\nu}, 1) = NF(kR_g)$$

当 k 很大时, 散射函数仅反映了高分子链内部尺度非常小的散射行为在 $kR_g \gg 1$ 时, $g(k)$ 应与 N 无关

$$g(\mathbf{k}) = \text{const.} \times N(kR_g)^a = \text{const.} \times N(klN^{\nu})^a \propto k^a$$

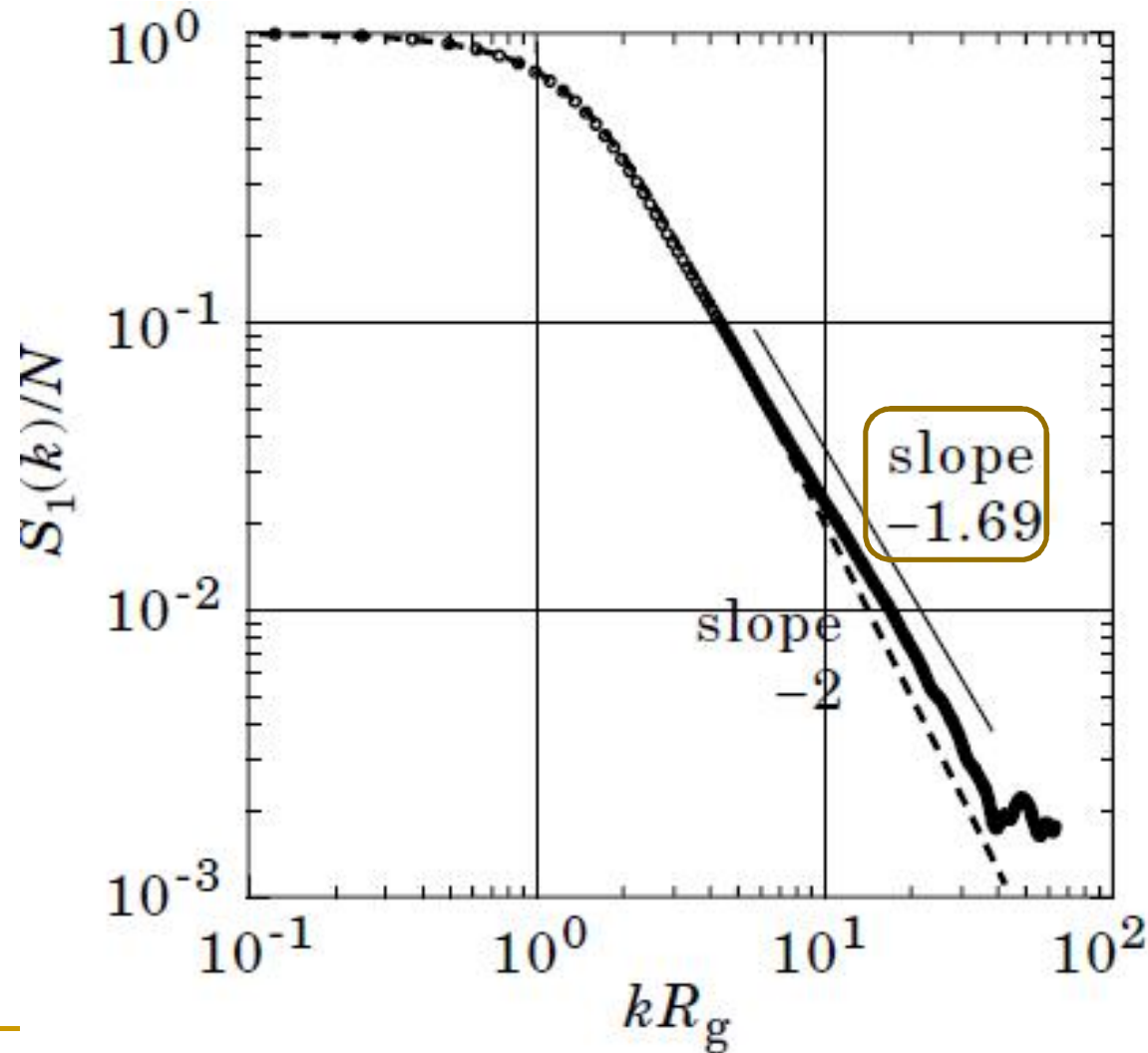
$a\nu + 1 = 0$
 $a = -1/\nu$

高斯链 — $g(\mathbf{k}) = 2N / k^2 \langle R_g^2 \rangle \propto k^{-2}$ $|k|^2 \langle R_g^2 \rangle \gg 1$

$\nu=1/2$	ideal
$\nu=3/5$	real

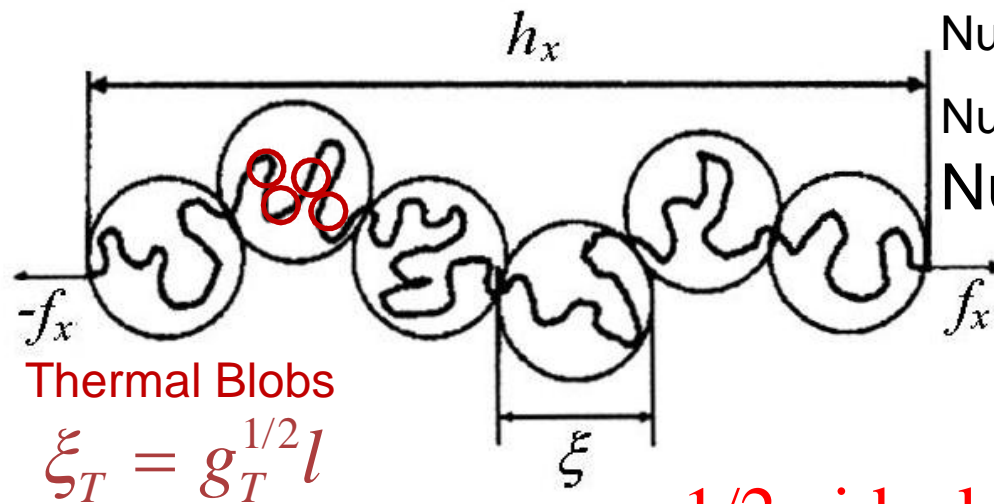
45

Form Factor of a Real Chain



$kR_g \gg 1$
 $p(k) \propto k^{-1/\nu}$
 $\nu = 3/5$

(3) Blob Model - a. Athermal Chain Stretching



Number of Thermal blobs $N_T = N / g_T$
 Number of Thermal Blobs in a large blob: g
 Number of large blobs: $n = N_T / g$
 Energy of one blob \approx thermal blob \approx
 Thermal fluctuation energy $k_B T$
 Total Free Energy: $G \sim k_B T \frac{N_T}{g}$

$\nu = 1/2$ ideal $\nu = 3/5$ athermal

$$\xi \sim g^\nu \xi_T$$

$$h_x \approx \left(\frac{N_T}{g} \right) \xi$$

$$g \sim \frac{(N_T \xi_T)^{1/1-\nu}}{h_x^{1/1-\nu}}$$

$$G \sim k_B T \frac{N_T}{g} \sim k_B T \left(\frac{h}{N_T^\nu \xi_T} \right)^{1/1-\nu}$$

由高斯链:

$$f|_{\nu=0.5} \sim k_B T \frac{h}{N_T \xi_T^2}$$

非高斯链:

$$f|_{\text{athermal}} \sim k_B T \frac{h^{3/2}}{N_T^{3/2} \xi_T^{5/2}}$$

$$f = \frac{\partial G}{\partial h} \sim k_B T \left(\frac{h^\nu}{N_T^\nu \xi_T} \right)^{1/1-\nu}$$

$$\sim k_B T \frac{h^{3/2}}{(N / g_T)^{3/2} \xi_T^{5/2}}$$

$\nu = 3/5$ thermal solution Energy of large blob $\xi \neq$ thermal blob ξ_T

Single-Molecule Elasticity Measurements of the Onset of Excluded Volume in Poly(Ethylene Glycol)

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A polymer must reach a certain size to exhibit significant excluded-volume interactions and adopt a swollen random-walk configuration. We show that single-molecule measurements can sense the onset of swelling by modulating the effective chain size with force: as the force is reduced from a large value, the polymer is first highly aligned, then a Gaussian coil, then finally a swollen chain, with each regime exhibiting a distinct elasticity. We use this approach to quantify the structural parameters of poly(ethylene glycol) and show that they vary in the expected manner with changes in solvent.

DOI: 10.1103/PhysRevLett.107.148301

PACS numbers: 36.20.Ey, 61.25.hp, 82.37.Rs, 87.15.La

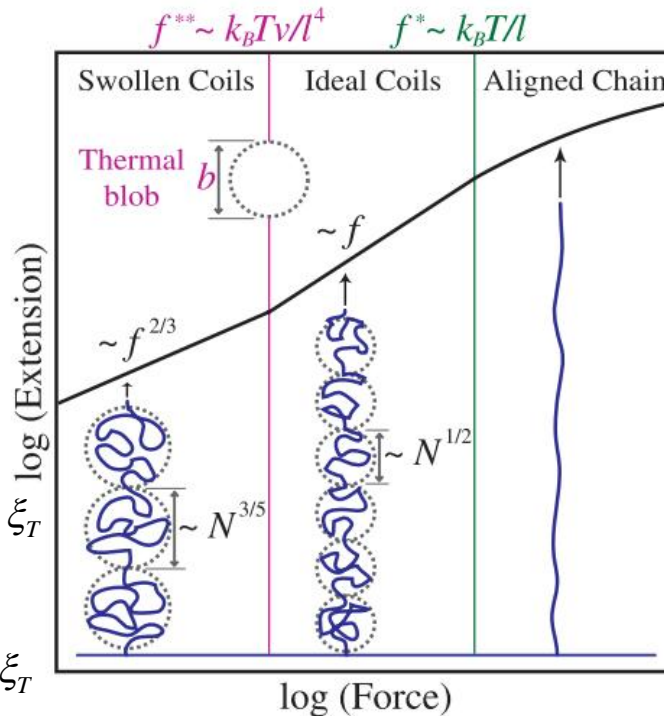
$$f|_{v=0.6} \sim k_B T \frac{h^{3/2}}{(N/g_T)^{3/2} \xi_T^{5/2}}$$

$$h \sim f^{2/3}$$

$$f \sim k_B T \frac{h^{3/2}}{(N/g_T)^{3/2} \xi_T^{5/2}}$$

to

$$f \sim k_B T \frac{h}{(N/g_T) \xi_T^2} \quad h^{**} \sim (N/g) \xi_T$$



$$\xi_T = \left(\frac{u}{l^3} \right)^{-1} l = \frac{l^4}{u}$$

$$f^{**} \sim k_B T / \xi_T$$

$$\xi_T \rightarrow l$$

$$f^* \sim k_B T / l \quad 48$$

(b) 真实链的构象(末端距)分布函数

由自由能与末端距的关系:

$$G \sim k_B T \left(\frac{h}{N^\nu l} \right)^{1/1-\nu}$$

$$\Phi_R(h, N) \sim \exp\left[-\frac{G}{kT}\right] \sim \exp\left[-\alpha \left(\frac{h}{\sqrt{\langle h^2 \rangle}} \right)^{1/1-\nu}\right]$$

$$h > \sqrt{\langle h^2 \rangle} = N^\nu l$$

$$\Phi_R(h, N) \sim \left(\frac{h}{\sqrt{\langle h^2 \rangle}} \right)^\mu \quad \mu = 0.28$$

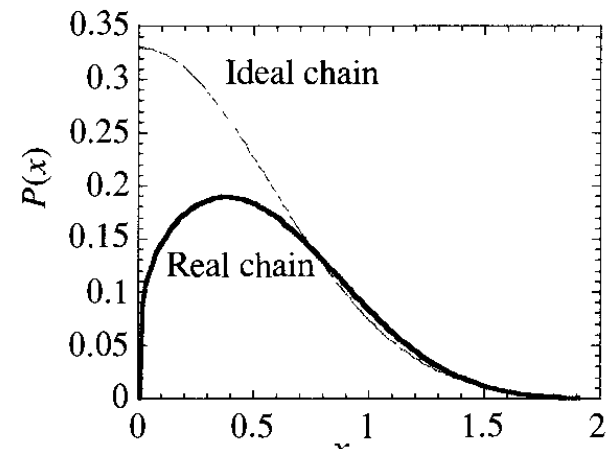
$$h \ll \sqrt{\langle h^2 \rangle}$$

$$\Phi_R(x) = 0.278 x^{0.28} \exp(-1.206 x^{2.5})$$

$$\Phi_I(x) = \left(\frac{3}{2\pi N l^2} \right)^{3/2} \exp\left(-\frac{3h^2}{2N l^2}\right)$$

$$= \left(\frac{3}{2\pi \langle h^2 \rangle} \right)^{3/2} \exp(-1.5x^2)$$

$$x = h / \sqrt{\langle h^2 \rangle}$$

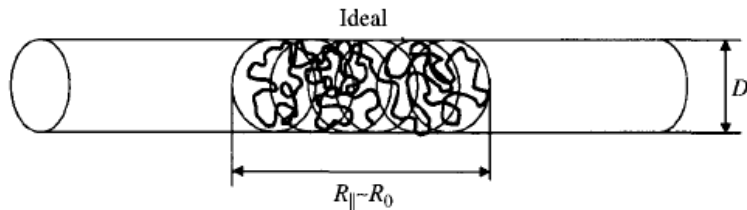


(2) Blob Model – c. Biaxial Compression

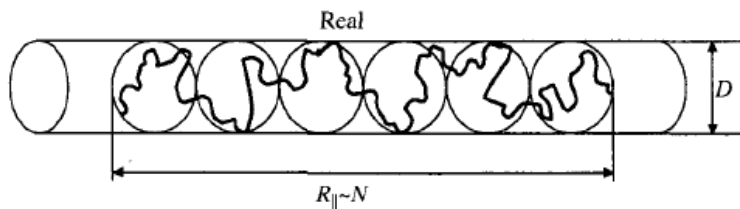
$$D = g^{\nu} l \text{ or } D = g^{\nu} \xi_T$$

$\nu=1/2$ ideal

$\nu=3/5$ athermal



$$R_{||} |_{ideal} \sim \left(\frac{N}{g} \right)^{1/2} \quad D \sim \left(\frac{Nl^2}{D^2} \right)^{1/2} \quad D \approx N^{1/2} l$$

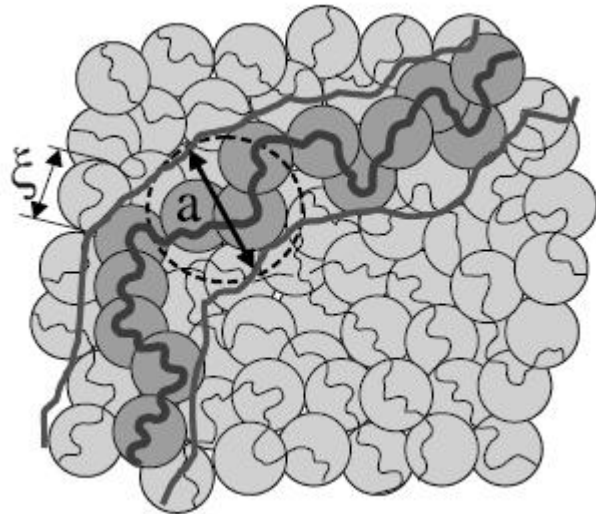
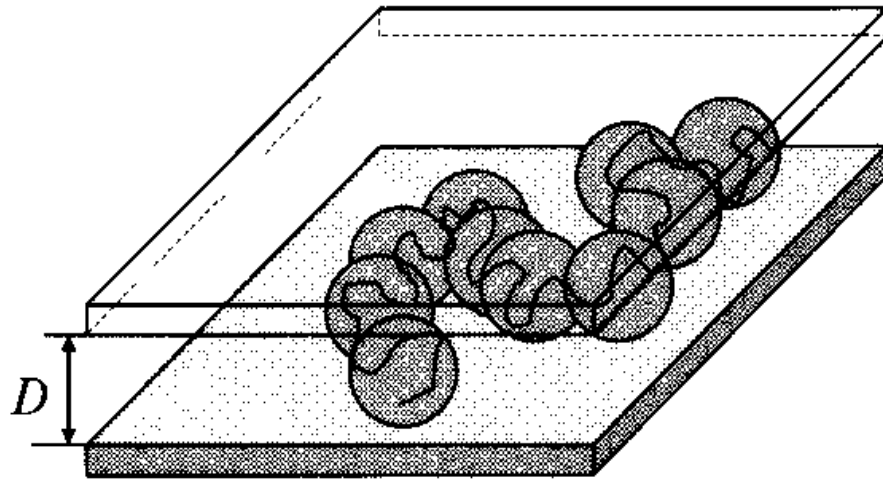


$$R_{||} |_{real} \sim \left(\frac{N}{g} \right) \quad D \sim \left(\frac{Nl^{1/\nu}}{D^{1/\nu}} \right) \quad D \sim \boxed{N} \left(\frac{l}{D} \right)^{2/3}$$

$$G_{conf} |_{ideal} = k_B T \frac{N}{g} = \boxed{k_B T N \left(\frac{l}{D} \right)^2} = k_B T \left(\frac{R_0}{D} \right)^2 \quad R_0 \approx N^{1/2} l$$

$$G_{conf} |_{real} = k_B T \frac{N}{g} = \boxed{k_B T N \left(\frac{l}{D} \right)^{1/\nu}} = k_B T \left(\frac{N^{\nu} l}{D} \right)^{1/\nu} = k_B T \left(\frac{R_r}{D} \right)^{5/3} \quad R_r \approx N^{3/5} l$$

d. Uniaxial compression ??



$$G_{conf} = k_B T \frac{R^2}{Nl^2} = k_B T \frac{R^2}{R_0^2}$$

Entropy of an ideal chain

$$G_{conf, blob} = k_B T \frac{R^2}{(N/g)D^2}$$

Entropy of an ideal blob chain

$$G_{int} = k_B T u \frac{N^2}{R^3}$$

$$u \approx l^3 (1 - 2\chi)$$

$$G_{int, blob} = k_B T D^2 \frac{(N/g)^2}{R^2}$$

Interaction between blobs

$$\frac{\partial (G_{conf, blob} + G_{int, blob})}{\partial R} = 0$$

Answers:

$$R_{real, d} \approx N^{\frac{3}{d+2}} l$$

d : dimensions (空间维度)

$$R_{||} \approx N^{3/4} l$$

$$R_{ideal} \approx N^{\frac{1}{2}} l$$

高分子物理中的理论方法I

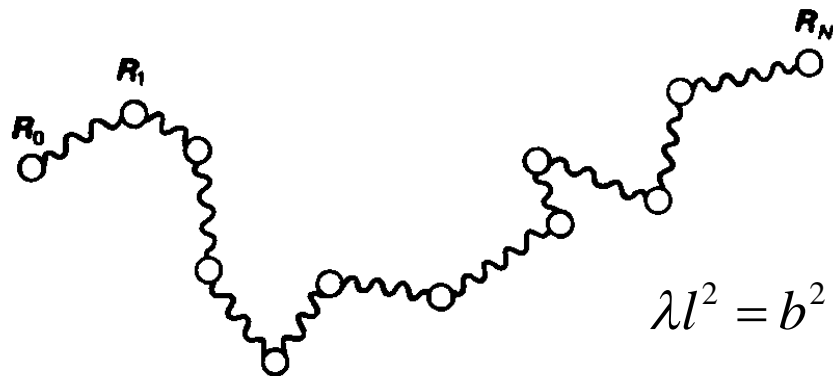
1. 高斯链模型

$$\langle R_{RW}^2 \rangle \sim N^1$$

$$\Phi(\mathbf{h}, N_g) = \left(\frac{3}{2\pi N_g l_g^2} \right)^{3/2} \exp\left(-\frac{3\mathbf{h}^2}{2N_g l_g^2} \right)$$



$$\frac{\partial \Phi(\mathbf{h}, N_g)}{\partial N} = \frac{l_g^2}{6} \frac{\partial^2 \Phi(\mathbf{h}, N_g)}{\partial \mathbf{h}^2}$$



Path Integral(路径积分)
Edward's Minimum Model

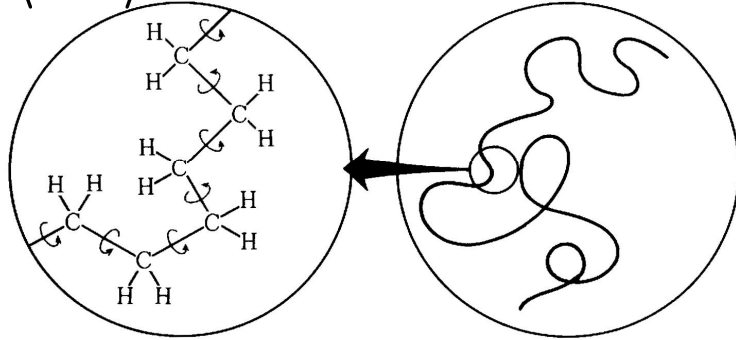
$$\begin{aligned} \Psi(\{\mathbf{h}_i\}) &= \prod_{i=1}^{N_g} \left(\frac{3}{2\pi \lambda l^2} \right)^{3/2} \exp\left(-\frac{3\mathbf{h}_i^2}{2\lambda l^2} \right) \\ &= \left(\frac{3}{2\pi b^2} \right)^{3N_g/2} \exp\left(-\sum_{n=1}^{N_g} \frac{3(\mathbf{R}_i - \mathbf{R}_{i-1})^2}{2b^2} \right) \end{aligned}$$

$$= \text{const} \exp\left[-\frac{3}{2b^2} \int_0^{N_g} \left(\frac{\partial \mathbf{R}_n}{\partial n} \right)^2 dn \right]$$

$\Psi(\{\mathbf{h}_i\}) + \text{interaction energy} \Rightarrow H$ 哈密顿量 \Rightarrow Mean-field Free Energy

高分子物理的主线-高斯链模型

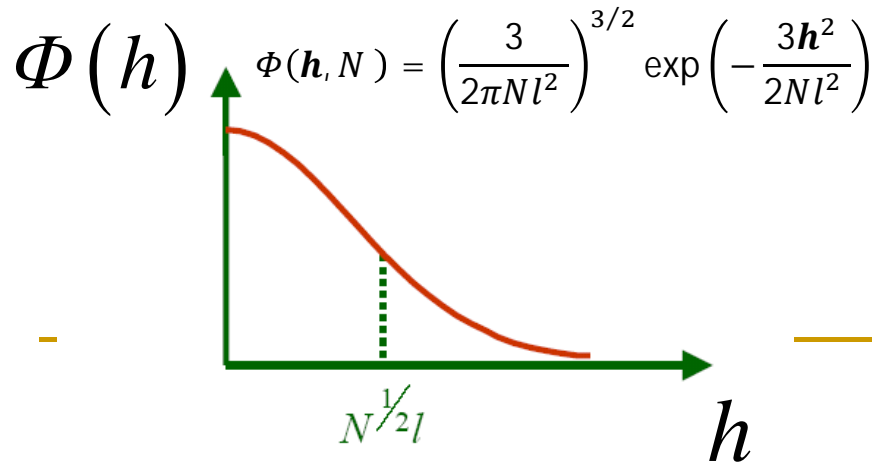
$$\langle R^2 \rangle \sim N^{2\nu} l^2$$



In θ solution:

$$\langle R^2 \rangle_0 = \alpha N l^2 \quad \langle R^2 \rangle_0 = l_e L$$

Gaussian Chain Model



Entropy of Chain Conformations

$$S_{conf}(\mathbf{h}, N_g) = -\frac{3}{2} k_B \frac{h^2}{N_g l^2} + C$$

$\mathbf{h}, \Phi(\mathbf{h}, N)$

Mechanic Properties

$$f = 3k_B T \frac{h}{N l^2}$$

Scattering Theory ($R > \lambda/20$)

$$p(k) = \frac{1}{1 + k^2 \langle R_g^2 \rangle / 2}$$

Scaling Concept & Blob Model

$$G \sim k_B T \frac{N}{g}$$

高分子物理中的理论方法II

标度律是高斯链模型的补充，
尤其适用于真实链

$$\langle R_{\text{SAW}} \rangle \sim N^{\nu} \sim N^{3/5}$$

根据变量 (N, l, k) 和量纲分析设计标度函数

利用降低分辨率时的标度不变性和量纲之间的关系，考察物理性质与变量的关联

结合blob model考察物理性质与变量的关联

2 Unique Features of Polymers

Thermodynamics:

(1) Large Spatial Extent

(2) Connectivity

a. Tacticity – 立构性 c. Flexible vs. Rigid

b. Polymer Topology

d. Multiple Conformations (Entropy)

(3) Multiple Interactions (Enthalpy)

Dynamics:

(4) Entanglement

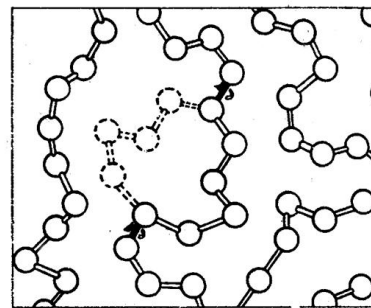
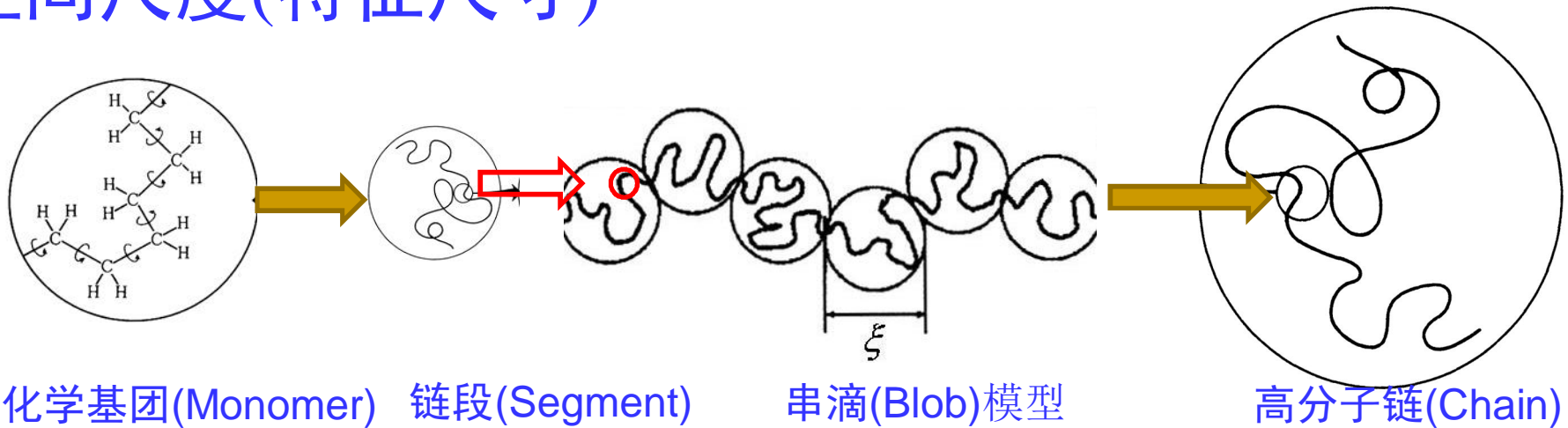
(5) Responsive Molecules

a. Large-scale Relaxation Time Spectrum

b & c . Temp, Rate and Time Dependent Behavior

Spatial Extent & Connectivity

空间尺度(特征尺寸)



多链聚集态

Entropy

Multiple Confirmations (Entropy)

$$\text{A Chain} \quad S_{conf} \approx -k_B \frac{R^2}{Nl^2} \quad \text{A Blob Chain} \quad S_{conf} \approx -k_B \frac{R^2}{(N/g)\xi^2}$$

Flory-Huggins Entropy of Mixing for Multi Chains

$$\Delta S_{mixing} = -k_B [N_1 \ln \phi_1 + N_2 \ln \phi_2] = -k_B \frac{V_m}{V_s} \left[\frac{\phi_1}{x_1} \ln \phi_1 + \frac{\phi_2}{x_2} \ln \phi_2 \right]$$

Enthalpy

Multiple Interactions (Enthalpy)

Two-body interaction

within a Blob $\bar{E} \approx k_B T |u| \frac{g_T^2}{\xi_T^3}$

In a 3d Chain $H_{2,int} = k_B T u \frac{N^2}{R^3}$ In a 3d Blob Chain $H_{2,int} = k_B T \xi^3 \frac{(N/g)^2}{R^3}$

$$u = v_c (1 - 2\chi) \approx v_c \tau \quad v_c \approx l^3$$

2d chain $H_{2,int} = k_B T u \frac{N^2}{R^2}$ 2d Blob Chain $H_{2,int} = k_B T \xi^2 \frac{(N/g)^2}{R^2}$

$$u = s_c (1 - 2\chi) \approx s_c \tau \quad s_c \approx l^2$$

Flory-Huggins Enthalpy of Mixing for Multi Chains

$$\Delta H_{mixing} = \frac{V_m}{V_s} k_B T \chi \phi_1 \phi_2 = k_B T \chi x N_2 \phi_1$$

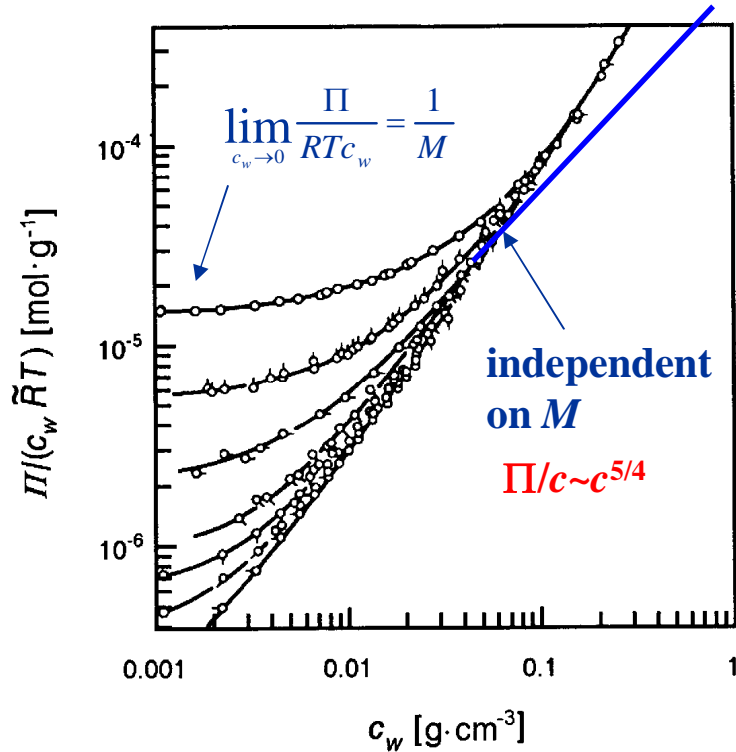
Three-body 3d $H_{3,int} / k_B T = w \phi_2^3 R^3 = w \frac{N^3}{R^6}$

3.6 Semi-dilute Solutions of Polymers

$$\Pi = \frac{RT}{\bar{V}_1} \left[\frac{1}{x} \phi_2 + \left(\frac{1}{2} - \chi \right) \phi_2^2 \right]$$

$$\phi_2 = \frac{c}{\rho_2} \quad \rho_2 = \frac{M}{x\bar{V}_1} \quad \phi_2 = \frac{cx\bar{V}_1}{M}$$

$$\frac{\Pi}{c} = \frac{RT}{\bar{V}_1} \left[\frac{\bar{V}_1}{M} + \left(\frac{1}{2} - \chi \right) \frac{c}{\rho_2^2} \right] = RT \left[\frac{1}{M} + \left(\frac{1}{2} - \chi \right) \frac{c}{\bar{V}_1 \rho_2^2} \right]$$



Osmotic pressure measured for samples of poly(α -methylstyrene) dissolved in toluene (25 °C). Molecular weight vary between $M = 7 \times 10^4$ (uppermost curve) and $M = 7.47 \times 10^6$ (lowest curve). (Noda, I.; et al. *Macromolecules* 1981, 14, 668.)

$$\phi_2 \ll 1$$

$$\phi_2^2 \gg \phi_2 / x$$

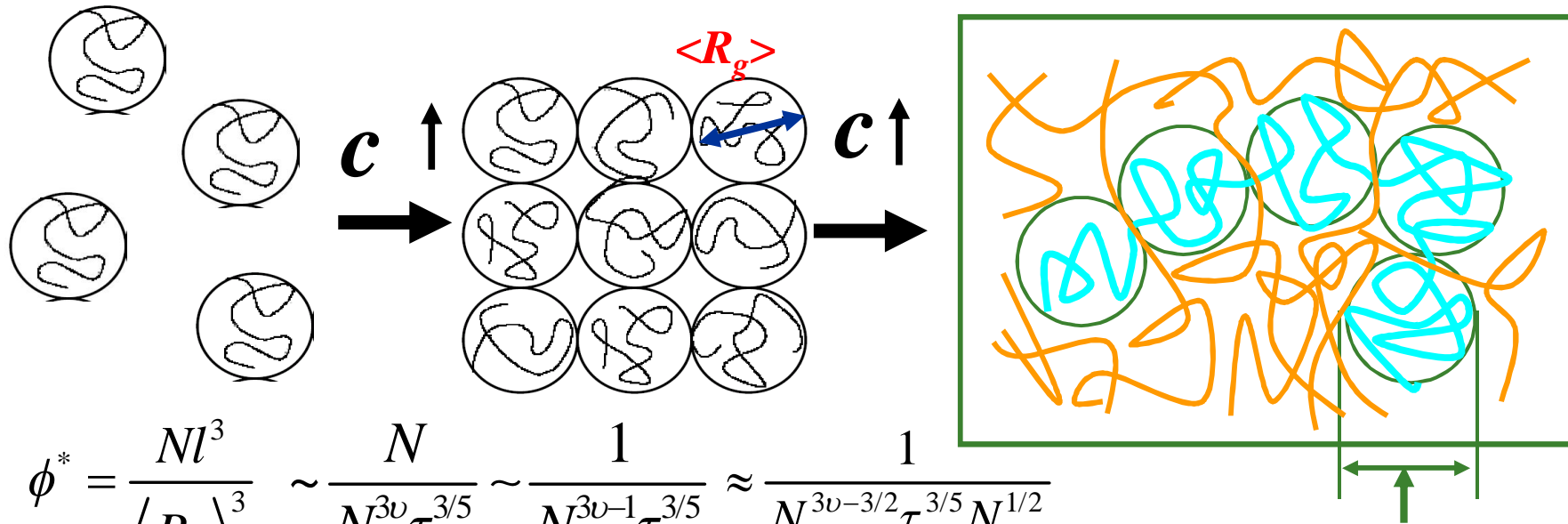
$$\Pi/c \sim c^0$$

~~$$\Pi/c \sim c^1$$~~

~~$$\Pi/c \sim c^{5/4}$$~~

(1) overlap concentration c^*

dilute $c: < c^*$ **Overlap concentration: $c = c^*$** Semi-dilute regime: $c > c^*$



$$\phi^* = \frac{Nl^3}{\langle R_g \rangle^3} \sim \frac{N}{N^{3\nu} \tau^{3/5}} \sim \frac{1}{N^{3\nu-1} \tau^{3/5}} \approx \frac{1}{N^{3\nu-3/2} \tau^{3/5} N^{1/2}}$$

$$\approx \frac{1}{\alpha^3 N^{1/2}} \quad \boxed{\sim N^{-4/5} \tau^{-3/5}} \quad c^* = \phi^* \rho_2$$

Apparent correlation length
 (表观相关长度) $R_g > \xi_{app} > \xi_T > l$

For good solvent, $\nu = 3/5$

$$\tau = 1 - 2\chi = 1 - \frac{\chi}{1/2} = \left(1 - \frac{T_\theta}{T}\right) \quad \boxed{R_g \propto N^\nu (1 - 2\chi)^{1/5} \quad l = N^\nu \tau^{1/5} l} \quad \alpha = \frac{\langle R_g \rangle}{\langle R_0 \rangle} = N^{\nu-1/2} \tau^{1/5}$$

(2) Osmotic pressure of semi-dilute solution

Van't Hoff relation of osmotic pressure $\frac{\Pi}{c} \approx \frac{RT}{M} f(c)$

$$\Pi = RT \left[\frac{c}{M} + \left(\frac{1}{2} - \chi \right) \frac{c^2}{\bar{V}_1 \rho_2^2} \right] \quad \begin{array}{l} \text{osmotic pressure} \\ \text{from Flory-Huggins} \\ \text{Theory} \end{array} \quad \rho_2 \approx \frac{M}{x \bar{V}_1} \quad \bar{V}_1 = \tilde{N} v_c$$

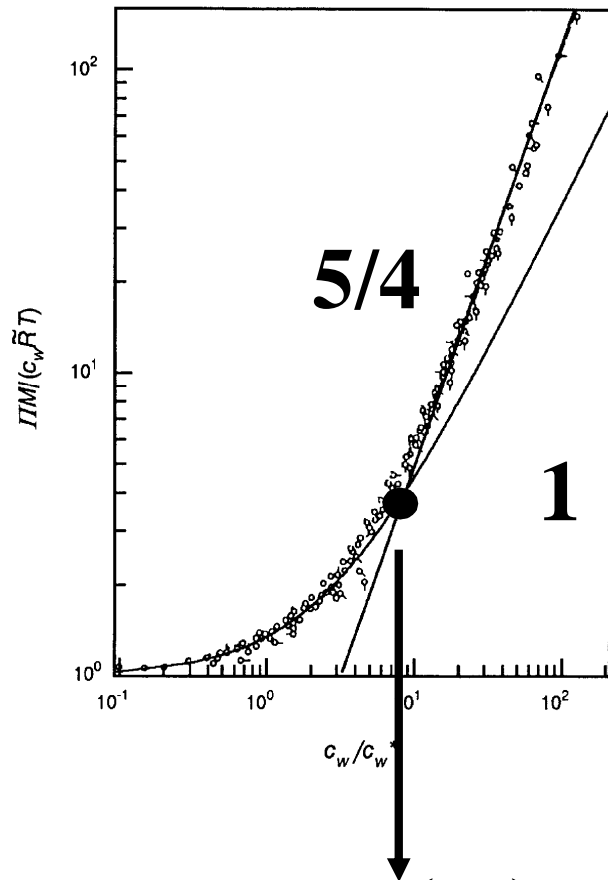
$$= RT \left[\frac{c}{M} + \left(\frac{1}{2} - \chi \right) \frac{x^2 \bar{V}_1}{M^2} c^2 \right] = RT \left[\frac{c}{M} + \frac{c^2}{M^2} \left(\frac{1}{2} - \chi \right) \tilde{N} v_c x^2 \right] \quad u = v_c (1 - 2\chi)$$

$$= RT \left[\frac{c}{M} + \tilde{N} \left(\frac{c}{M} \right)^2 x^2 \frac{u}{2} \right] = RT \left[\frac{c}{M} + \tilde{N} \left(\frac{c}{M} \right)^2 u \sum_{i=1}^x i \right] \quad \sum_{i=1}^x i = \frac{x^2}{2}$$

$$\approx RT \left[\frac{c}{M} + \left(\frac{c}{M} \right)^2 \tilde{N} R_g^3 \right] = RT \frac{c}{M} \left[1 + c \frac{\tilde{N} R_g^3}{M} + \dots \right] \quad c^* = \frac{M}{R_g^3}$$

$$= RT \frac{c}{M} \left[1 + B \left(\frac{c}{c^*} \right) + B' \left(\frac{c}{c^*} \right)^2 + \dots \right] \quad \boxed{\Pi = \frac{c}{M} RT f \left(\frac{c}{c^*} \right)} = \frac{c}{M} RT \left(\frac{c}{c^*} \right)^m$$

Scaling Law of semi-dilute solution



➤ Osmotic pressure:

$$\Pi = \frac{c}{N} k_B T \left(\frac{c}{c^*} \right)^m = \frac{c}{N} k_B T \quad (c = c^*)$$

$$c^* \sim N^{1-3\nu} = \frac{c}{N} k_B T c^m N^{m(3\nu-1)} \quad (c \geq c^*)$$

In semi-dilute regime, Π is independent on N :

$$m(3\nu - 1) - 1 = 0$$

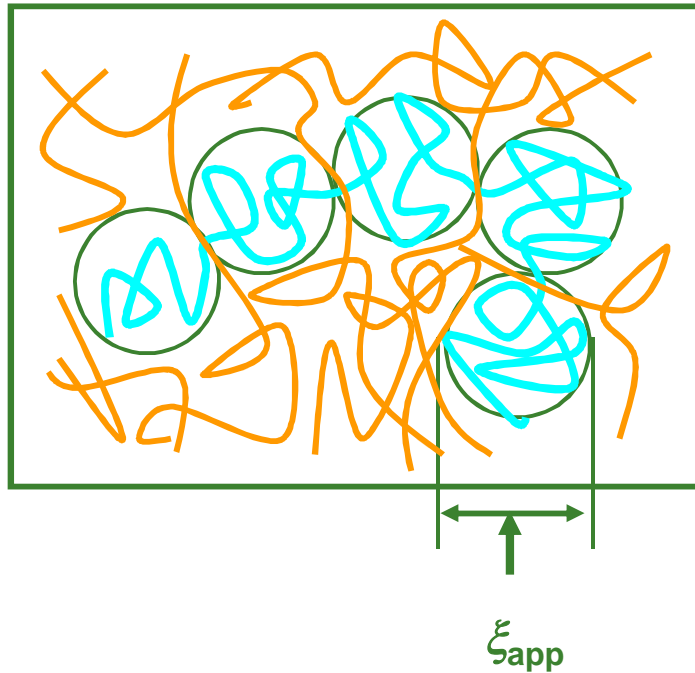
For good solvent, $\nu = 3/5$, therefore $m = 5/4$.

$$\Pi = \frac{c}{N} k_B T f \left(\frac{c}{c^*} \right)$$

$$\Pi \propto c^{1+m} \propto c^{9/4}$$

$$c^2 < \Pi < c^3$$

(3) Apparent correlation length ξ_{app} :



$$\xi_{app} \propto N^\nu l \tau^{1/5} \left(\frac{c}{c^*} \right)^m \quad \propto R_g = N^\nu l \quad (c = c^*)$$

$$\propto N^\nu c^m N^{m(3\nu-1)} \tau^{(1+3m)/5} l \quad (c \geq c^*)$$

$$c^* \propto N^{1-3\nu} \tau^{-3/5}$$

ξ_{app} is independent on N :

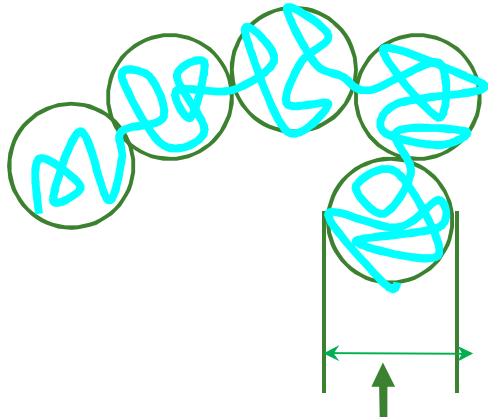
$$\nu + m(3\nu - 1) = 0$$

For good solvent, $\nu = 3/5$,
therefore $m = -3/4$.

$$\xi_{app} = R_g f \left(\frac{c}{c^*} \right)$$

$$\xi_{app} \propto c^{-3/4} \tau^{-1/4} l$$

(4) Polymer Shapes in Semi-dilute Solutions



$$\xi_{app} \sim c^{-3/4} \tau^{-1/4} l$$

blob model:

由 N/g 个串滴单元组成的理想链

$$\langle R_g^2 \rangle = (N / g) \xi_{app}^2$$

串滴内- 由 g 个单元组成的扩张(良溶剂下)的短链

$$\langle \xi_{app}^2 \rangle \sim g^{6/5} l^2 \tau^{2/5}$$

串滴内有 g 个链段单元, 串滴数 N/g , 每个串滴大小 ξ_{app}

$$\xi_{app} \sim g^{3/5} \tau^{1/5} l$$

$$\longrightarrow c \sim gl^3 / \xi_{app}^3$$

证明串滴内外浓度均匀

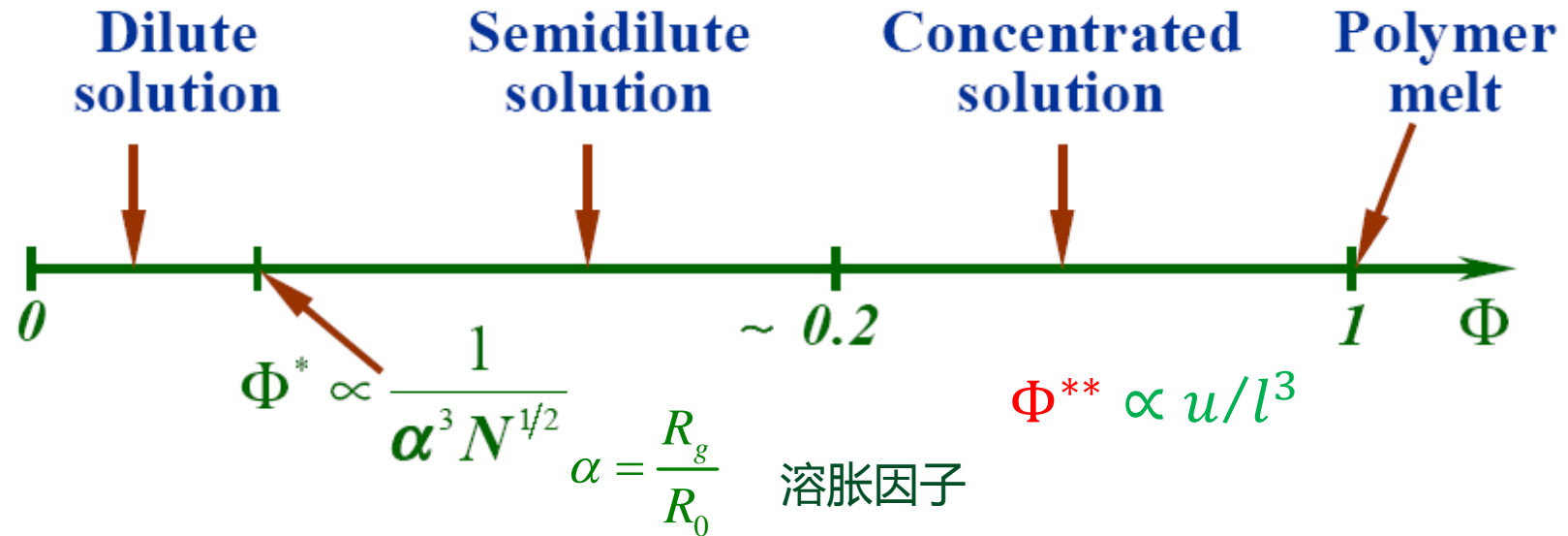
$$\xi_{app} \sim c^{-3/4} \tau^{-1/4} l$$

$$\xi_{app} \sim g^{3/5} \tau^{1/5} l$$

$$g \sim \xi_{app}^{5/3} \tau^{-1/3} \sim c^{-5/4} \tau^{-3/4}$$

$$\langle R_g^2 \rangle_{\text{semi-dilute}} \sim \frac{N}{g} \xi_{app}^2 \sim \frac{N}{c^{-5/4}} c^{-6/4} l^2$$

$$\langle R_g^2 \rangle_{\text{semi-dilute}} \sim N c^{-1/4} \tau^{1/4} l^2 \text{ Gaussian Chain}$$



$$\xi_{\text{app}} \gg R_g$$

$$\xi_{\text{app}} \leq R_g$$

$$\xi_{\text{app}} \sim u \ll R_g$$

$$\langle R_g^2 \rangle_{\text{dilute}} \sim N^{2\nu}$$

$$\langle R_g^2 \rangle_{\text{semi-dilute}} \sim Nc^{-1/4}$$

$$\langle R_g^2 \rangle_{\text{concentrated}} \sim N$$

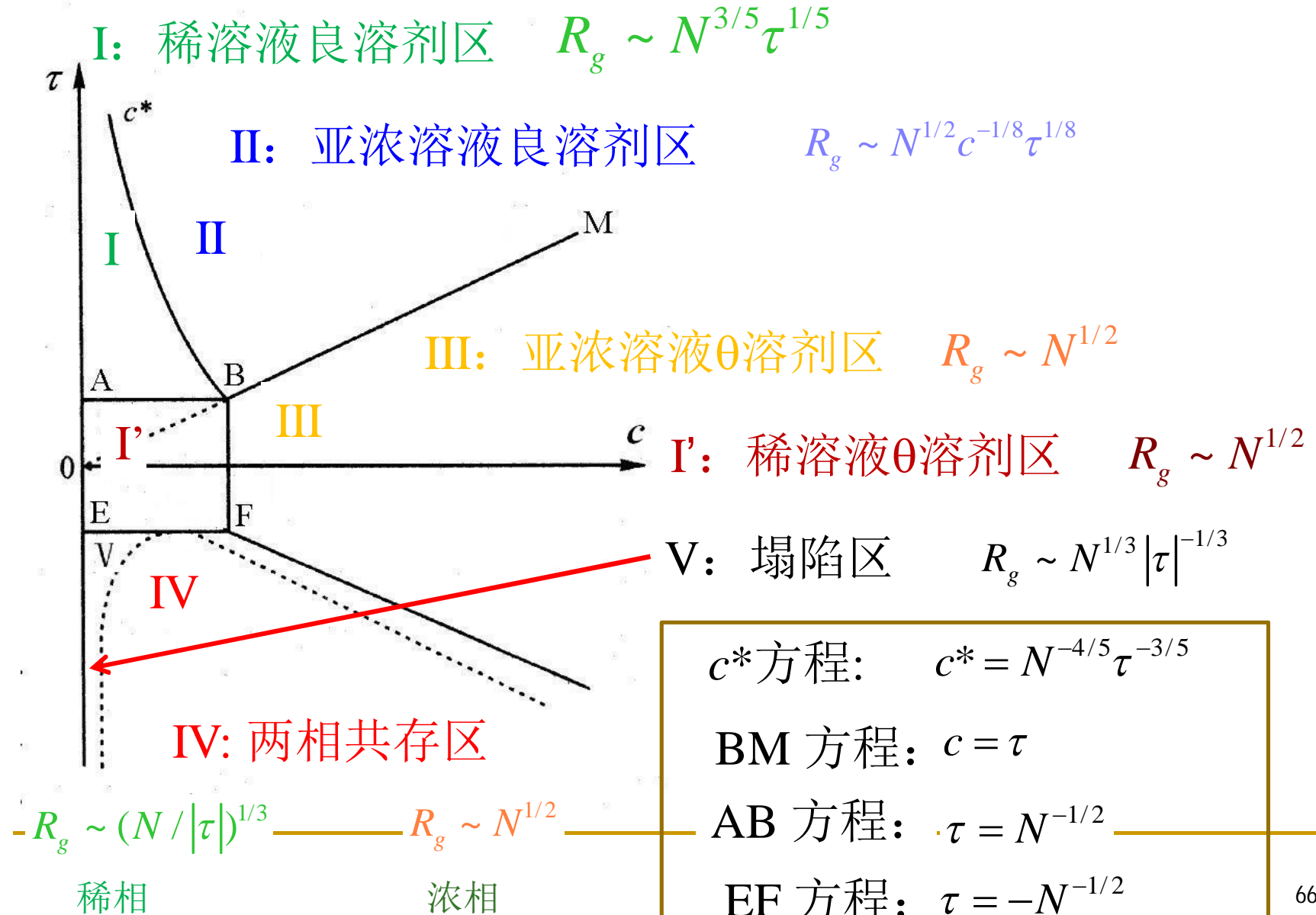
The presence of monomers from the other chains begins to “screen” (屏蔽) the intramolecular excluded volume interactions.

实质

亚浓溶液: 大串滴在溶液中的分布达到均匀, 链段分布未达均匀

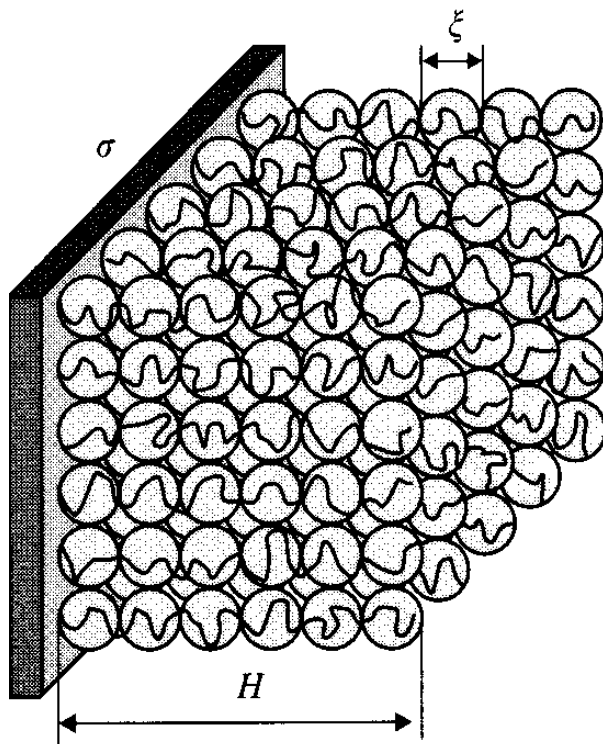
浓溶液: 小串滴在溶液中的分布完全均匀

(5) Regions of the Polymer-Solvent Phase Diagram



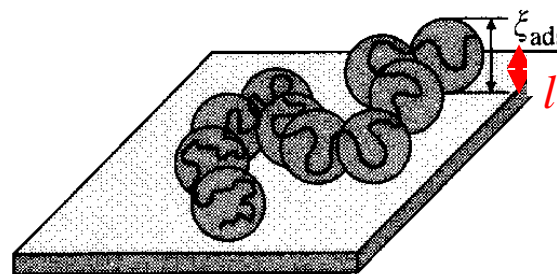
Other Interesting Topics:

Grafted Layer

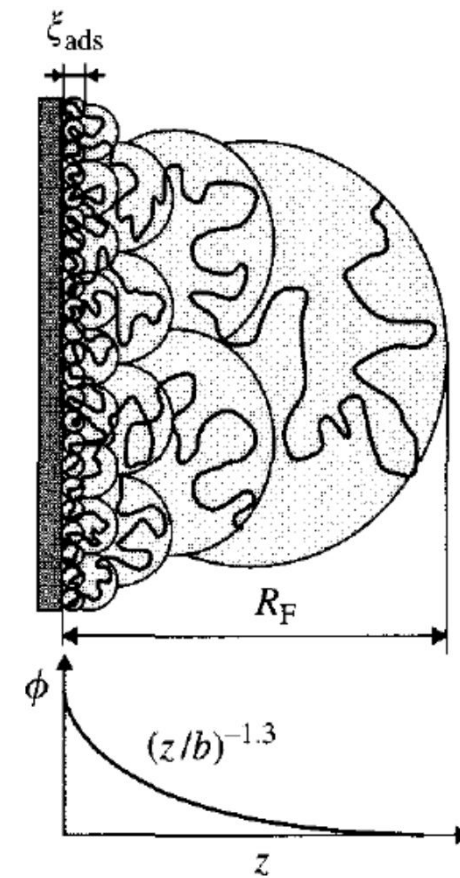


Adsorption:

from Single Chain



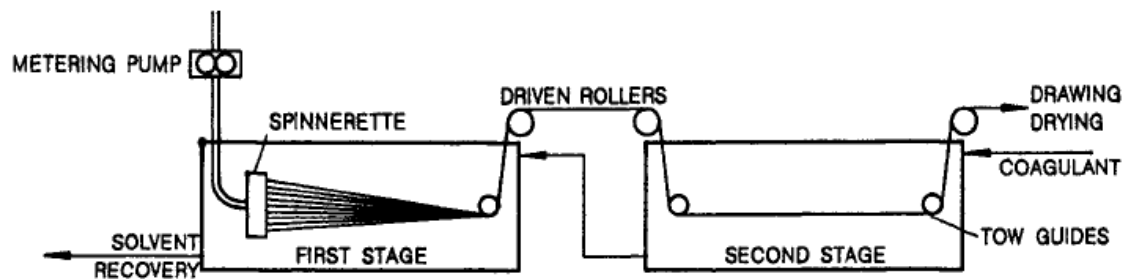
to Multichain



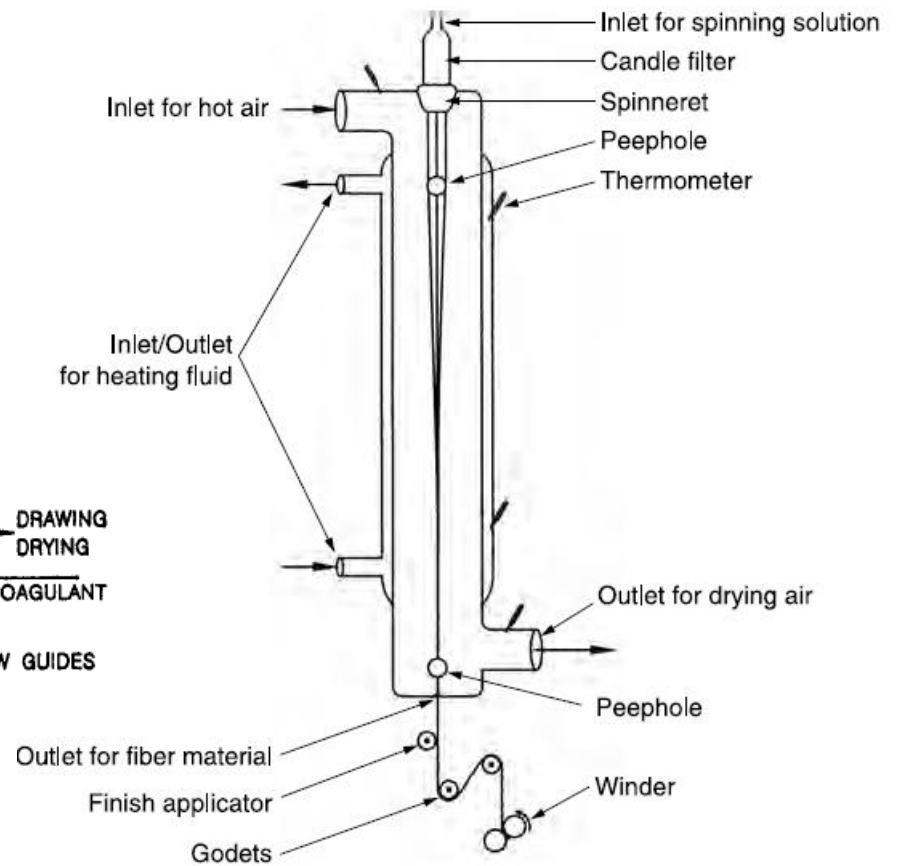
(6) Concentrated Solutions

1. Polymer-Plasticizer
2. Spinning Solution
3. Gel

Fiber Spinning



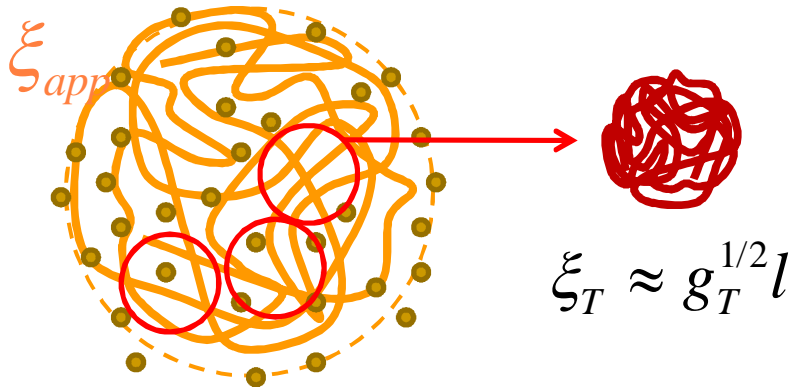
Wet Spinning



Dry Spinning

(6) Concentrated Polymer Solutions

Concentrated regime c^{**}



$$R \propto \xi_T \left(\frac{N}{g_T} \right)^{3/5} \approx g_T^{1/2} \left(\frac{N}{g_T} \right)^{3/5} l = g_T^{-1/10} N^{3/5} l$$

$$= N^{3/5} \left(\frac{u}{l^3} \right)^{1/5} l$$

$$u \approx v_c (1 - 2\chi) = v_c \tau$$

$$v_c \approx l^3$$

$$g_T \approx \left(\frac{u}{l^3} \right)^{-2}$$

$$\xi_T \approx \left(\frac{u}{l^3} \right)^{-1} \quad l \approx \tau^{-1} l \quad \bar{E} \approx k_B T g_T^2 \frac{|u|}{\xi_T^3} \approx k_B T$$

Dilute

$$c < c^*$$

$$\xi_{app} \gg R_g$$

Semi-dilute

$$c > c^*$$

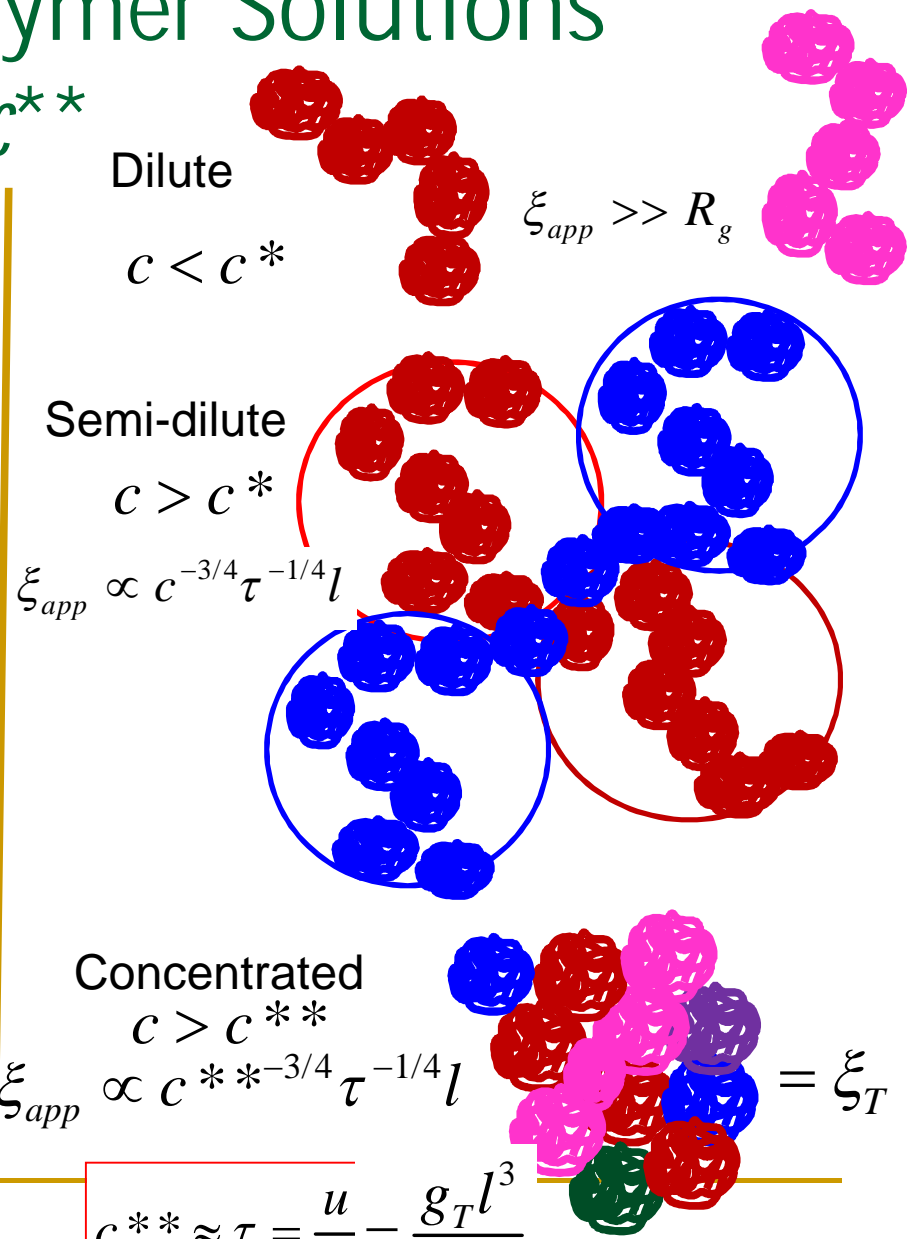
$$\xi_{app} \propto c^{-3/4} \tau^{-1/4} l$$

Concentrated

$$c > c^{**}$$

$$\xi_{app} \propto c^{** -3/4} \tau^{-1/4} l = \xi_T$$

$$c^{**} \approx \tau = \frac{u}{l^3} = \frac{g_T l^3}{\xi_T^3}$$



(7) Polymer Melts

Polymer A + Solvent B

$$\Pi = \frac{kT}{v_c} \left[\frac{\phi_A}{N_A} + (1-2\chi) \frac{\phi_A^2}{2} + \dots \right]$$

$c_A = \phi_A / v_c$ 单体A的质量浓度

Excluded Volume

$$\Pi = kT \left[\frac{c_A}{N_A} + (1-2\chi) v_c \frac{c_A^2}{2} + \dots \right]$$

$$u = v_c (1-2\chi) \approx l^3 (1-2\chi)$$

Polymer A + Polymer B

$$\Pi = kT \left[\frac{c_A}{N_A} + \left(\frac{1}{N_B} - 2\chi \right) v_c \frac{c_A^2}{2} + \dots \right]$$

$$u = v_c \left(\frac{1}{N_B} - 2\chi \right)$$

$$\chi = 0$$

$$u = \frac{v_c}{N_B} \approx \frac{l^3}{N_B}$$



$$\xi_T \approx l g_T^{1/2}$$

$$\bar{E} \approx k_B T g_T^2 \frac{u}{\xi_T^3}$$

$$\approx k_B T \frac{u}{l^3} \frac{g_T^2}{g_T^{3/2}} \approx k_B T$$

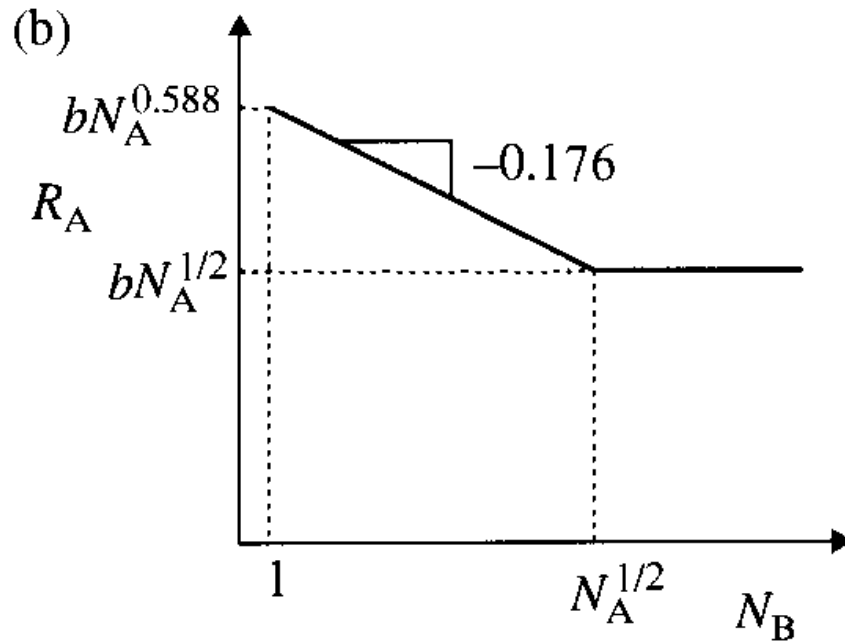
$$g_T \approx \frac{l^6}{u^2} \approx N_B^2$$

$$\xi_T \approx l g_T^{1/2} \approx l N_B$$

Polymer Chain in Melts

串滴并非像亚浓溶液那样处于随机高斯分布，而是由于短B链(溶剂)的存在具有体积排斥效应

$$R_A \approx \xi_T \left(\frac{N_A}{g_T} \right)^{\nu} = l N_B \left(\frac{N_A}{N_B^2} \right)^{\nu} = l N_A^{1/2} \left(\frac{N_A}{N_B^2} \right)^{\nu-1/2} \quad \nu = \frac{3}{5}$$



Overlap parameter P

$$3D \quad P = \frac{R_A^3}{Nl^3} = \frac{N^{3/2}l^3}{Nl^3} = \sqrt{N}$$

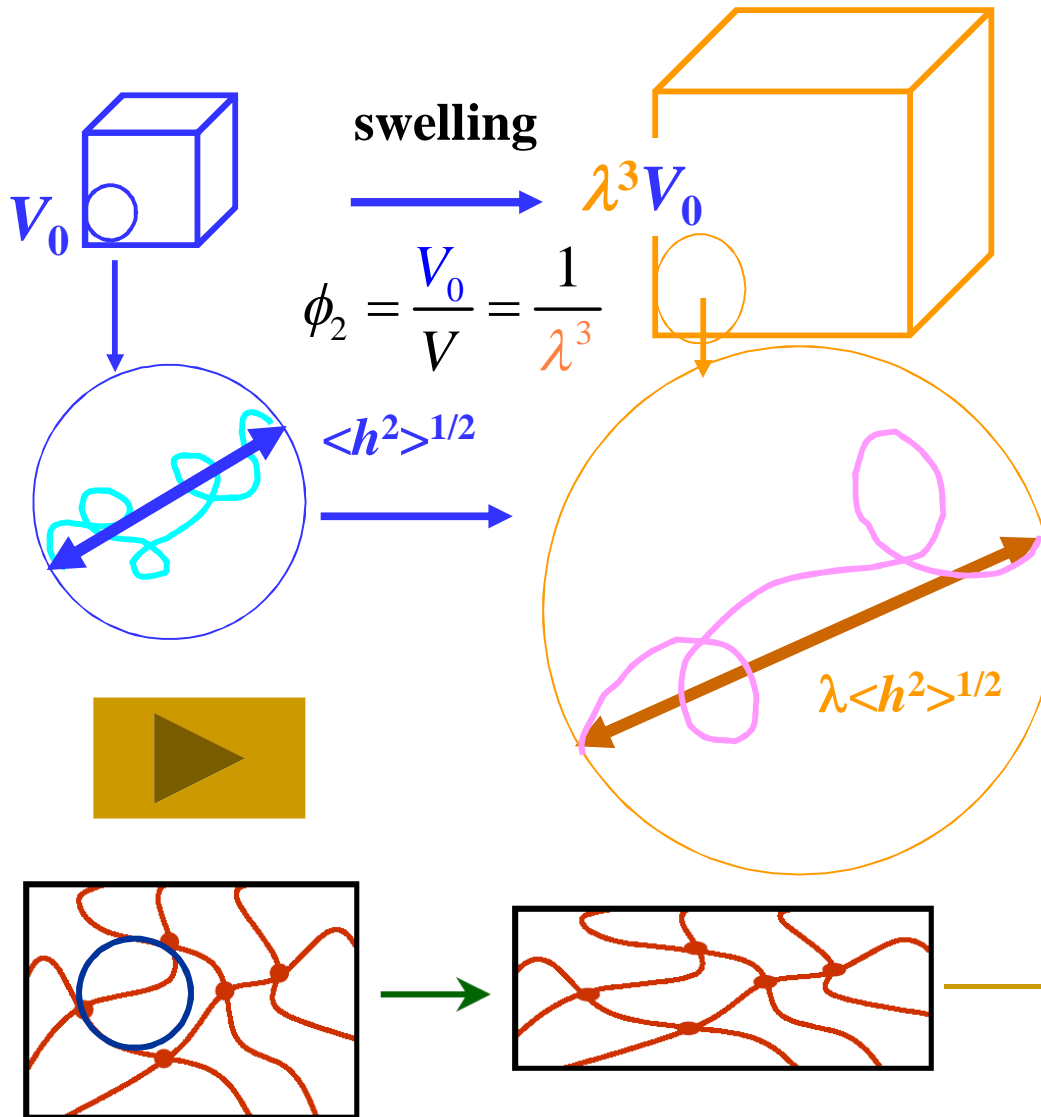
链与链之间发生强烈交叠

$$2D \quad P \approx \frac{R^2}{Nl^2} = \frac{Nl^2}{Nl^2} = 1$$

两维链之间没有交叠

Flory 猜测的熔体中链呈排斥体积被屏蔽的无扰状态完全正确!

3.7 Flory-Huggins free energy of a gel



$$\Delta F = \Delta F_{mixing} + \Delta F_{elastic}$$

$$\Delta F_{mixing} = RT [n_1 \ln \phi_1 + n_2 \ln \phi_2 + \chi n_1 \phi_2]$$

$$S = k \ln \Omega \sim k \ln \Phi(\mathbf{R}, N)$$

$$\Delta F_{elastic} = -T \Delta S_{elastic}$$

$$= NkT \left(\frac{3}{2h_0^2} \right) (\lambda^2 \bar{x}^2 + \lambda^2 \bar{y}^2 + \lambda^2 \bar{z}^2)$$

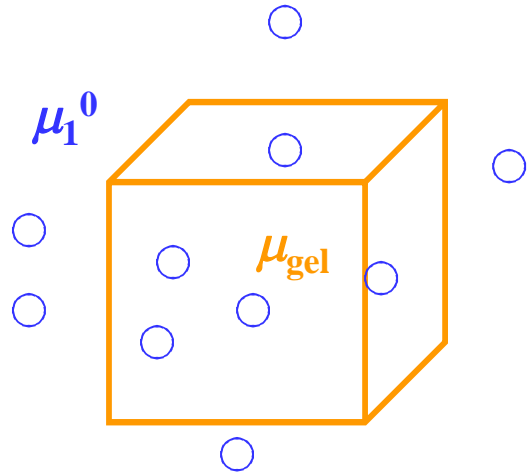
$$- NkT \left(\frac{3}{2h_0^2} \right) (\bar{x}^2 + \bar{y}^2 + \bar{z}^2)$$

$$= \frac{1}{2} NkT (3\lambda^2 - 3) \quad \bar{x}^2 = \bar{y}^2 = \bar{z}^2 = \frac{1}{3} h_0^2$$

$$N = \frac{MN / \tilde{N} / V_0}{M} V_0 \tilde{N} = \frac{\rho_2}{\bar{M}_c} V_0 \tilde{N}$$

$$\Delta F_{elastic} = \frac{3}{2} \frac{\rho_2 V_0}{\bar{M}_c} RT (\phi_2^{-2/3} - 1)$$

Basic Equation of Gel Swelling



$$\mu_{\text{gel}} = \mu_1^0 \quad \Delta\mu_1 = \mu_{\text{gel}} - \mu_1^0 = 0$$

$$\Delta\mu_{\text{gel}} = \frac{\partial\Delta F}{\partial n_1} = \frac{\partial\Delta F_m}{\partial n_1} + \frac{\partial\Delta F_{\text{elastic}}}{\partial\phi_2} \frac{\partial\phi_2}{\partial n_1} = 0$$

$$\begin{aligned} \frac{\partial\Delta F_m}{\partial n_1} &= RT \left[\ln(1-\phi_2) + \left(1 - \frac{1}{x}\right)\phi_2 + \chi\phi_2^2 \right] & \frac{\partial\Delta F_{\text{elastic}}}{\partial\phi_2} &= -\frac{\rho_2 V_0}{\bar{M}_c} RT \phi_2^{-5/3} \\ &= RT \left(\chi - \frac{1}{2} \right) \phi_2^2 & \frac{\partial\Delta F_{\text{elastic}}}{\partial\phi_2} \frac{\partial\phi_2}{\partial n_1} &= \frac{\rho_2 \bar{V}_s}{\bar{M}_c} RT \phi_2^{1/3} \end{aligned}$$

$$\ln(1-\phi_2) \doteq -\phi_2 - \frac{1}{2}\phi_2^2 \quad x \rightarrow \infty$$

$$\Delta\mu_1 / RT \doteq \left(\chi - \frac{1}{2} \right) \phi_2^2 + \frac{\rho_2 \bar{V}_s}{\bar{M}_c} \phi_2^{1/3} = 0$$

$$\frac{\partial\phi_2}{\partial n_1} = \frac{\partial \left(\frac{V_0}{V_0 + n_1 \bar{V}_s} \right)}{\partial n_1} = -\frac{V_0}{(V_0 + n_1 \bar{V}_s)^2} \bar{V}_s = -\phi_2^2 \frac{\bar{V}_s}{V_0}$$

$$Q = V/V_0 = 1/\phi_2 = \lambda^3$$

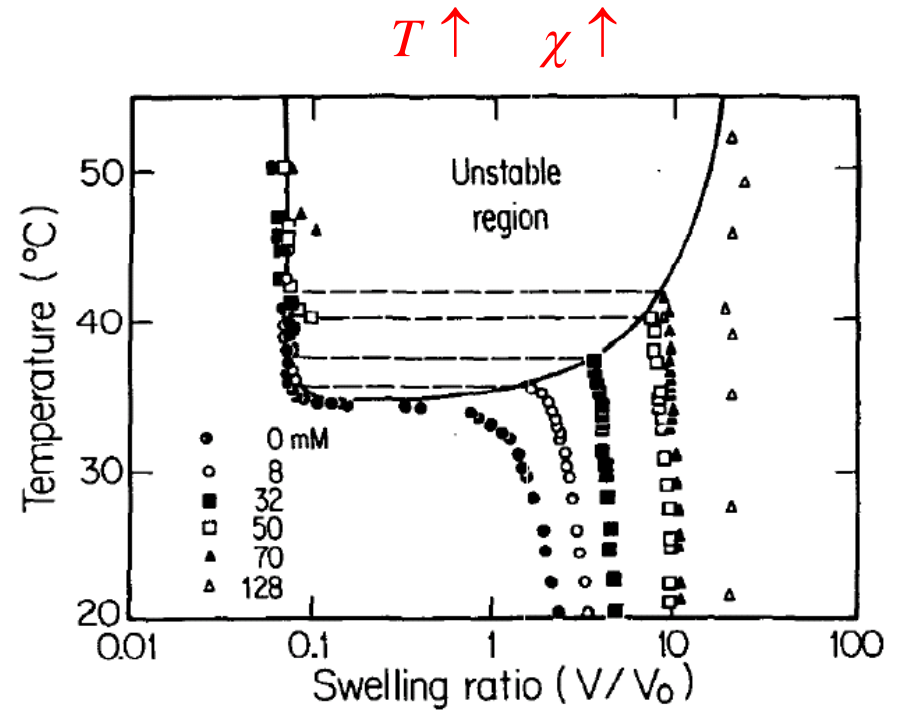
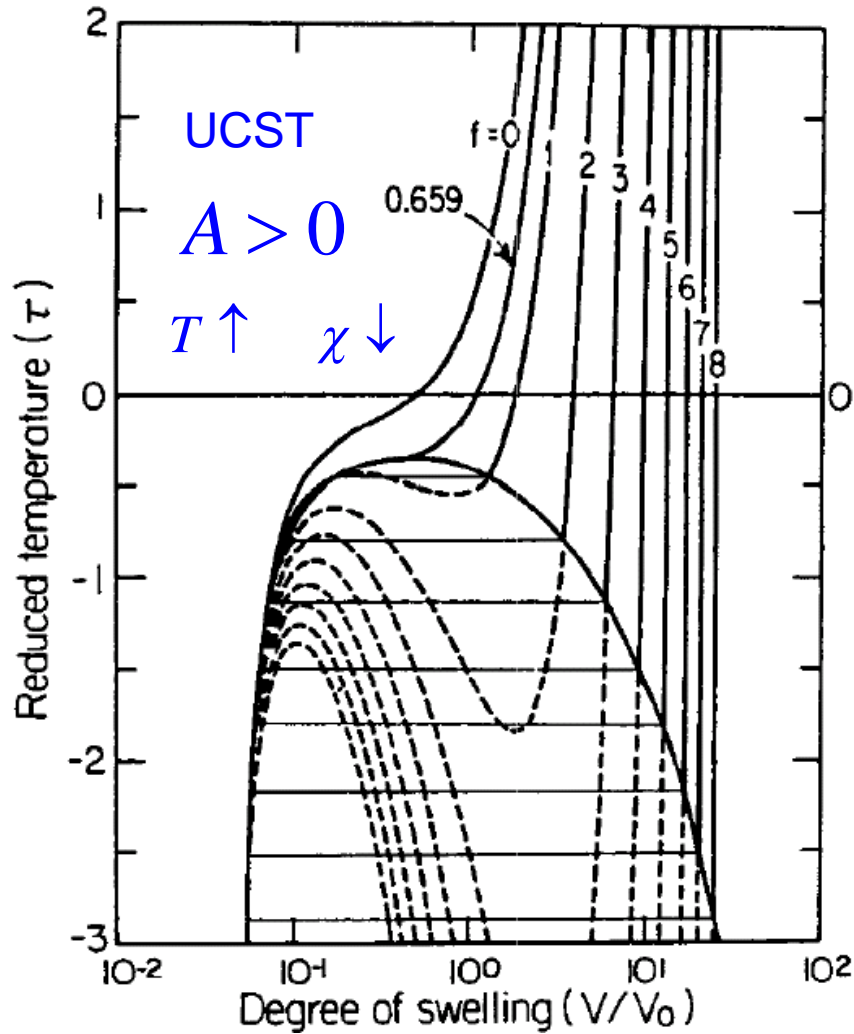
$$\left(\frac{1}{2} - \chi \right) \frac{\bar{M}_c}{\rho_2 \bar{V}_s} = Q^{5/3}$$

(1) 求 χ

(2) 求 M

$$Q \approx \bar{M}_c^{3/5}$$

Volume Phase Transition of Gels



Experiment

LCST $A < 0$

Theory, $\tau = 1 - 2\chi \sim 1 - T_\theta/T$

Flory-Huggins
 Parameter

$$\chi = A/T + B$$

Problem: semi-dilute solution???

$$\Delta\mu_{gel} = \frac{\partial\Delta F}{\partial n_1} = \Delta\mu_1 + \frac{\partial\Delta F_{elastic}}{\partial\phi_2} \frac{\partial\phi_2}{\partial n_1} = 0$$

$$\begin{aligned} \Delta\mu_1 &= \frac{\partial\Delta F_m}{\partial n_1} = RT \left[\ln(1 - \phi_2) + \left(1 - \frac{1}{x}\right) \phi_2 + \chi\phi_2^2 \right] \\ &= -\bar{V}_s \Pi \approx RT \left(\chi - \frac{1}{2} \right) \phi_2^2 \quad \langle R_0^2 \rangle \approx Nl^2 \end{aligned}$$

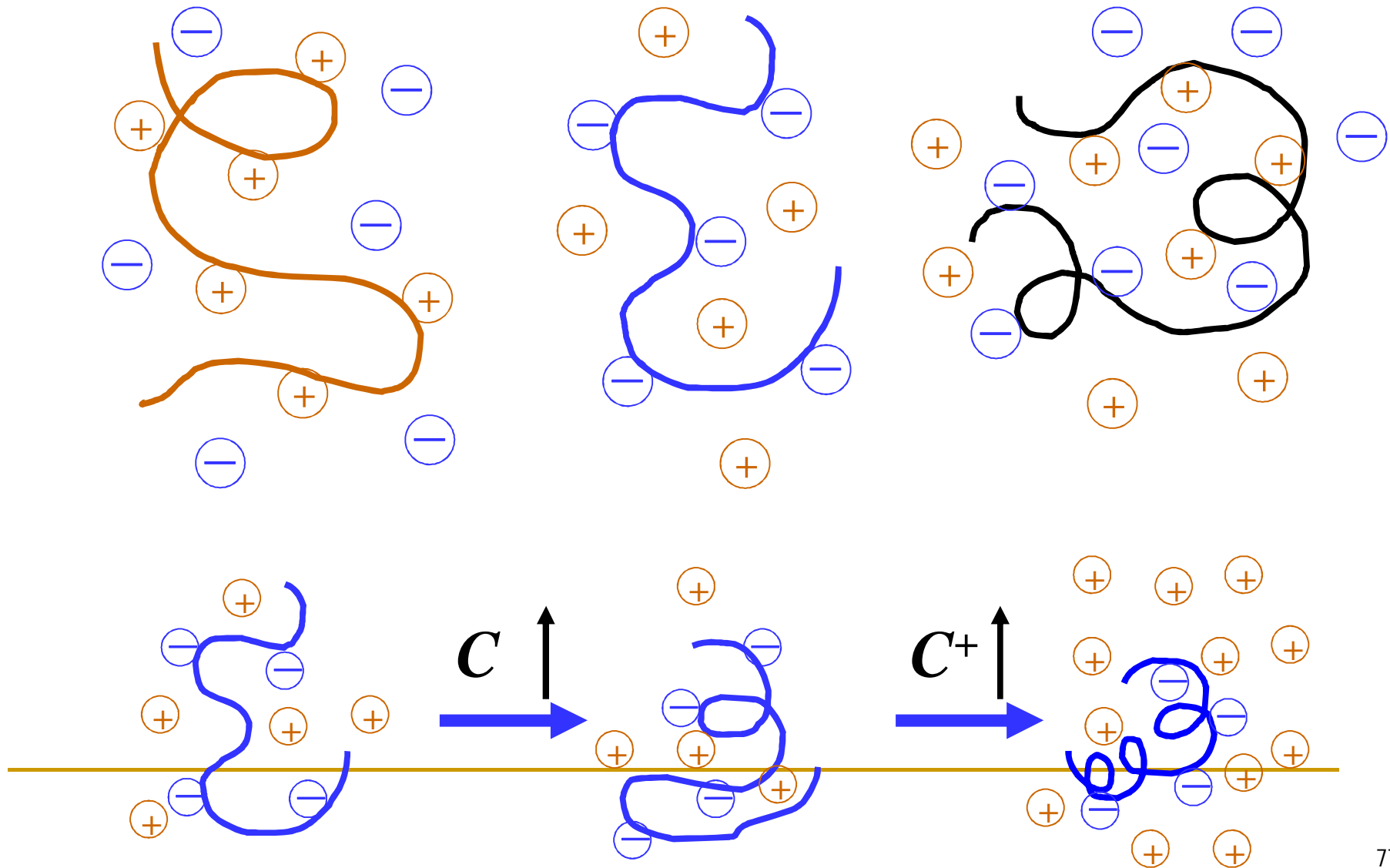
$$\Delta F_{elastic} \approx Nk_B T \frac{\lambda^2 R_0^2}{R_{fluct}^2} = \frac{\rho_2}{\bar{M}_c} V_0 \tilde{N} k_B T \frac{\lambda^2 R_0^2}{R_{fluct}^2}$$

$$\bar{V}_s \Pi = \frac{\rho_2}{\bar{M}_c} V_0 RT \frac{\partial \left(\frac{\lambda^2 R_0^2}{R_{fluct}^2} \right)}{\partial\phi_2} \frac{\partial\phi_2}{\partial n_1} = -\frac{\rho_2}{\bar{M}_c} \bar{V}_s RT \frac{\partial \left(\frac{\lambda^2 R_0^2}{R_{fluct}^2} \right)}{\partial\phi_2} \phi_2^2$$

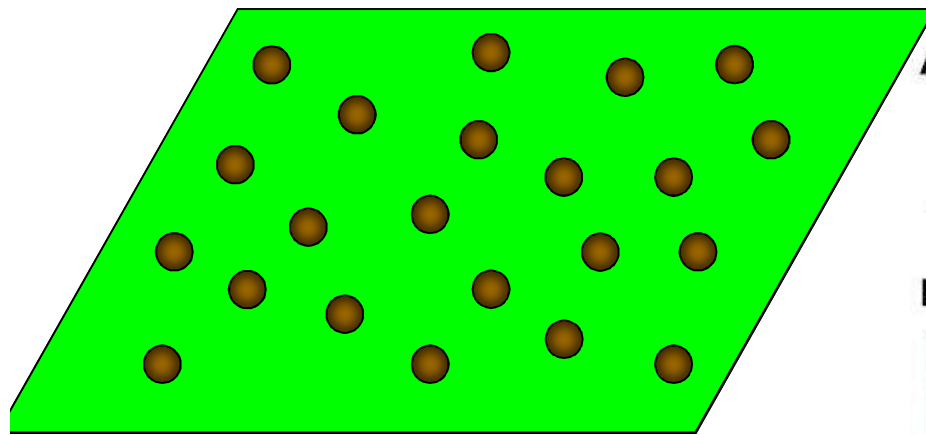
$$\frac{\partial\phi_2}{\partial n_1} = -\phi_2^2 \frac{\bar{V}_s}{V_0} \quad \Pi \propto c^{9/4} \tau^?$$

$$Q = \frac{V}{V_0} = \phi_2^{-1} = \lambda^3 \quad \lambda = \phi_2^{-1/3} \quad \langle R_{fluct}^2 \rangle \approx N \phi_2^{-1/4} \tau^{1/4} l^2$$

3.8 Solutions of Polyelectrolytes



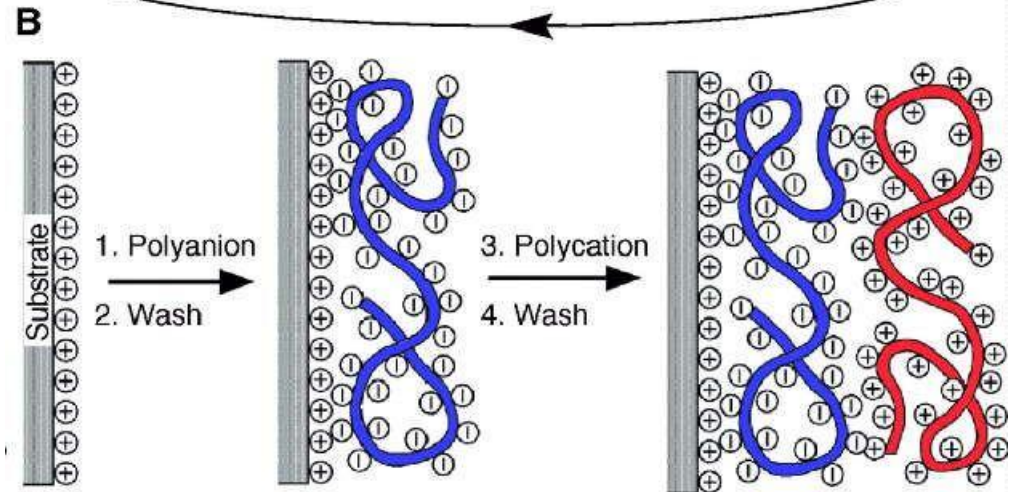
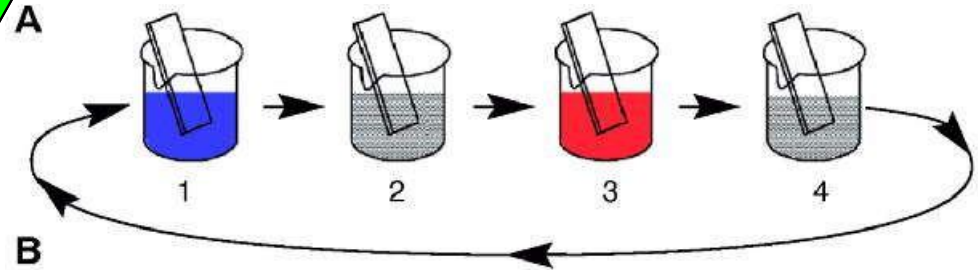
Charge Reversal & Layer by Layer Assembly



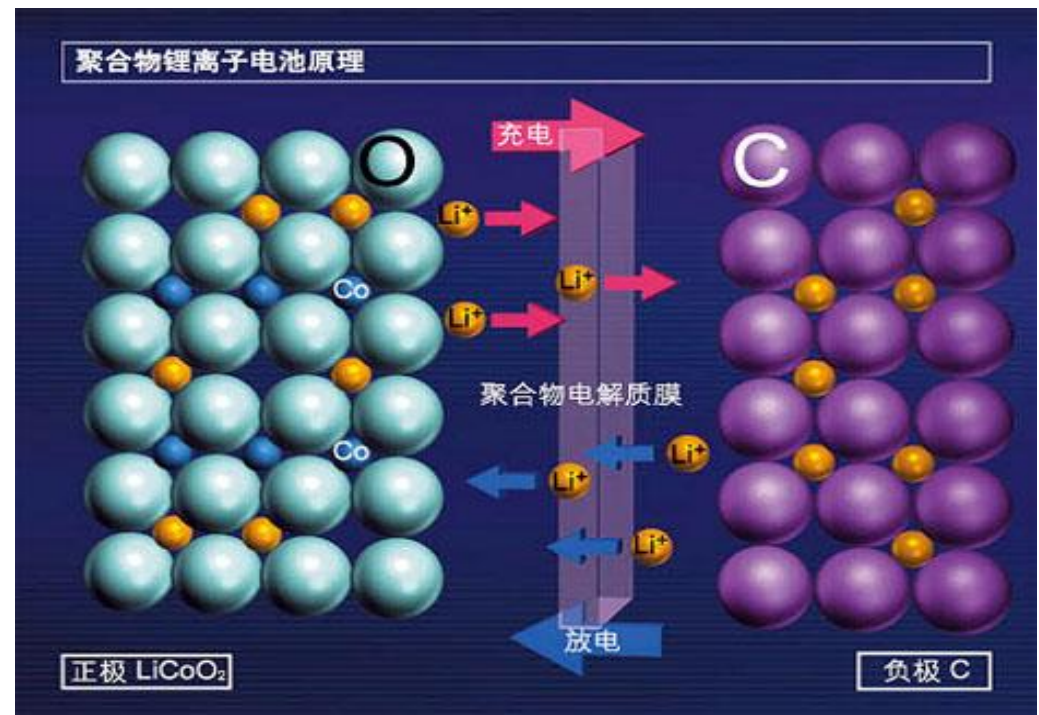
Oppositely charged plane



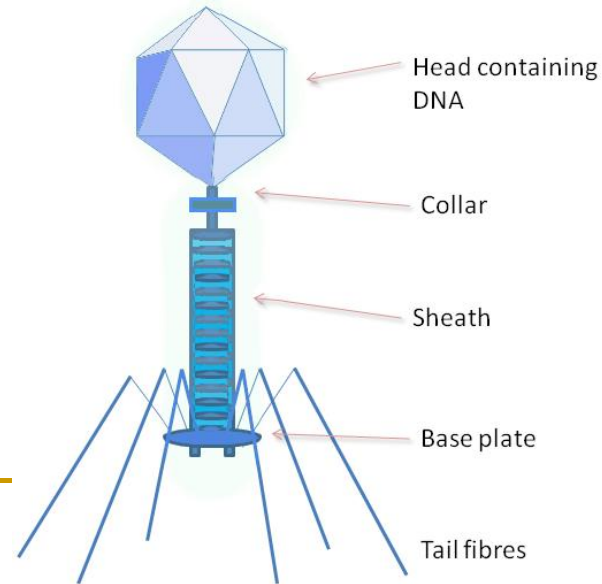
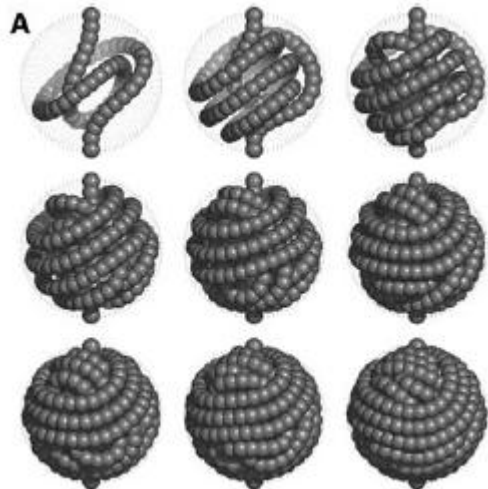
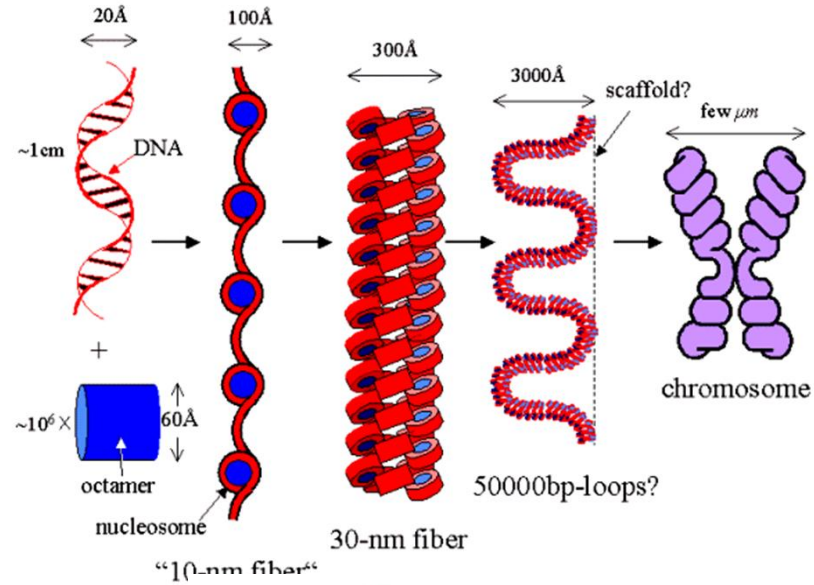
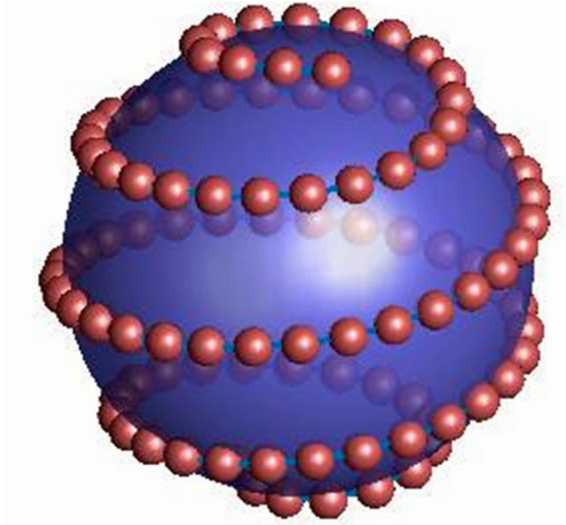
Polyion of charge Z



Li-ion Battery



Wrapping a chain on/in a sphere



Appendix: Introduction to the theory of electrolytes

Long-range Coulomb interaction

- The **force** between two spherically symmetric charges in vacuum



$$f(\mathbf{r}) = \frac{Q_1 Q_2 e^2 \mathbf{r}}{4\pi\epsilon_0 r^3}$$

- The **interaction energy** (in unit of $k_B T$) between two spherically symmetric charges in vacuum

$$U(r) / k_B T = \frac{Q_1 Q_2 e^2}{4\pi\epsilon_0 r}$$

Compared to van der Waals Interaction

$$U_{LJ} / k_B T = \frac{A}{r^{12}} - \frac{B}{r^6}$$

— **Summation of two-body Interactions within a Chain or a Blob**

$$-\bar{E} / k_B T = \frac{v_c}{2} \frac{N^2}{R^3} (1 - 2\chi) \text{ —}$$

Linearized Poisson-Boltzmann Equation

- Debye-Hückel Theory

- When the electric potential is low ($|\phi| < 25\text{mV}$), we can make the expansion and only keep the linear term. Thus the Debye-Hückel equation (linearized Poisson-Boltzmann equation) is obtained. The Debye-Hückel treatment gives a simple (mean-field) description to the many-body interactions between ions.

$$\nabla^2 \phi(\mathbf{r}) = \frac{8\pi e^2 n_0}{\varepsilon} \left[\frac{\phi(\mathbf{r})}{k_B T} + \frac{1}{3!} e^2 \left(\frac{\phi(\mathbf{r})}{k_B T} \right)^3 + \dots \right] \approx \frac{8\pi e^2 n_0}{\varepsilon k_B T} \phi(\mathbf{r}) = \frac{1}{\lambda_D^2} \phi(\mathbf{r})$$

$$\boxed{\nabla^2 \phi(\mathbf{r}) = \lambda_D^{-2} \phi(\mathbf{r})} \quad \text{where} \quad \lambda_D = \sqrt{\frac{\varepsilon k_B T}{8\pi e^2 n_0}} = \sqrt{\frac{1}{8\pi l_B n_0}} \quad l_B = \frac{e^2}{\varepsilon k_B T}$$

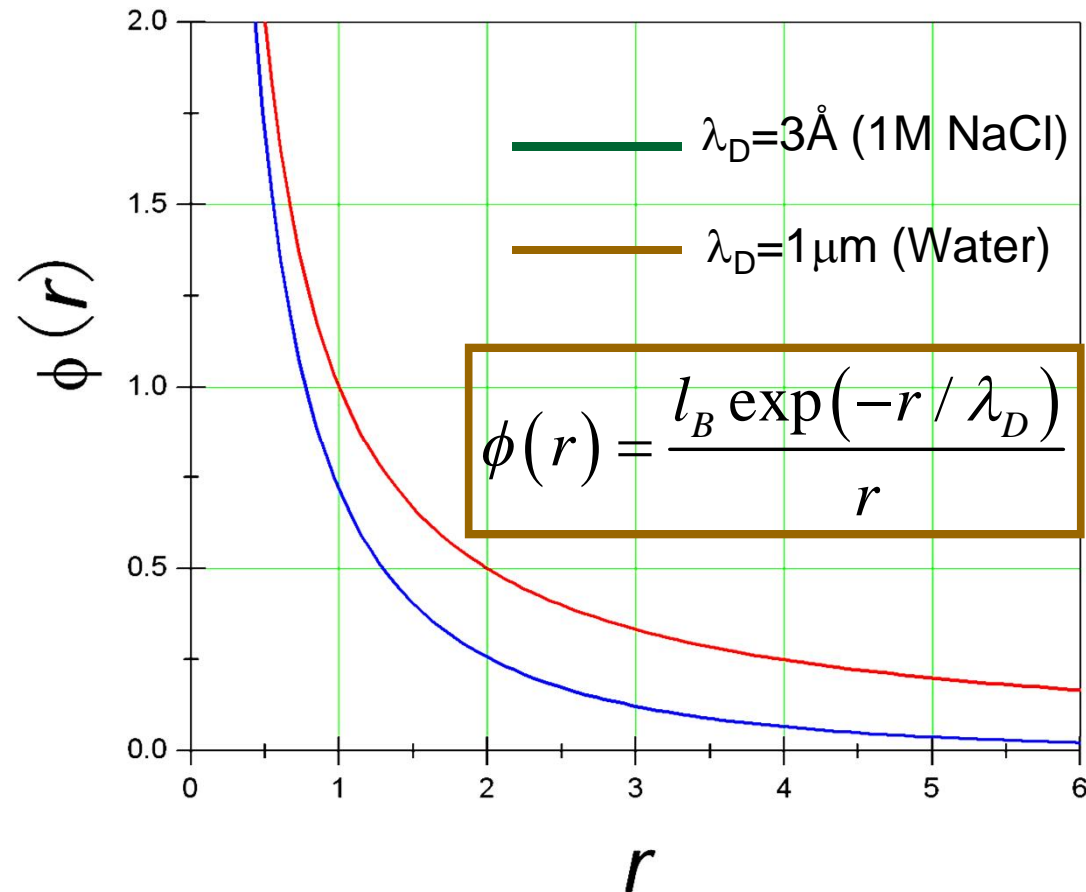
n_0 is the number density (per unit volume) of the ions.

l_B : Bjerrum 长度

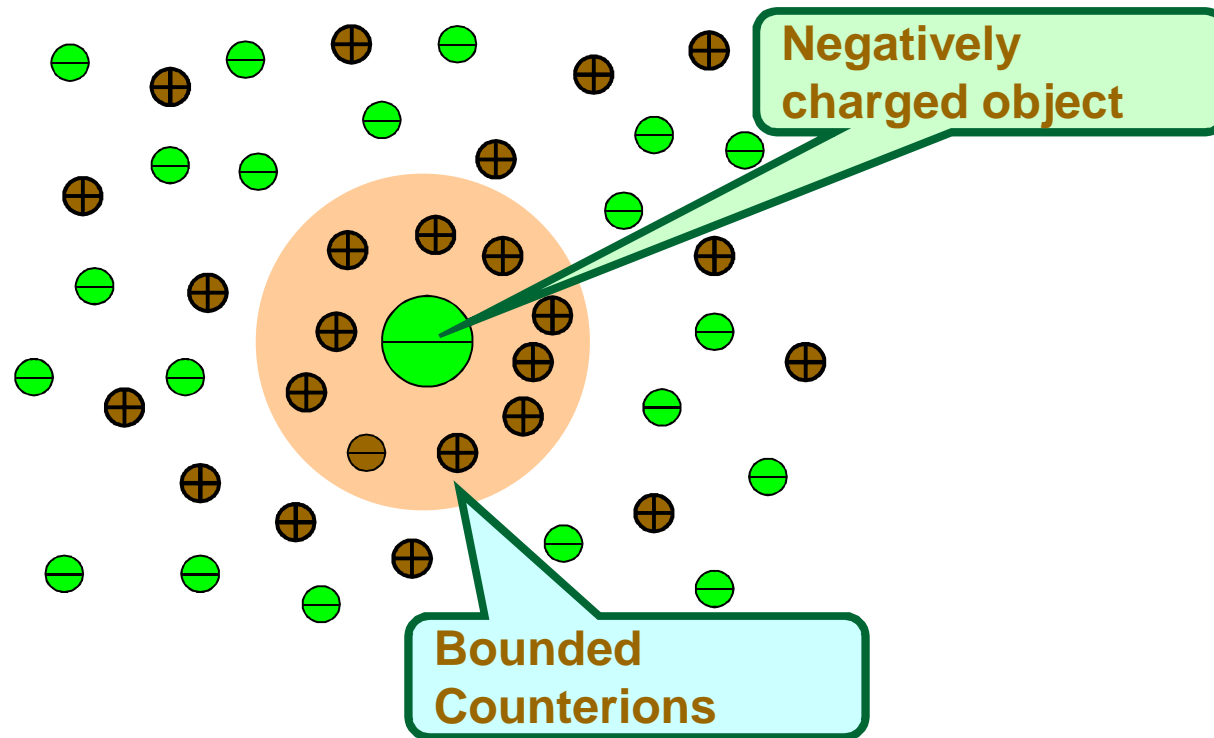
- In the limit of a strong electrolyte, the surface potential ϕ_s is small enough so a linearization of the P-B equation can be justified.

Debye-Hückel potential

■ The effect of charge screening is dramatically different from the presence of a polarizable environment. As has been shown by Debye and Hückel 80 years ago, screening modifies the electrostatic interaction such that it falls off exponentially with distance.

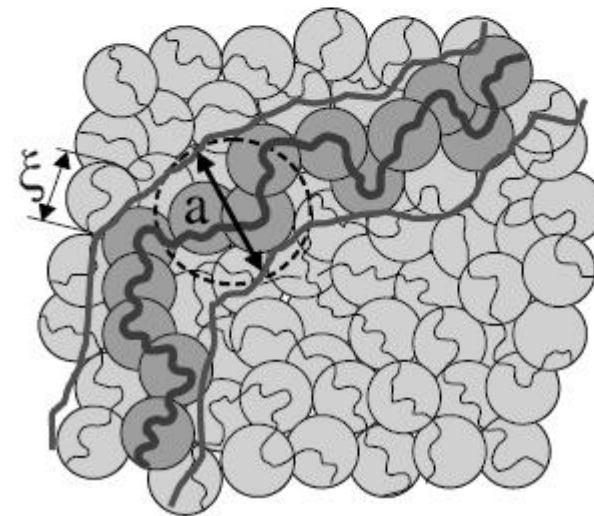
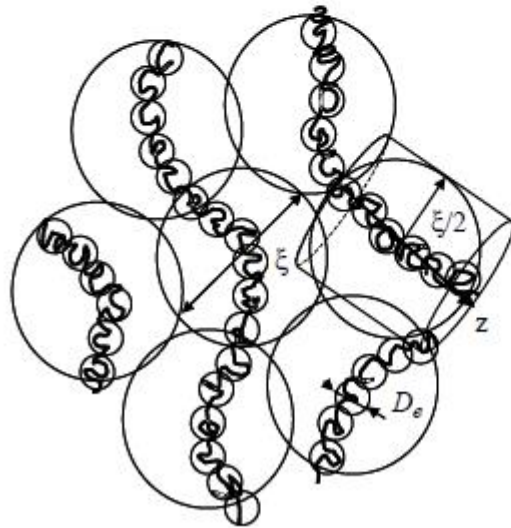
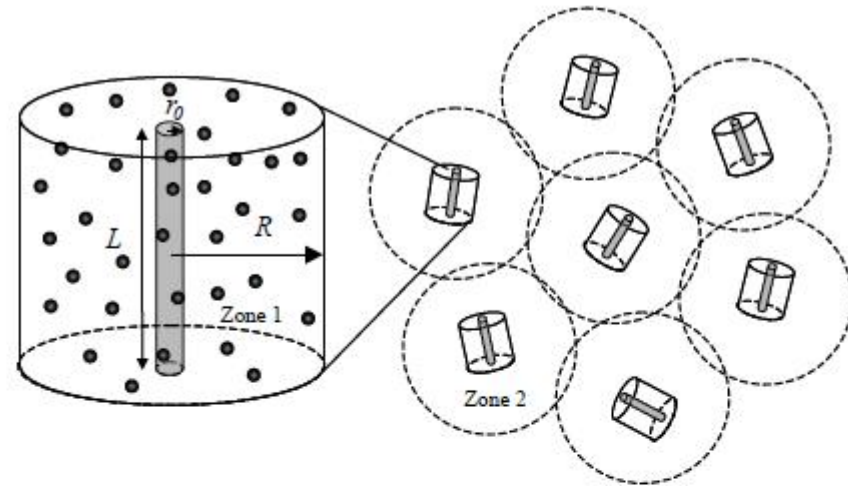
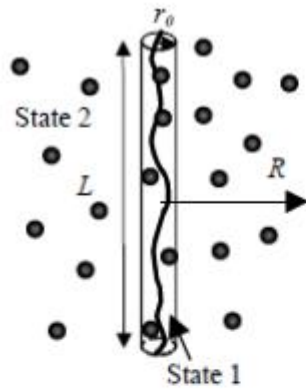


Charge screening



- Salt ions of opposite charge are drawn to charged objects and form loosely bound counter-ion clouds and thus effectively reduce their charges. This process is called **screening**.

Polyelectrolyte in solution



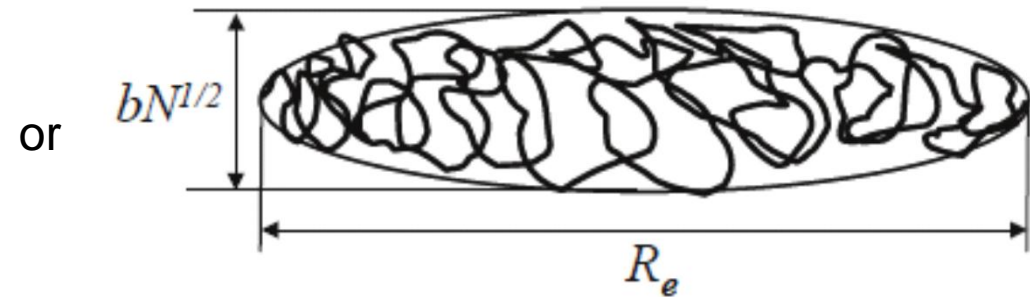
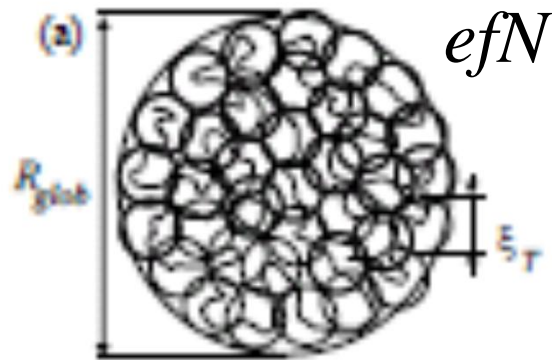
Semi-dilute

concentrated

Theoretical Model of A Single Polyelectrolyte Chain

$$\frac{F(R_e)}{k_B T} = \frac{F_{\text{conf}}(R_e)}{k_B T} + \frac{F_{\text{electr}}(R_e)}{k_B T} \quad \frac{F_{\text{conf}}(R_e)}{k_B T} \approx \frac{R_e^2}{Nl^2} \quad \text{Gaussian Chain}$$

l : Kuhn segment



$$\frac{F_{\text{electr}}(R_e)}{kT} \approx \frac{l_B (fN)^2}{R_e}$$

or

$$\frac{F_{\text{electr}}(R_e)}{kT} \approx \frac{l_B (fN)^2}{R_e} \ln\left(\frac{R_e}{N^{1/2}l}\right)$$

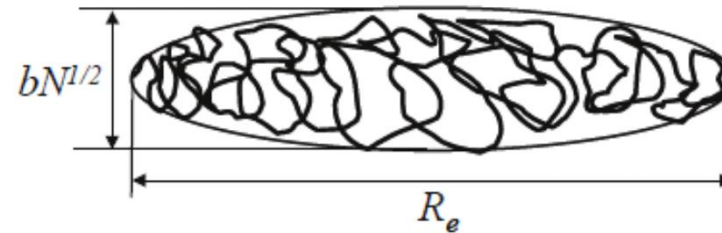
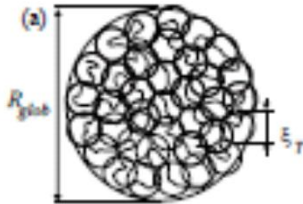
l_B 为 Bjerrum 长度 $l_B = e^2 / (\epsilon k_B T)$ $u_B = l_B / l$

$$\frac{\partial F(R_e)}{\partial R_e} = 0$$

(1) A Single Polyelectrolyte Chain in good solvents

Good solvent, $\chi < 1/2$:

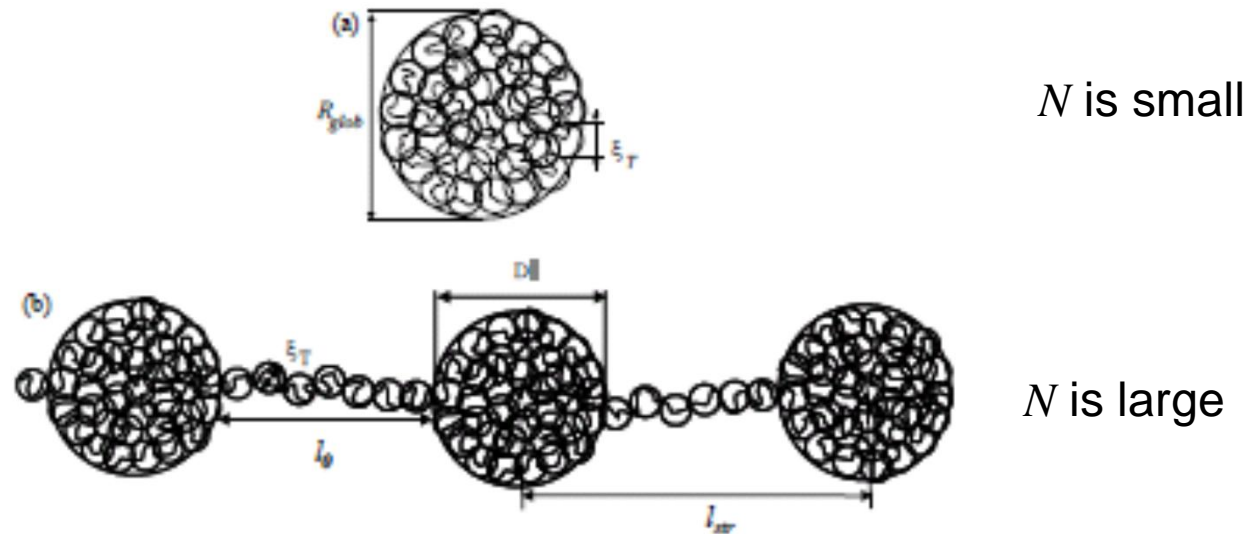
$$R_e \approx N l u_B^{1/3} f^{2/3} \quad \text{or} \quad R_e \approx N l u_B^{1/3} f^{2/3} \left[\ln \left(e N \left(u_B f^2 \right)^{2/3} \right) \right]^{1/3}$$

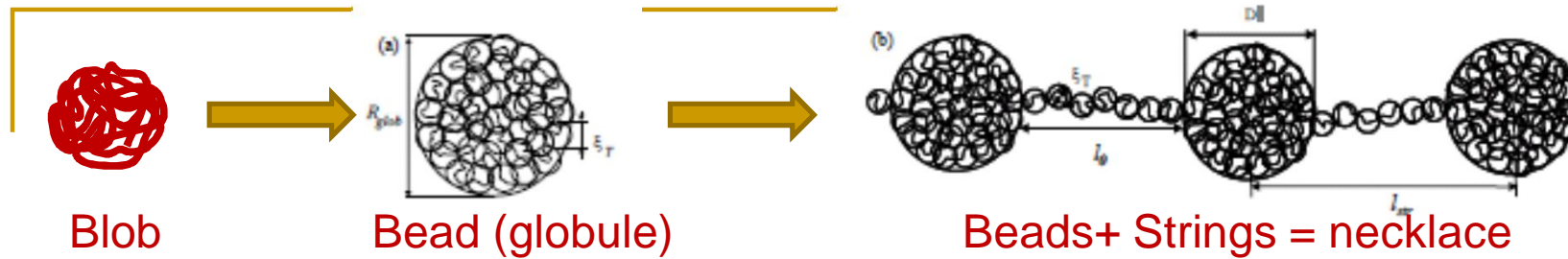


$$R_e \gg N^{1/2}$$

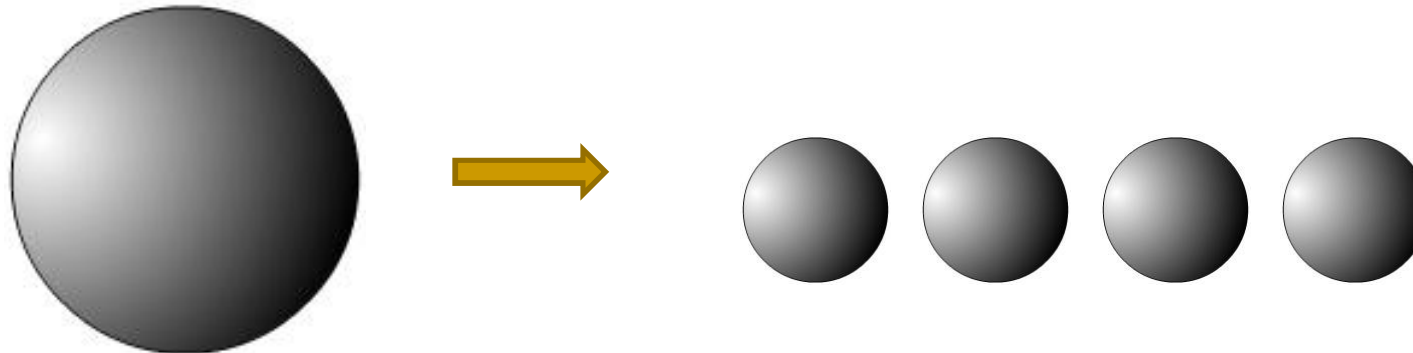
(2) A Single Polyelectrolyte in poor solvents

Poor solvent, $\chi > 1/2$:





Rayleigh instability of a charged droplet – 1882



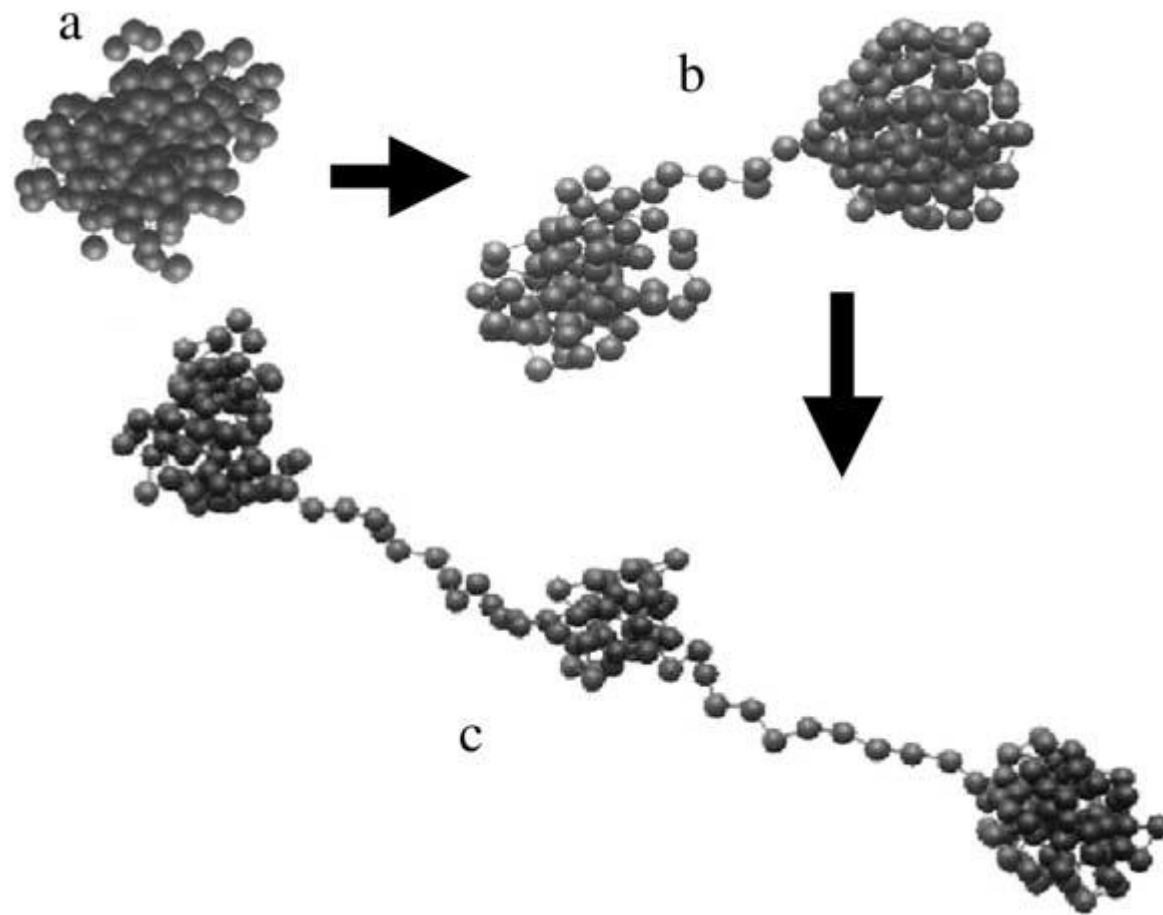
the break-up of a charged drop of liquid into droplets due to electrostatic repulsion

$$F_{Rayleigh} / k_B T = \frac{Q^2}{\epsilon R_{drop}} + \gamma R_{drop}^2 \quad \frac{\partial F_{Rayleigh}}{\partial R_{drop}} = 0 \quad \Rightarrow \quad Q_{crit} \sim R_{drop}^{3/2}$$

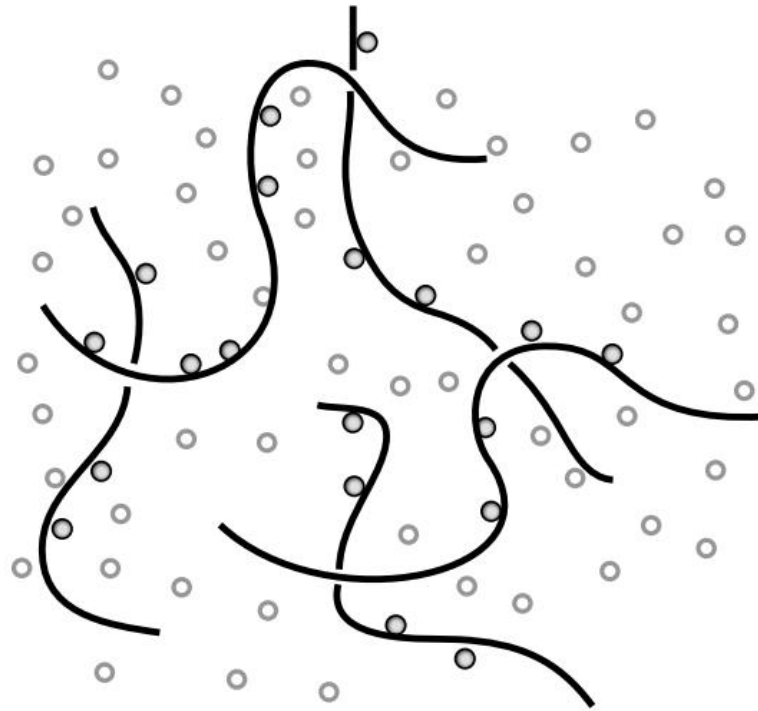
$$F_{electro} = k_B T l_B (fN)^2 / R_{glob} \quad \xi_T = l |\tau|^{-1} \quad R_{glob} \approx l |\tau|^{-1/3} N^{1/3} \quad f_{crit} \approx \left(\frac{|\tau|}{u_B N} \right)^{1/2}$$

$$F_{surf} = k_B T R_{glob}^2 / \xi_T^2$$

Computer Simulations



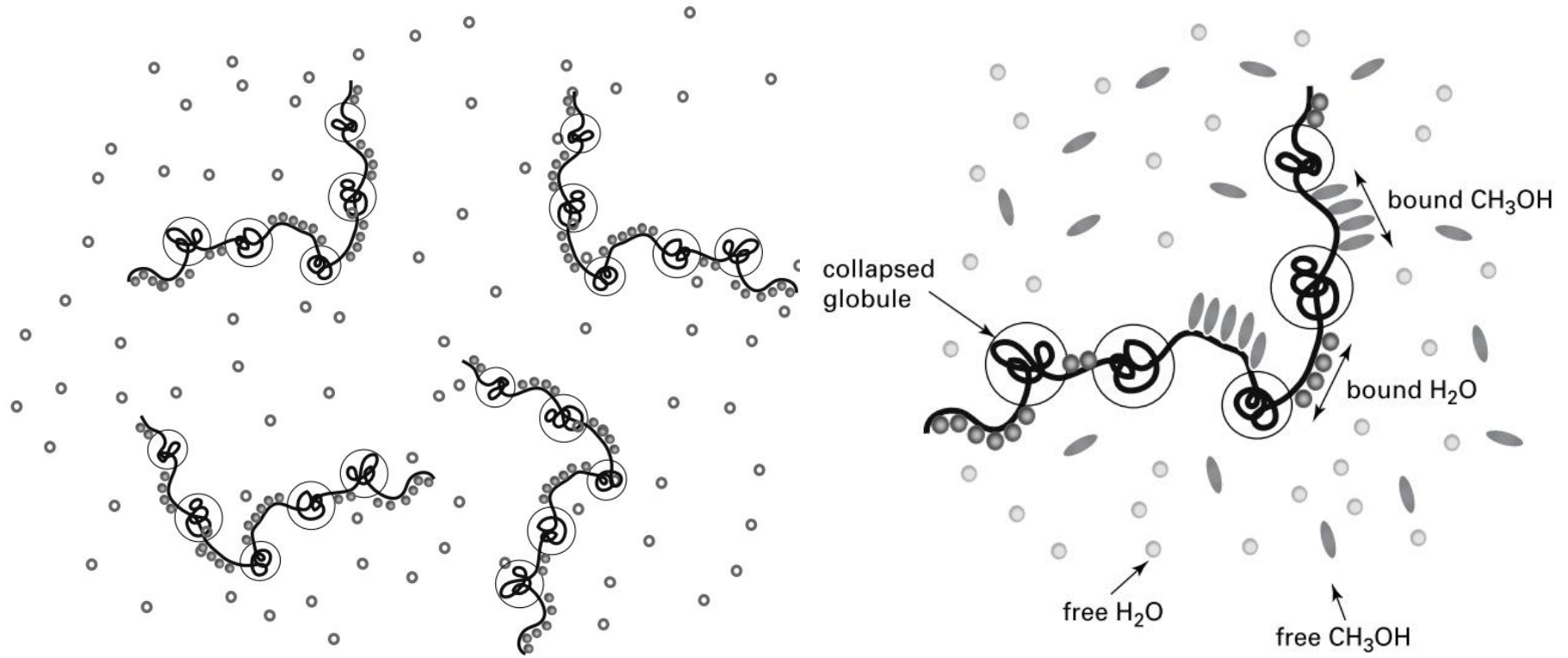
Topics not Discussed: Hydration and Associating in Polymer Solutions



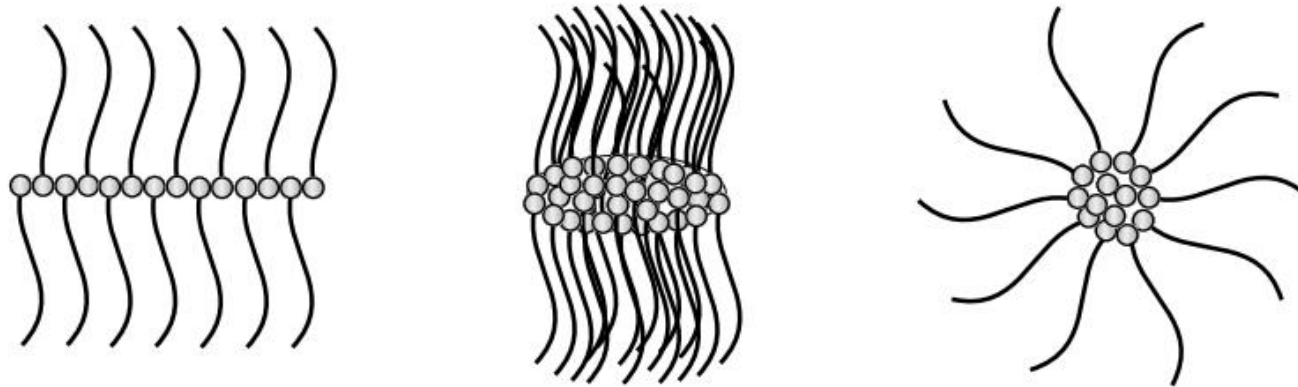
Hydration

PNIPAM (*N*-异丙基丙烯酰胺) in Water

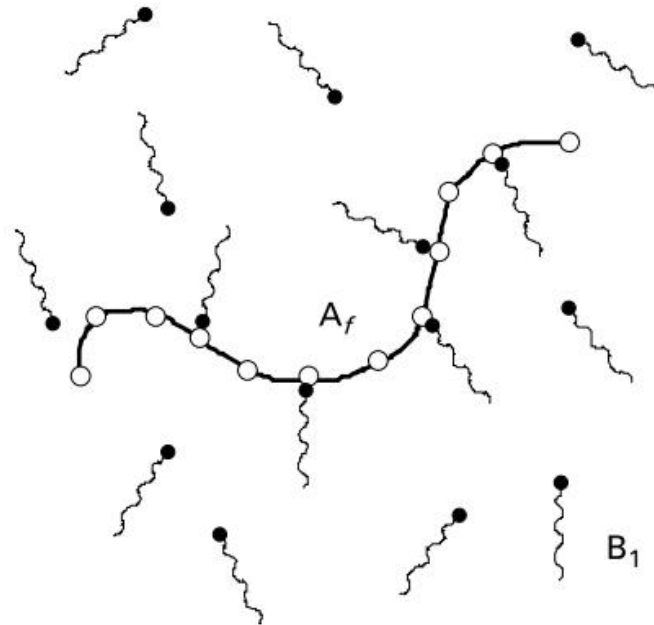
and Mixed Solvents



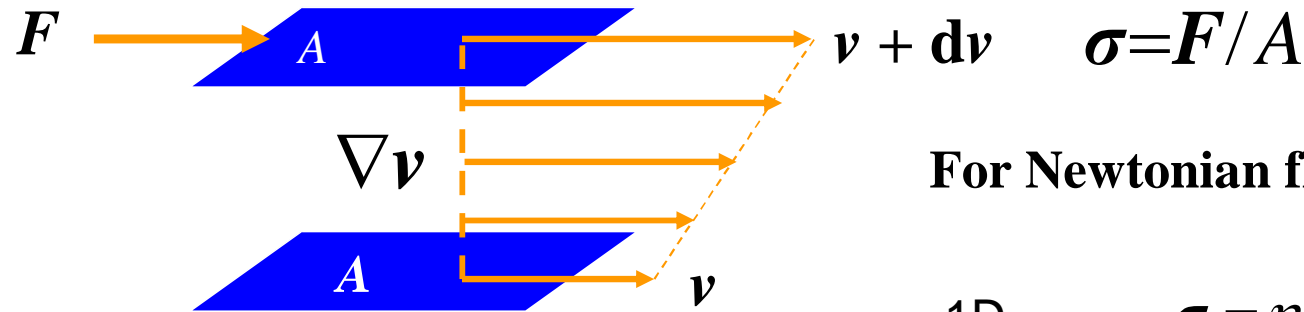
Topics not Discussed: Associating Polymer Solutions



(a)



3.9 Hydrodynamics Properties of Polymer Solutions

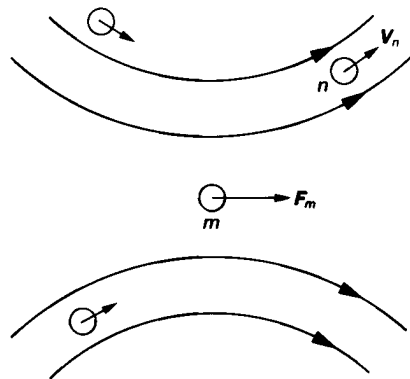


For Newtonian fluids

1D $\sigma = \eta v$

2D $\sigma = \eta \frac{dv}{dy}$

3D $\sigma = \eta \left[\nabla v + (\nabla v)^T \right]$

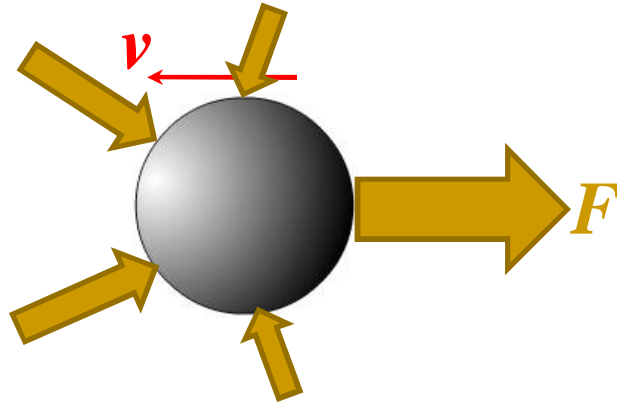


$$v_n(\mathbf{r}) = \sum_m \mathbf{H}_{nm} \cdot \mathbf{F}_m$$

$$v(\mathbf{r}) = \int d\mathbf{r}' H(\mathbf{r} - \mathbf{r}') \cdot F(\mathbf{r}')$$

Correlation function: \mathbf{H}_{nm} or $\mathbf{H}(\mathbf{r} - \mathbf{r}')$

Diffusion of Suspensions in Solution



Stokes formula

$$F = -6\pi R\eta v = -\zeta v \quad \zeta = 6\pi R\eta$$

Stokes-Einstein relation

$$D = k_B T / \zeta = \frac{k_B T}{6\pi\eta R}$$

$$D = D_0 (1 + k_D c + \dots)$$

Fick's law

flux $\vec{J} = -D \frac{\partial c}{\partial r}$

$$\frac{\partial c}{\partial t} = -\vec{\nabla} \cdot \vec{J} = D \frac{\partial^2 c}{\partial r^2}$$

$$D_0 = k_D M^{-b} = \frac{k_B T}{6\pi\eta R_h} \quad \begin{aligned} [\eta] &= K_{MH} M^a \\ b &\approx \frac{1+a}{3} \end{aligned}$$

hydrodynamics radius: R_h

Effective viscosity of suspensions

For the solution of impenetrable spheres of radius R , Einstein derived the Effective viscosity of suspensions

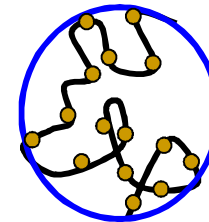
$$\eta = \eta_0 (1 + 2.5\Phi)$$

η_0 : viscosity of pure solvent

Φ : volume fraction occupied by the suspensions in the solution.

If each sphere consists of n particles (monomer units) of mass m , and their density is c , we have

$$\Phi = N \frac{4}{3} \pi R^3 / V = \frac{N_A c}{M} \frac{4}{3} \pi R^3$$



$$nm = M$$

Intrinsic viscosity (特性粘数)

$$[\eta] = \left[\frac{\eta - \eta_0}{\eta_0 c} \right]_{c \rightarrow 0}$$

N_A : Avogadro Number

$$[\eta] = \frac{2.5\Phi}{c} = 2.5 N_A \frac{4\pi R^3 / 3}{M} = 2.5 N_A \frac{V_h}{M}$$

V_h hydrodynamics volume

[η] dependence of MW: Flory-Fox equation

ϕ_0 is calculated by Rouse-Zimm Theory and confirmed by experiments

$$[\eta] = \phi \frac{\langle h^2 \rangle^{3/2}}{M} = \phi \left[\frac{\langle h^2 \rangle}{M} \right]^{3/2} M^{1/2}$$

$$\alpha = \left(\frac{h^2}{h_0^2} \right)^{1/2} \sim N^{\nu-0.5} \quad \text{扩张因子}$$

$$[\eta] = \phi \left[\frac{\langle h_0^2 \rangle}{M} \right]^{3/2} M^{1/2} \alpha^3$$

$$\chi=1/2 \quad [\eta]_{\Theta} = \phi_0 \left[\frac{\langle h_0^2 \rangle}{M} \right]^{3/2} M^{1/2}$$

$$\phi_0 = 2.84 \times 10^{23} \text{ mol}^{-1}$$

Mark-Houwink Relation $[\eta] = KM^a$

For Θ solution

$$\langle h_0^2 \rangle \sim M^1 \quad [\eta] \sim M^{0.5}$$

For flexible chain in good solvent

$$\langle h^2 \rangle \sim M^{6/5} \quad [\eta] \sim M^{0.8}$$

For stiff chain

$$\langle h^2 \rangle \sim M^2 \quad [\eta] \sim M^2$$

For flexible chain $a=0.5\sim 0.8$

For stiff chain $a=0.8\sim 1.2$

Rouse-Zimm Model

$$R_H = \frac{1}{8} \sqrt{\frac{3\pi}{2}} \sqrt{N} b = 0.66467 R_g$$

$$D_G = \frac{k_B T}{\zeta_0} = \frac{k_B T}{6\pi\eta R_H} = 0.196 \frac{k_B T}{6\pi\eta \sqrt{N} b}$$

$$[\eta] = 0.425 \frac{N_A}{M} (\sqrt{N} a)^3 = \frac{\phi}{M} (\sqrt{6} R_g)^3$$

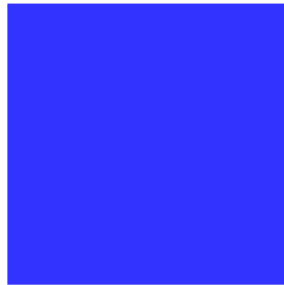
$$\phi_{0(\text{RZ})} = 0.425 N_A = 2.56 \times 10^{23}$$

$$\phi_{0(\text{exp})} = 2.2 \sim 2.87 \times 10^{23}$$

Chapter 4 Multi-component Polymer Systems

- **4.1 Thermodynamics of Polymer Mixtures**
- **4.2 Properties of Polymer Interface**
- **4.3 Thermodynamics of Block Copolymers**

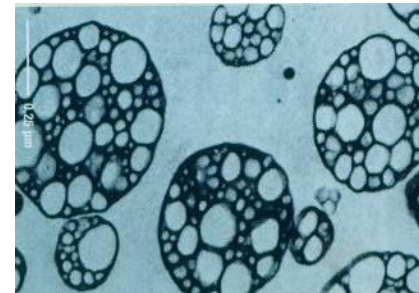
Mixing?



Polymer A



Polymer B



Polymer Blends

4.1 Thermodynamics of Polymer Mixtures

Why are two kinds of polymers not compatible?

$$\Delta G_{\text{mixing}} = kT (N_1 \ln \phi_1 + N_2 \ln \phi_2 + \chi x_1 N_1 \phi_2)$$

Entropy of Mixing

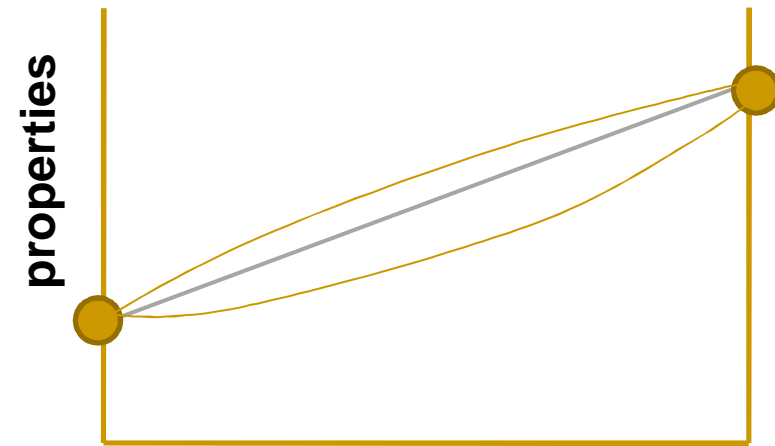
$$N_1 \text{Polymer} / N_2 \text{Polymer} \quad \Delta S_{xN_1, xN_2}^P = -k \left(N_1 \ln \frac{xN_1}{xN_1 + xN_2} + N_2 \ln \frac{xN_2}{xN_1 + xN_2} \right)$$

$$N_1 \text{Solvent} / N_2 \text{Solvent} \quad \Delta S_{N_1, N_2}^S = -k \left(N_1 \ln \frac{N_1}{N_1 + N_2} + N_2 \ln \frac{N_2}{N_1 + N_2} \right)$$

$$xN_1 \text{Solvent} / xN_2 \text{Solvent} \quad \Delta S_{xN_1, xN_2}^S = -k \left(xN_1 \ln \frac{xN_1}{xN_1 + xN_2} + xN_2 \ln \frac{xN_2}{xN_1 + xN_2} \right)$$

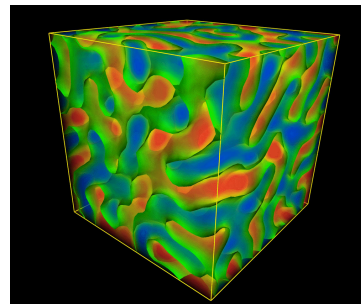
$$\left| \Delta S_{xN_1, xN_2}^P \right| \sim \left| \Delta S_{N_1, N_2}^S \right| \ll \left| \Delta S_{xN_1, xN_2}^S \right|$$

The importance of multi-component, multi-phase materials

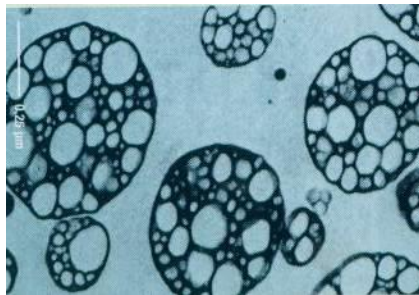


Polymer A **contents** Polymer B

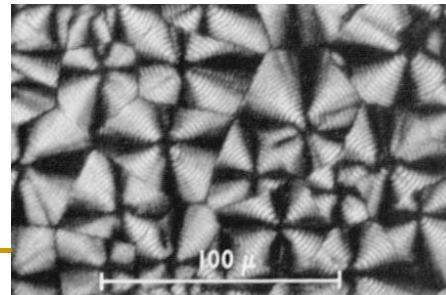
heterogeneous



Polymer blends



HIPS, ABS



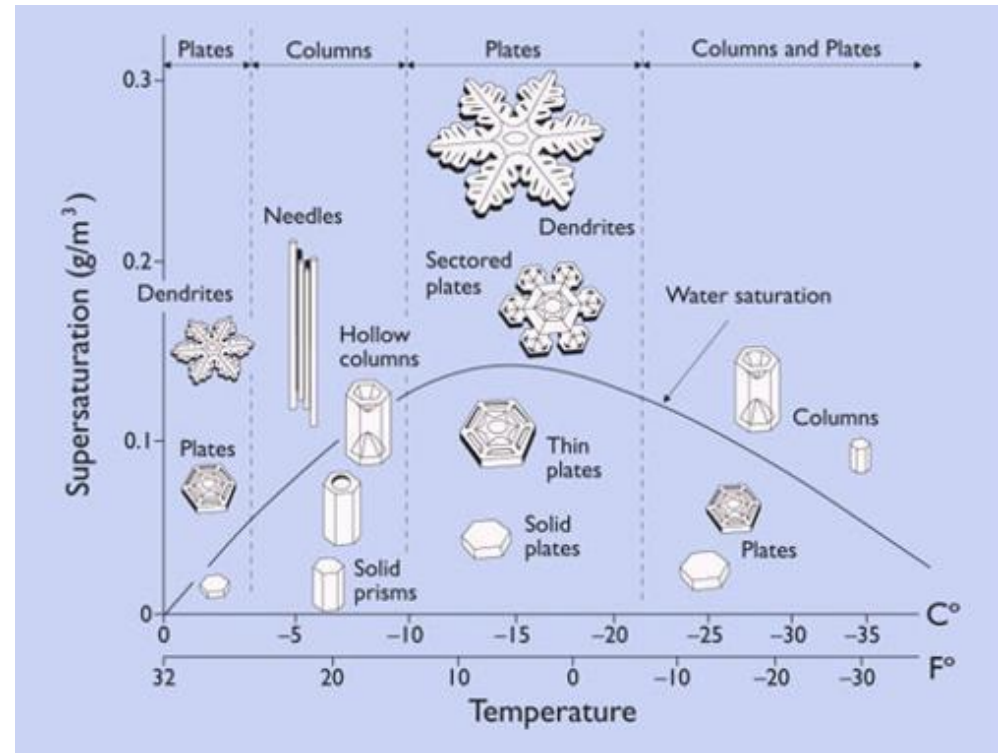
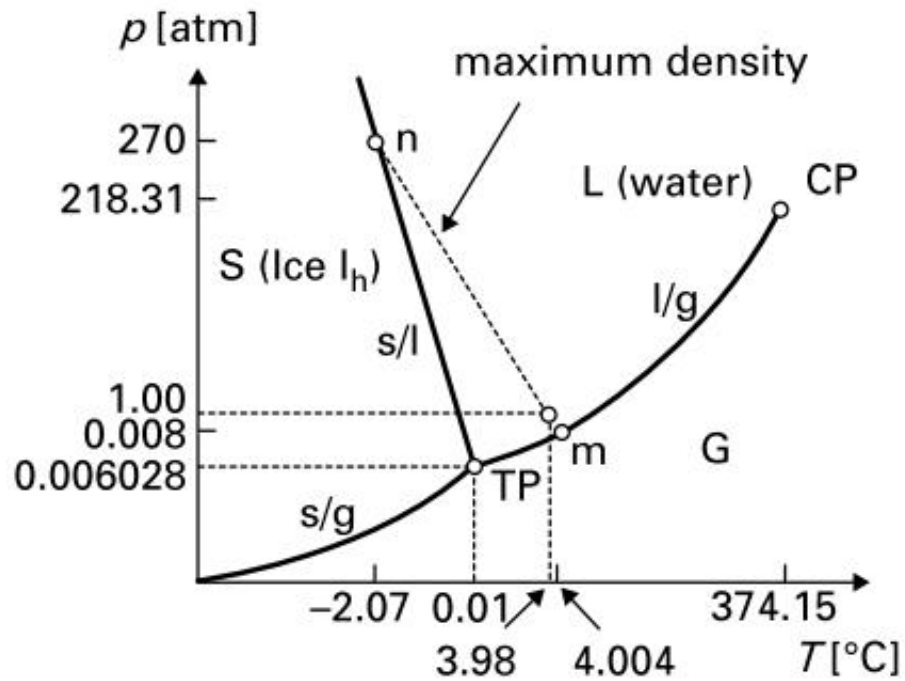
Polyolefins



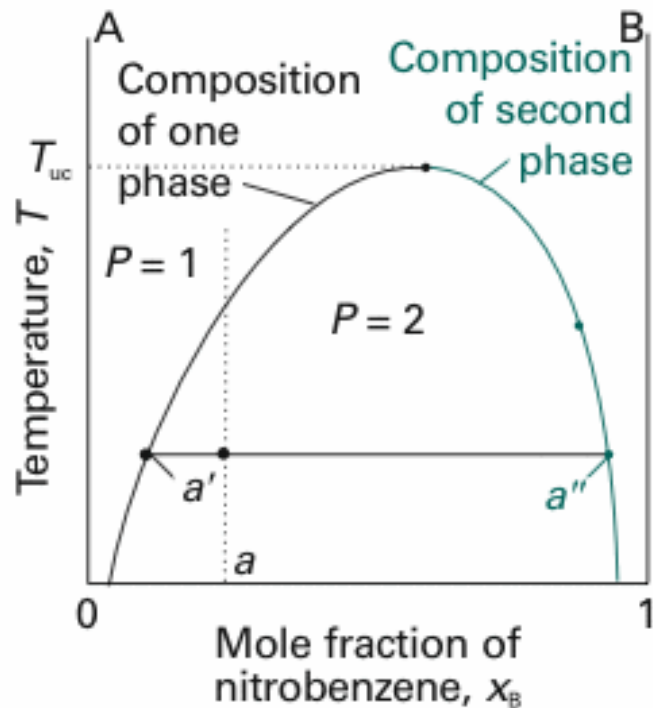
Polymer A **contents** Polymer B

crystallinity

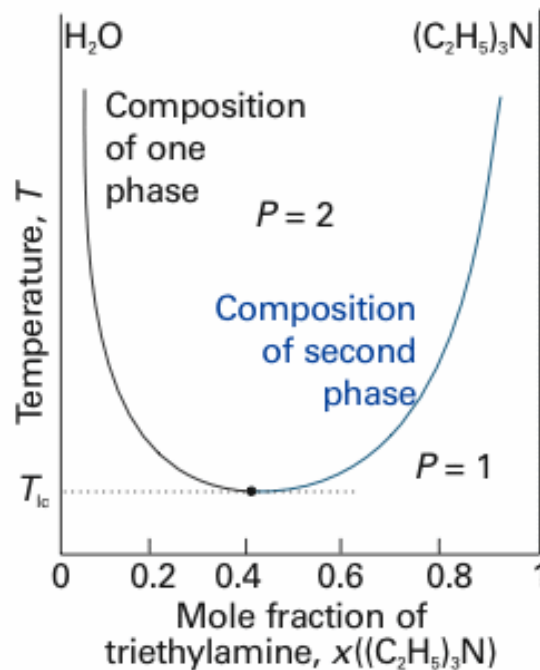
Typical Phase Diagram of One Component



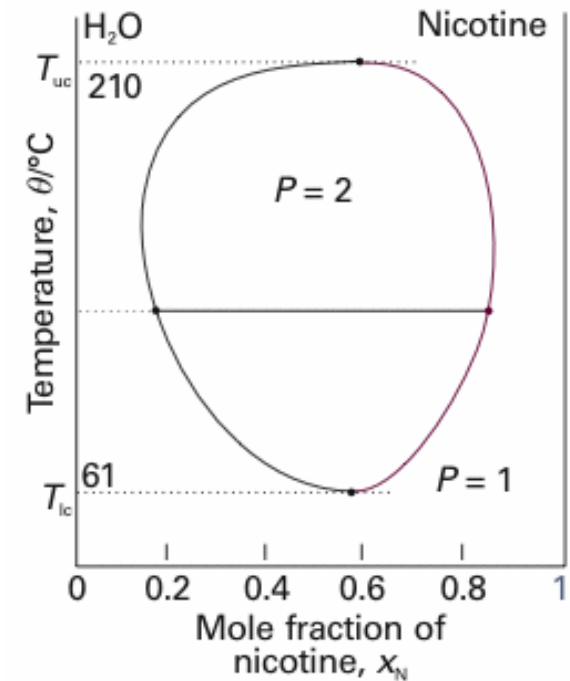
Typical Phase Diagram of Mixture I: Liquid-Liquid



UCST

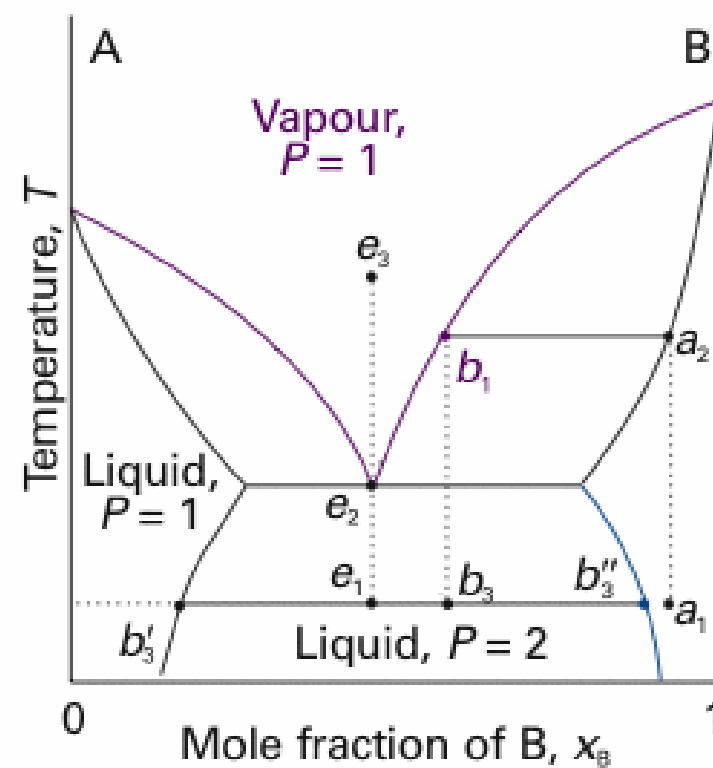
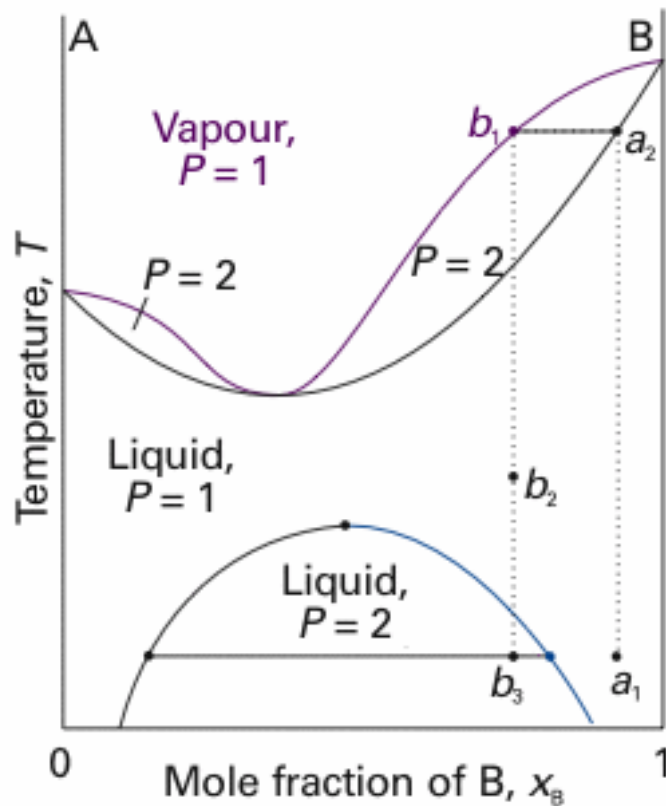


LCST



LCST + UCST

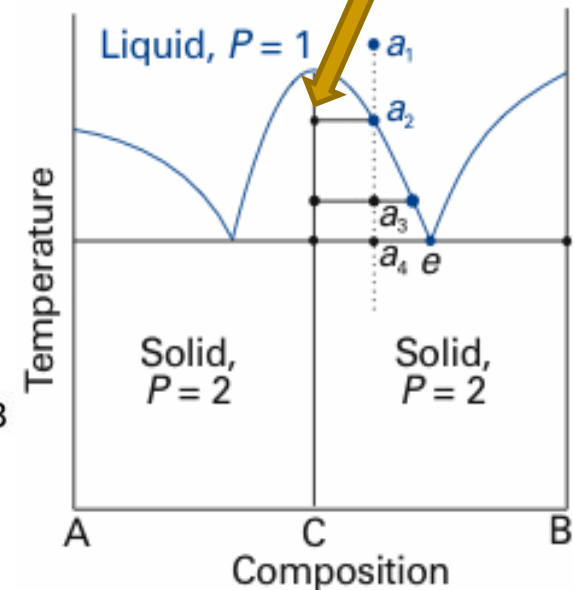
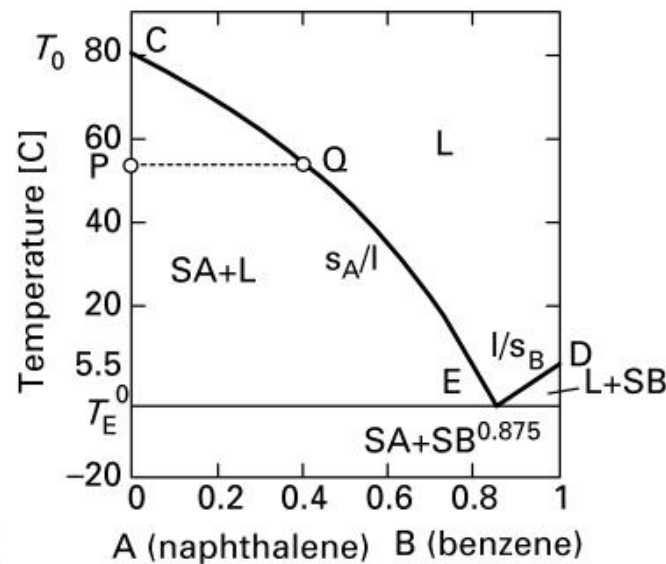
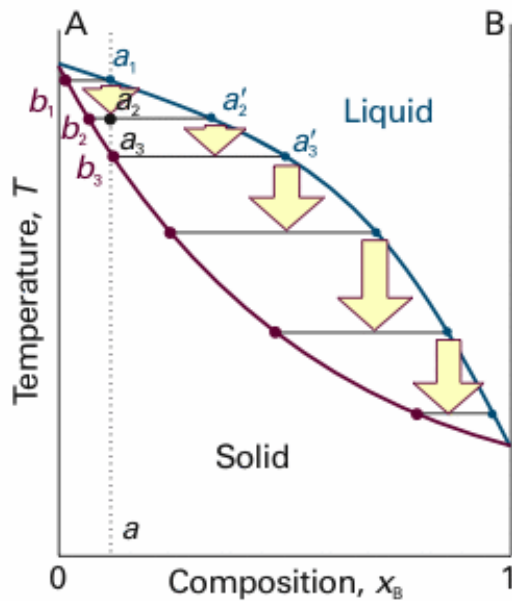
Typical Phase Diagram of Mixture II: Liquid-Liquid & Liquid-Vapour



There is no Vapour Phase in Polymer System

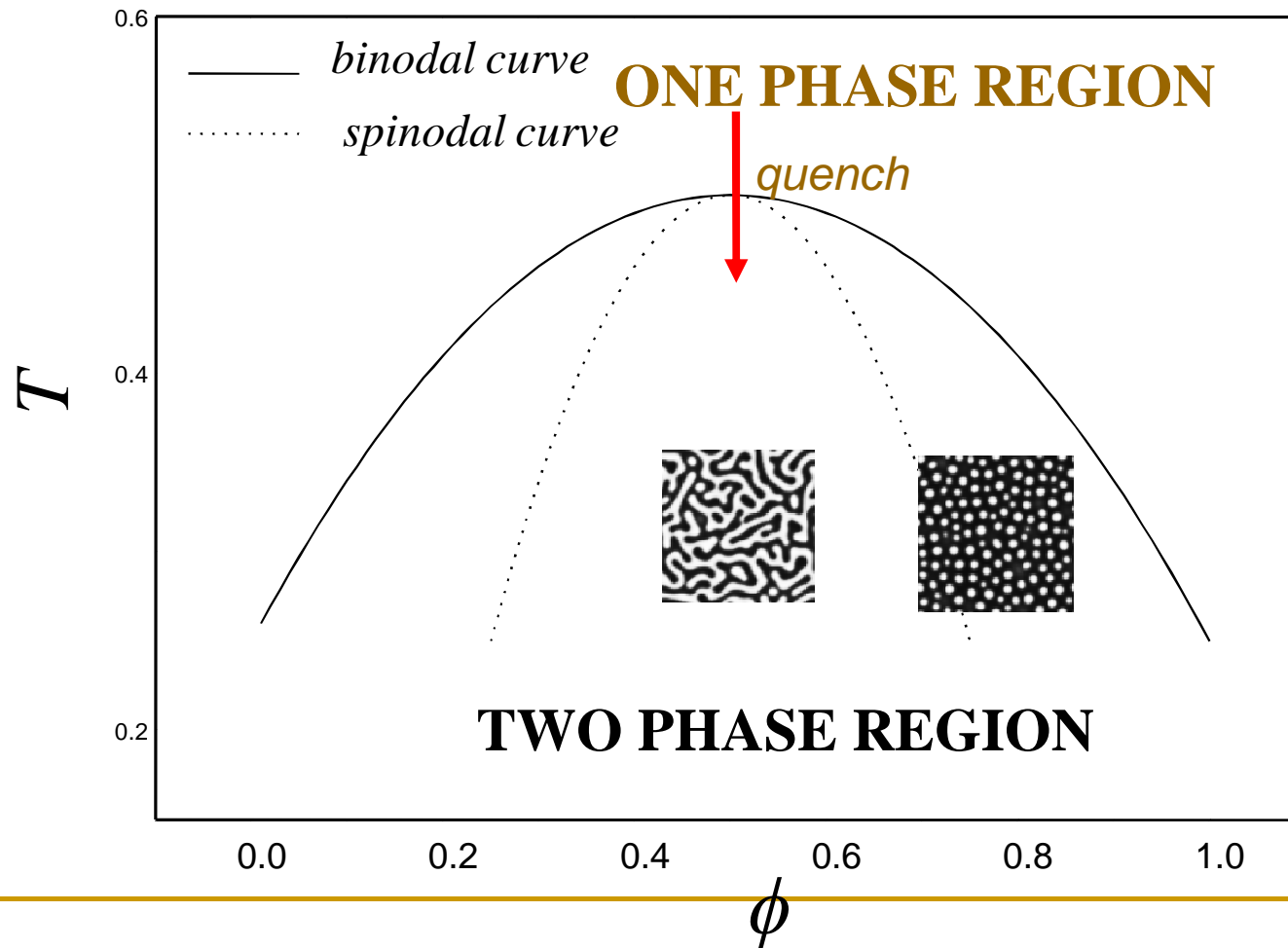
Typical Phase Diagram of Mixture III: Liquid-Solid & Solid-Solid

& Liquid-Liquid

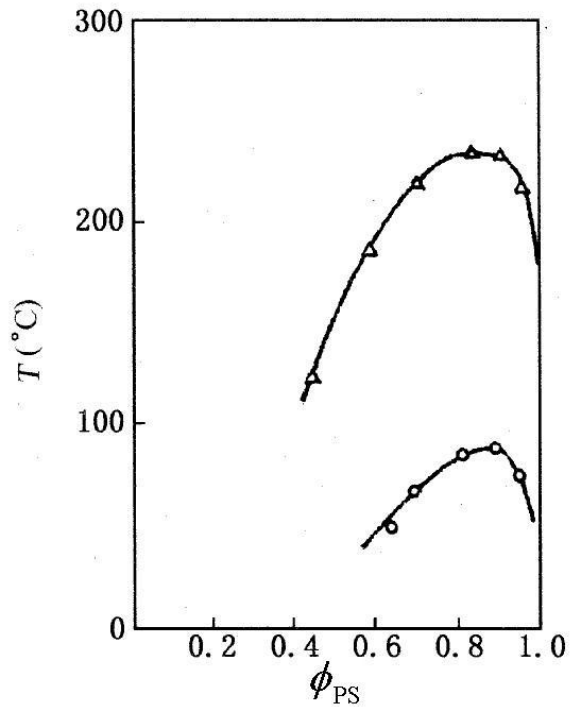


There may exist Solid Phase in Polymer System

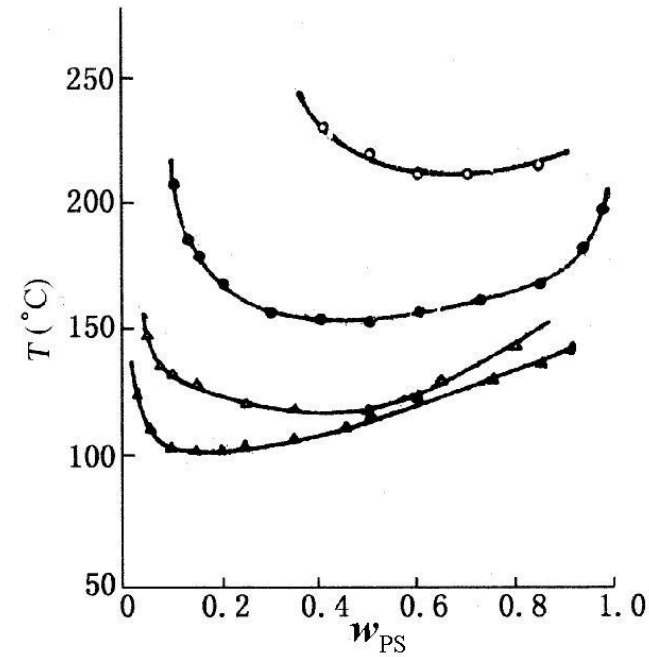
Relation between phase diagram and morphology



Phase Diagrams of Polymer Blends



UCST

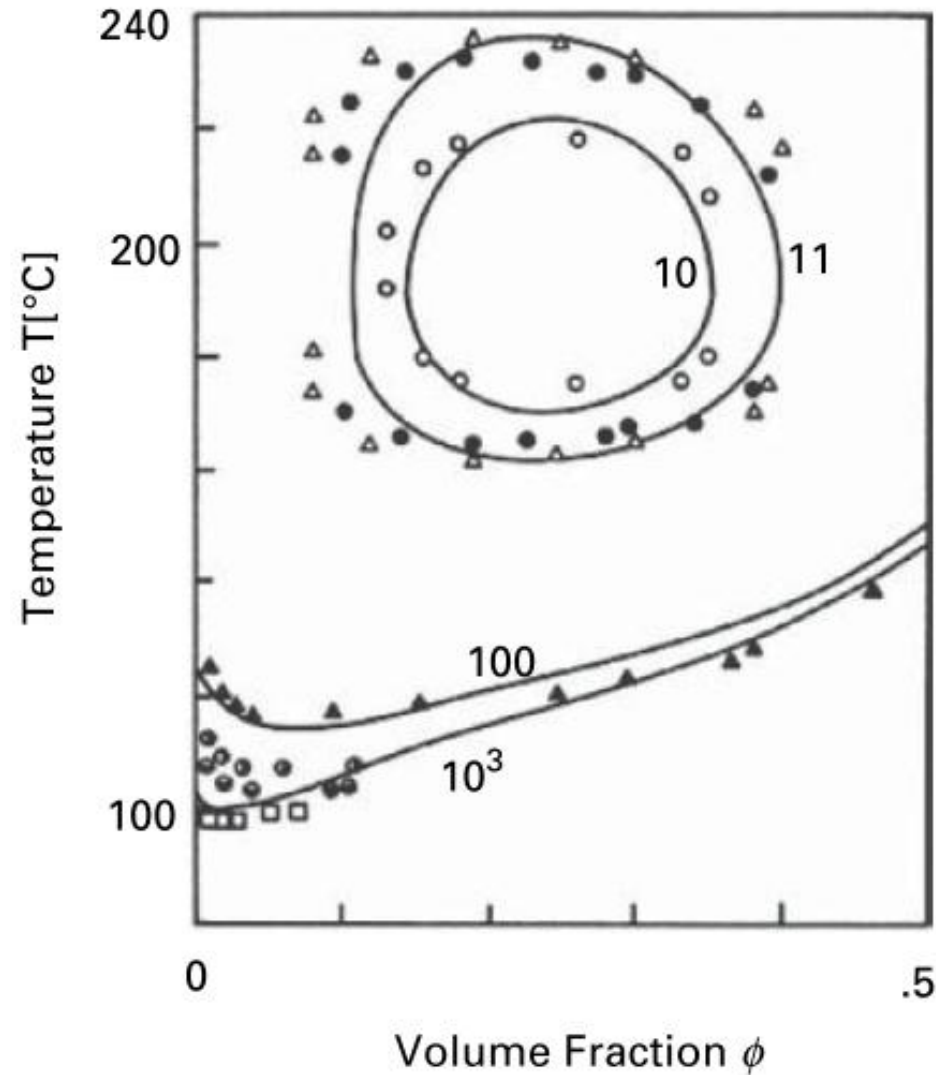


LCST

$$\chi = \frac{(Z-2)\Delta\epsilon_{12}}{kT} = \frac{A}{T} \quad A > 0$$

$$A < 0 ???$$

Phase diagram of aqueous solutions of PEO

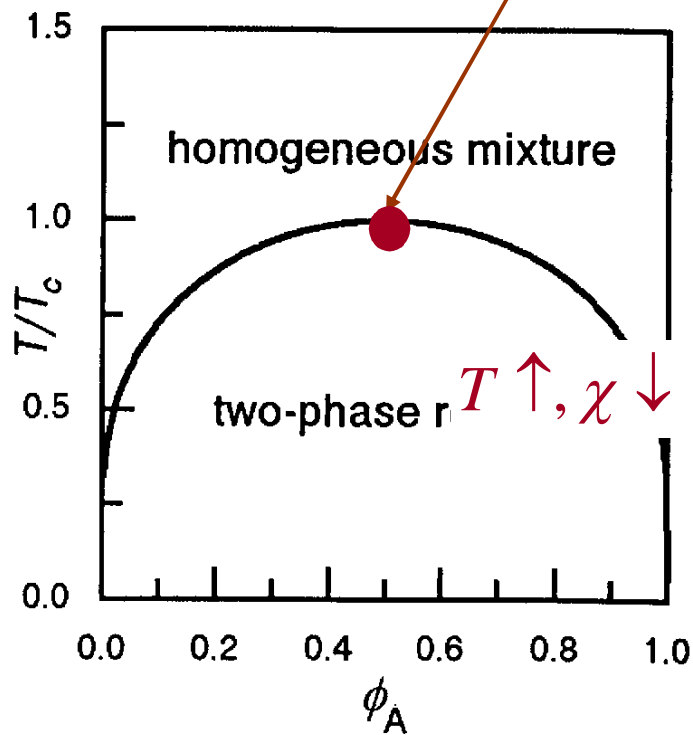


UCST/LCST

$$\Delta G = \chi \phi_1 \phi_2 - T \Delta S \quad \chi = \frac{A}{T}$$

Upper critical solution temperature (UCST)

$$A > 0$$



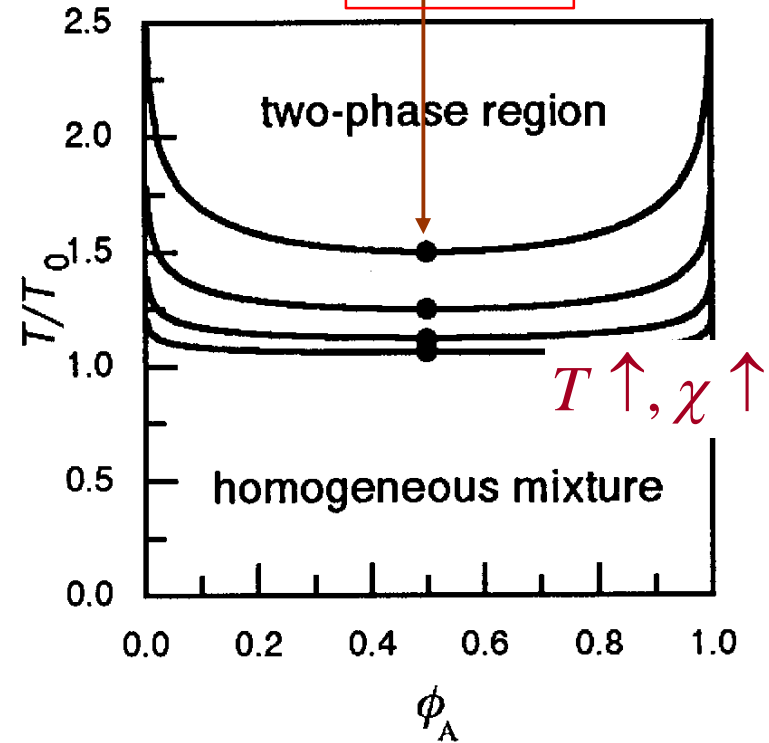
Endothermic symmetrical polymer mixture

Lower critical solution temperature (LCST)

$$A < 0$$

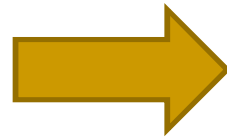
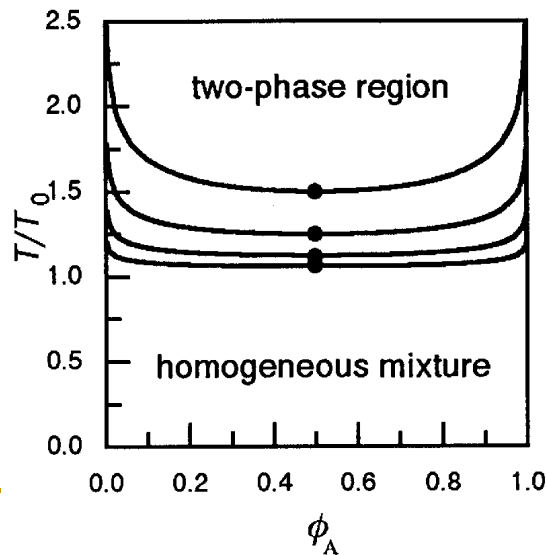
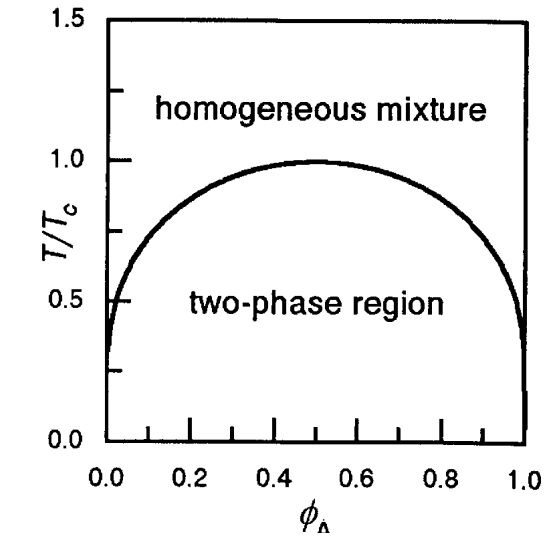
$$\chi = \frac{A}{T} + B$$

$$B > 0$$

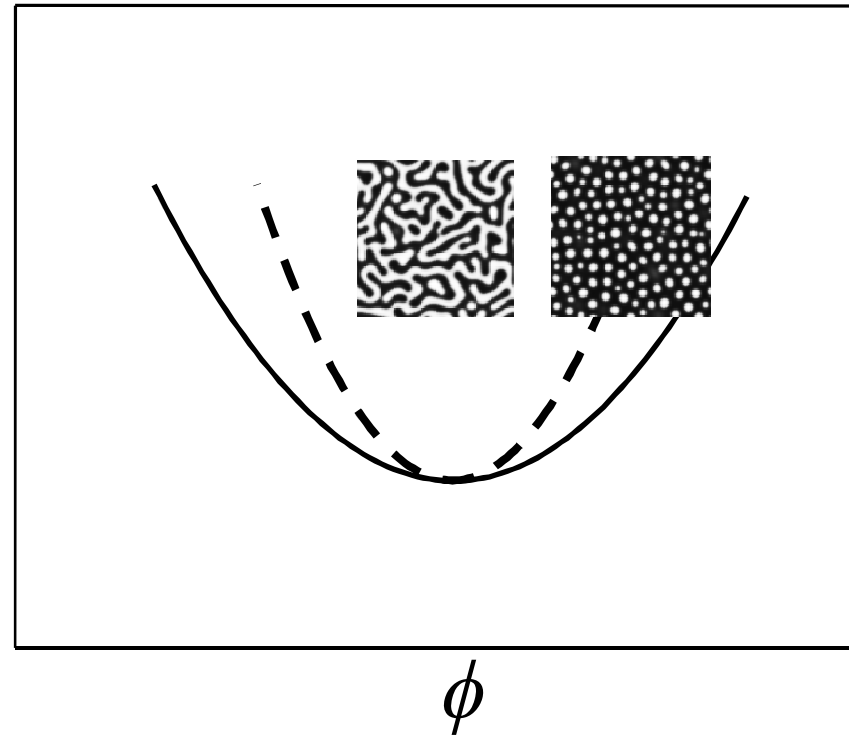


Exothermal symmetrical polymer mixture

Universal Phase Diagram



N or χN



Why UCST or LCST ?

$$\Delta G_{mix} = RTV \left(\frac{\phi_A}{N_A} \ln \phi_A + \frac{\phi_B}{N_B} \ln \phi_B + \chi \phi_A \phi_B \right) \longrightarrow \chi \text{ is the key issue.}$$

➤ Effective interaction parameter χ_{eff} :

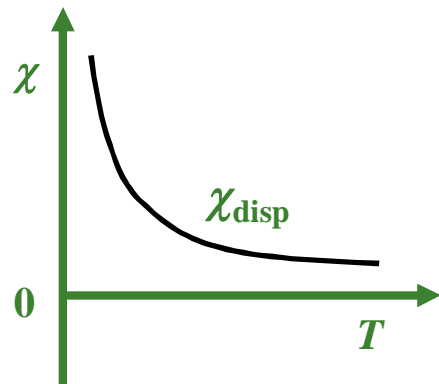
Dispersion forces

Free volume effects

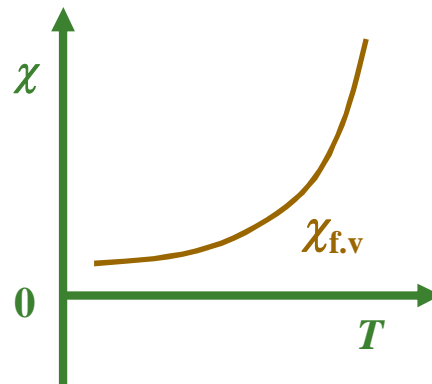
Specific interactions

$$\chi_{\text{eff}} = \chi_{\text{disp}} + \chi_{\text{f.v.}} + \chi_{\text{s.i.}} = \frac{A}{T} + B$$

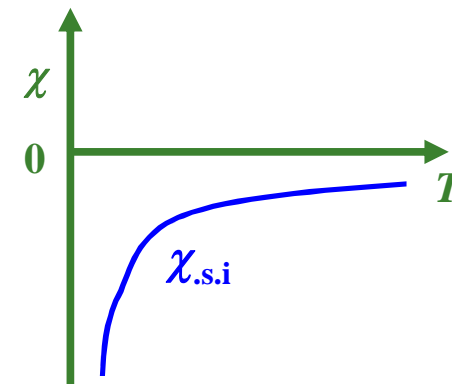
$A > 0$ UCST
 $A < 0$ LCST



Dispersion force:
~1/T monotonic decreasing,
 $\chi_{\text{disp}} \rightarrow 0$ as $T \rightarrow \infty$.



Free volume effect:
Monotonic increasing with T,
small, but positive at low T.

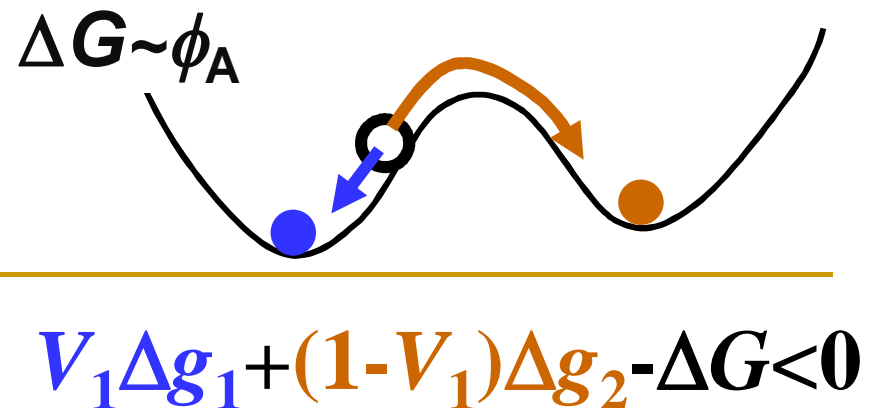
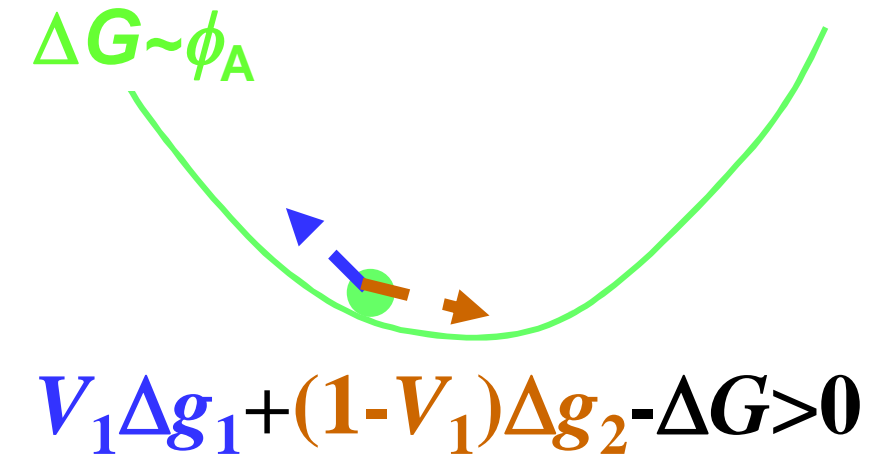
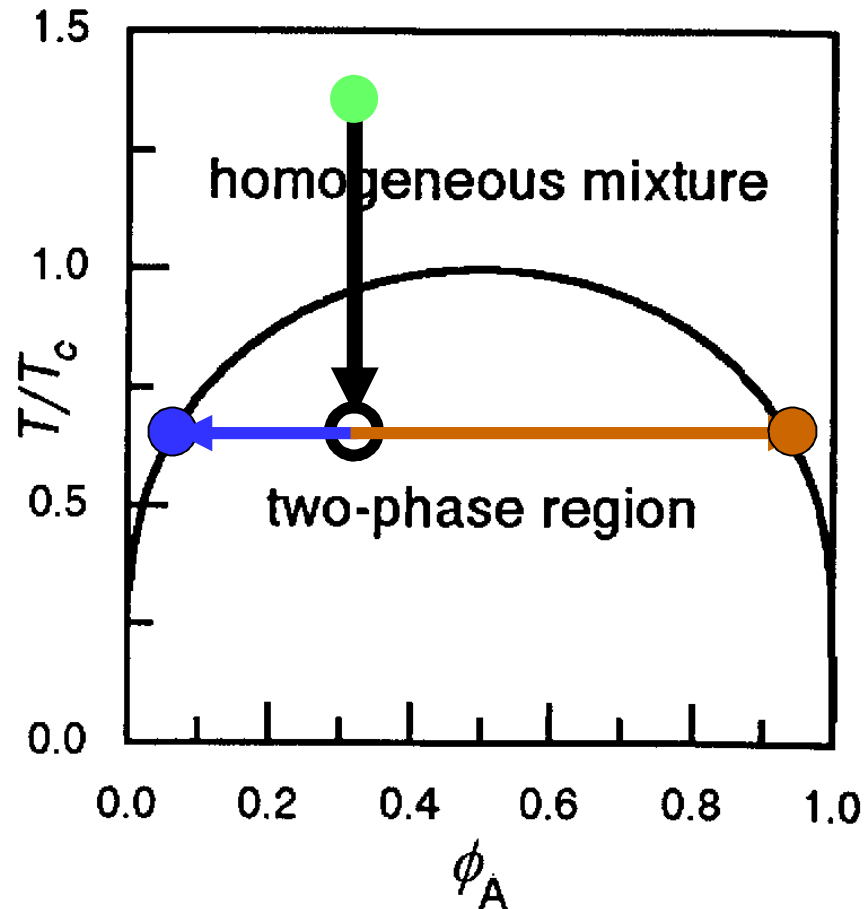


Specific interaction:
— Always < 0, decreasing
magnitude with increasing T.

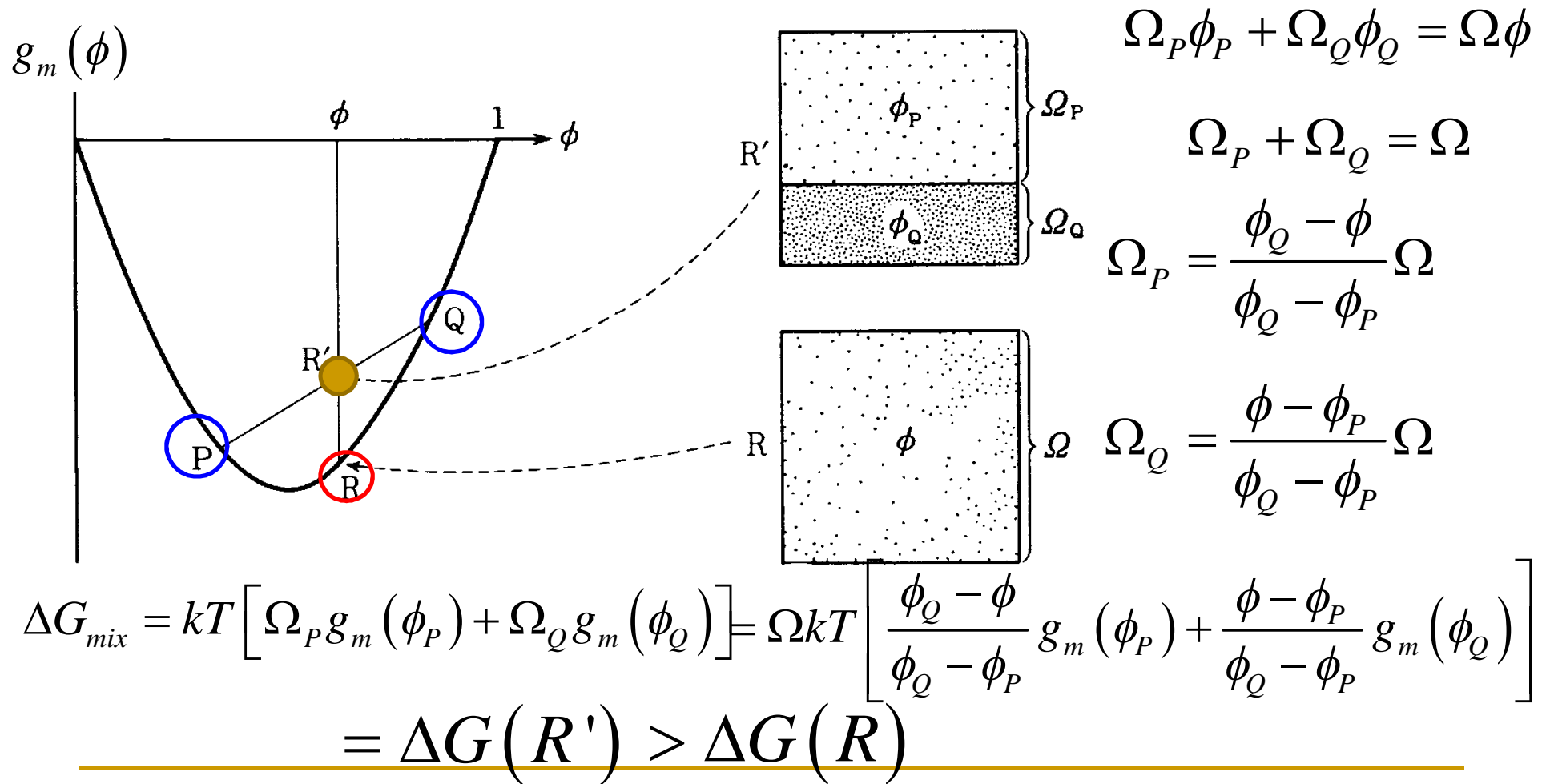
The Phase Behavior of Polymer Mixtures

How to judge it's homogeneous state or inhomogeneous state ?

What is the mechanism of phase separation?

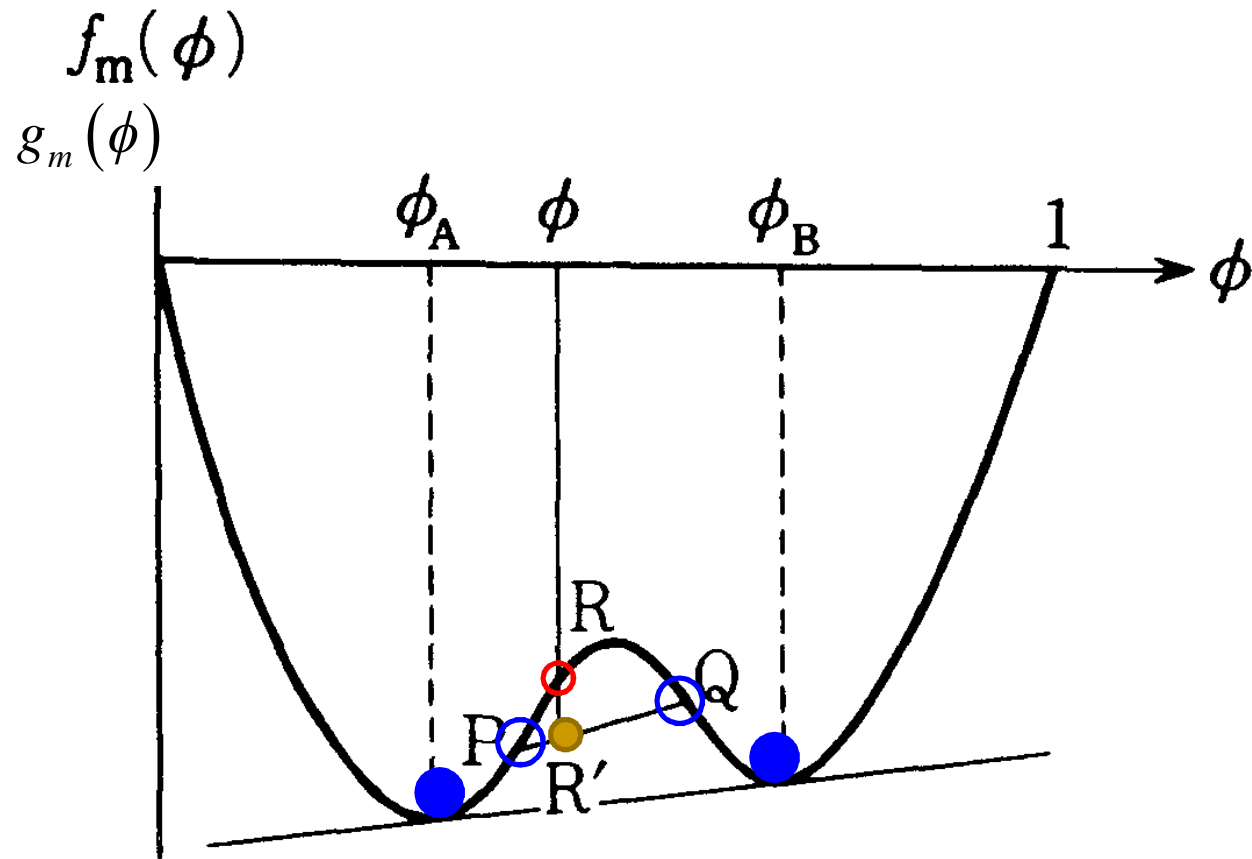


The shape of the mixing free energy curve with **one local minimum**



Phase Separation will not occur if free energy curve has **one local minimum**

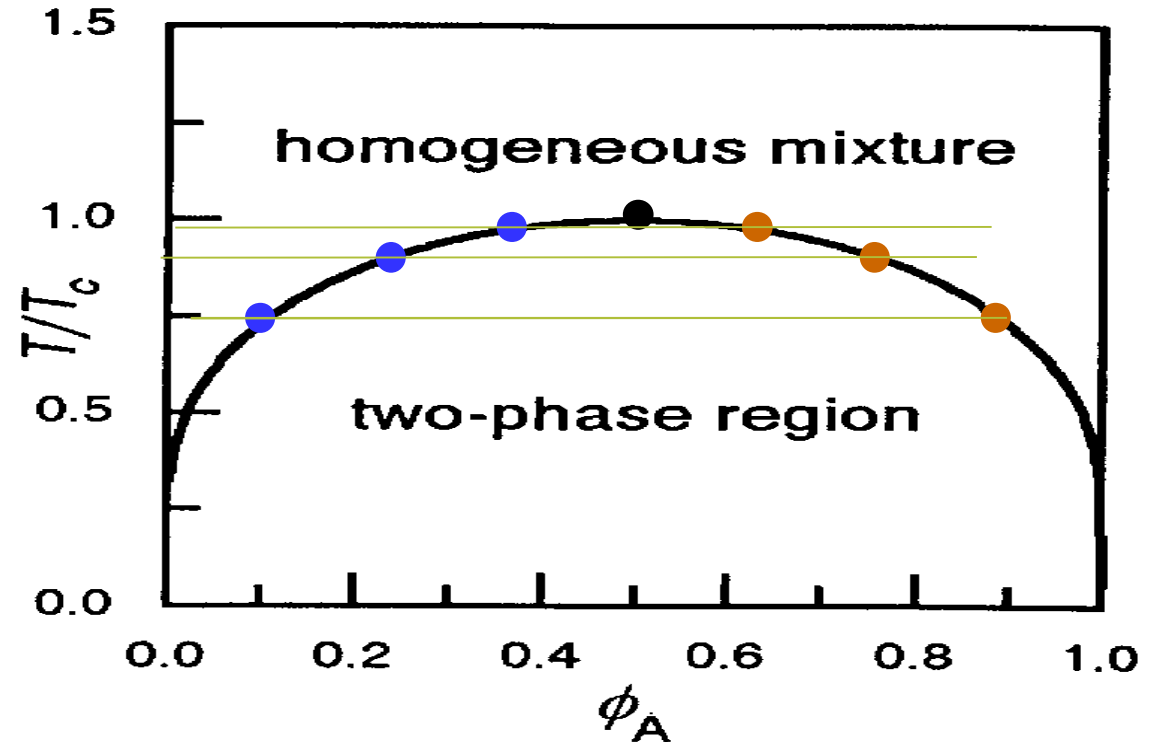
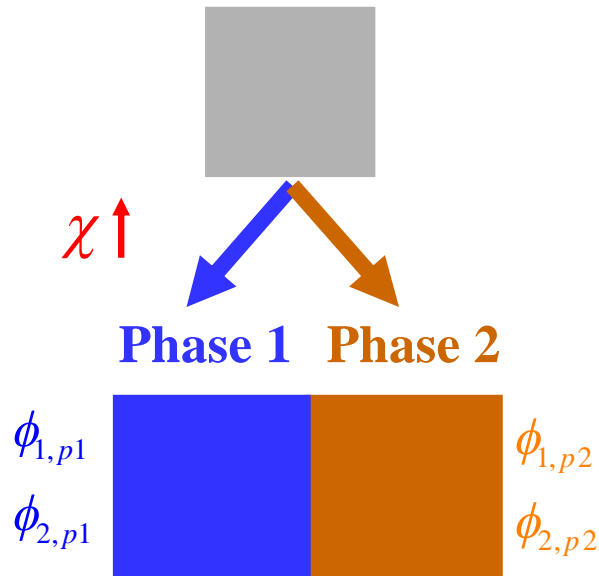
Free energy curve with two local minima



Phase Separation can take place if free energy curve has two local minima

$$\left[\frac{\partial g_m(\phi)}{\partial \phi} \right]_{\phi_A} = \left[\frac{\partial g_m(\phi)}{\partial \phi} \right]_{\phi_B} = \frac{g_m(\phi_B) - g_m(\phi_A)}{\phi_B - \phi_A}$$

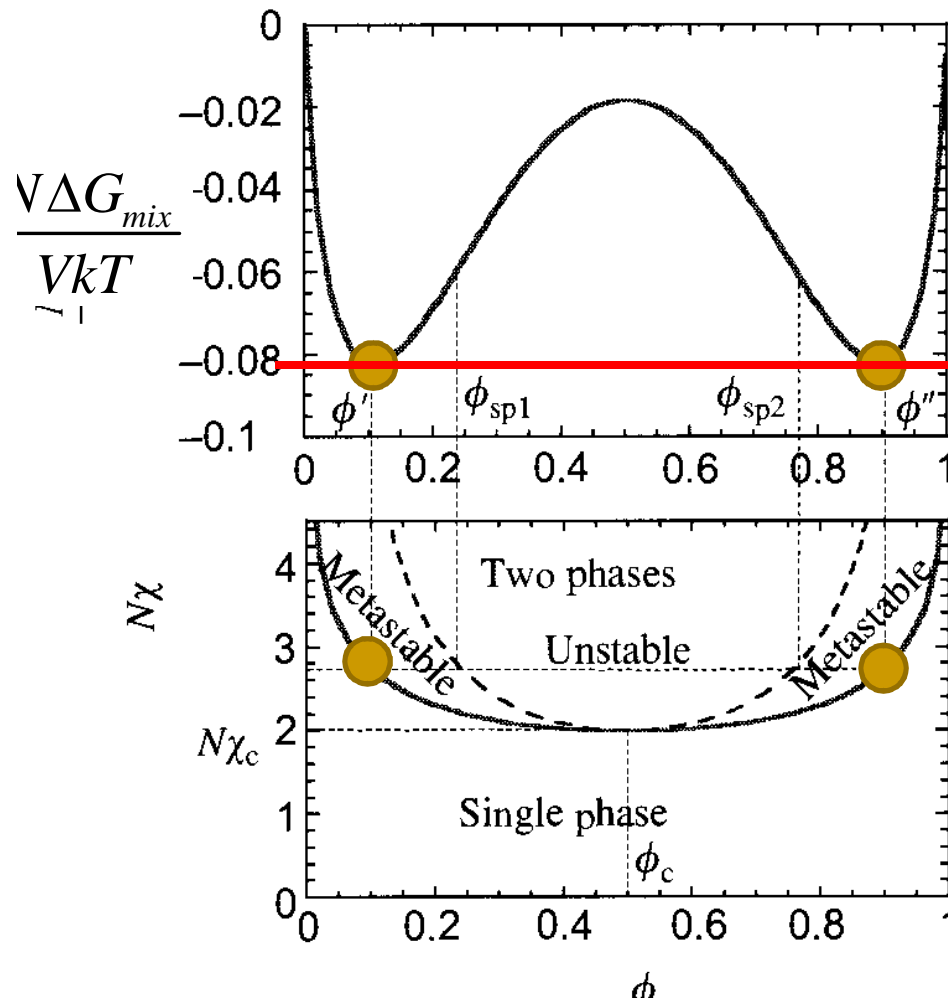
Phase Diagram and Phase Equilibrium



$$\begin{array}{l}
 \Delta\mu_{1,p1} = \Delta\mu_{1,p2} \\
 \Delta\mu_{2,p1} = \Delta\mu_{2,p2} \\
 \phi_{1,p1} + \phi_{2,p1} = 1 \\
 \phi_{1,p2} + \phi_{2,p2} = 1
 \end{array}
 \rightarrow
 \begin{array}{l}
 \ln(1 - \phi_{2,p1}) + \left(1 - \frac{x_1}{x_2}\right)\phi_{2,p1} + x_1\chi(\phi_{2,p1})^2 = \ln(1 - \phi_{2,p2}) + \left(1 - \frac{x_1}{x_2}\right)\phi_{2,p2} + x_1\chi(\phi_{2,p2})^2 \\
 \ln\phi_{2,p1} + \left(1 - \frac{x_2}{x_1}\right)(1 - \phi_{2,p1}) + x_2\chi(1 - \phi_{2,p1})^2 = \ln\phi_{2,p2} + \left(1 - \frac{x_2}{x_1}\right)(1 - \phi_{2,p2}) + x_2\chi(1 - \phi_{2,p2})^2
 \end{array}$$

I. Phase diagram of symmetric mixtures

$$\Delta G_{mix} = RTV \left(\frac{\phi}{N} \ln \phi + \frac{1-\phi}{N} \ln(1-\phi) + \chi \phi(1-\phi) \right) \quad \frac{\partial \Delta G_{mix}}{\partial \phi} = 0$$



$$= RTV \left(\frac{\ln \phi}{N} + \frac{1}{N} - \frac{\ln(1-\phi)}{N} - \frac{1}{N} + \chi_b (1-2\phi) \right)$$

$$= RTV \left(\frac{1}{N} \ln \frac{\phi}{(1-\phi)} + \chi_b (1-2\phi) \right) = 0$$

$$\chi_b N = \frac{1}{(2\phi-1)} \frac{\ln \phi}{\ln(1-\phi)}$$

$$\chi_b = \frac{A}{T_b} + B$$

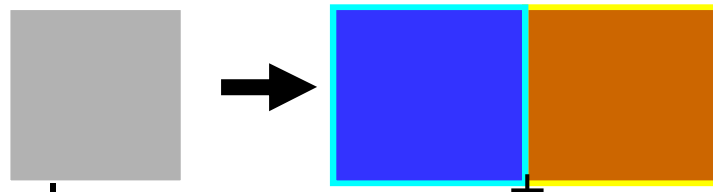
$$T_b = \frac{A}{\frac{1}{N(2\phi-1)} \ln \frac{\phi}{(1-\phi)} - B}$$

II. Phase diagram of asymmetric mixtures

$$\Delta G_{mix} = RTV \left(\frac{\phi}{N_1} \ln \phi + \frac{1-\phi}{N_2} \ln(1-\phi) + \chi \phi(1-\phi) \right)$$

$$d\Delta G = \Delta\mu_1 dn_1 + \Delta\mu_2 dn_2$$

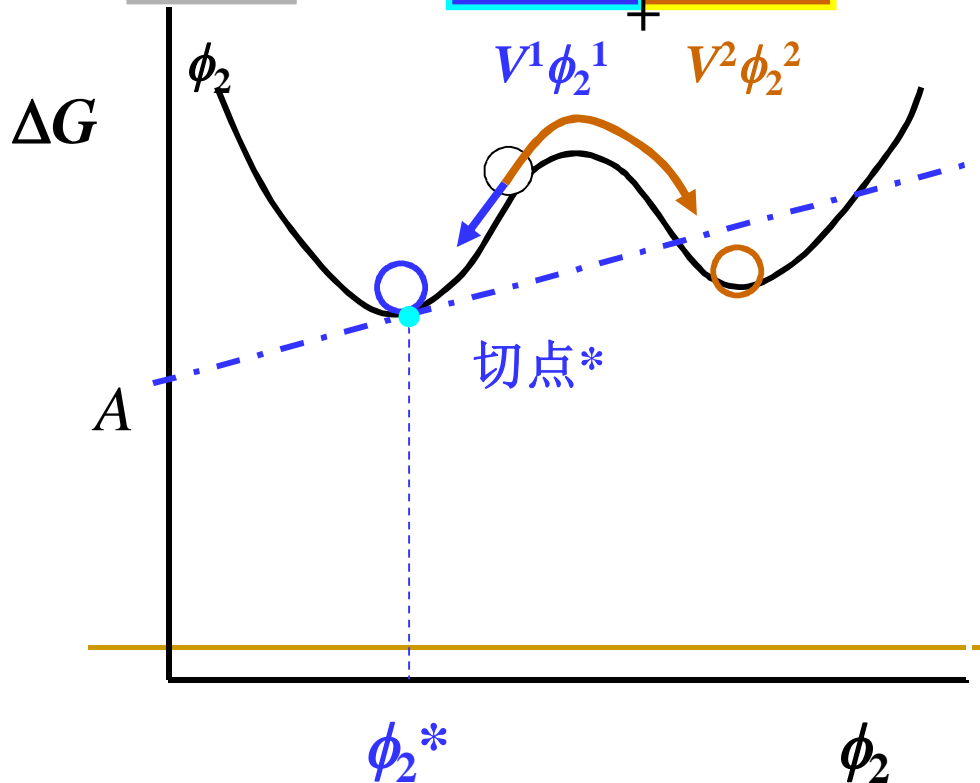
$$\Delta G = n_1 \Delta\mu_1 + n_2 \Delta\mu_2$$



$$\Delta\mu_1^1 = \Delta\mu_1^2$$

$$\Delta\mu_2^1 = \Delta\mu_2^2$$

$$\phi_1 = \frac{n_1 x_1 V_s}{V_m}, \quad \phi_2 = \frac{n_2 x_2 V_s}{V_m}, \quad \phi_1 = 1 - \phi_2$$



$$\Delta G = \phi_1 \frac{V_m}{V_s} x_1^{-1} \Delta\mu_1 + \phi_2 \frac{V_m}{V_s} x_2^{-1} \Delta\mu_2$$

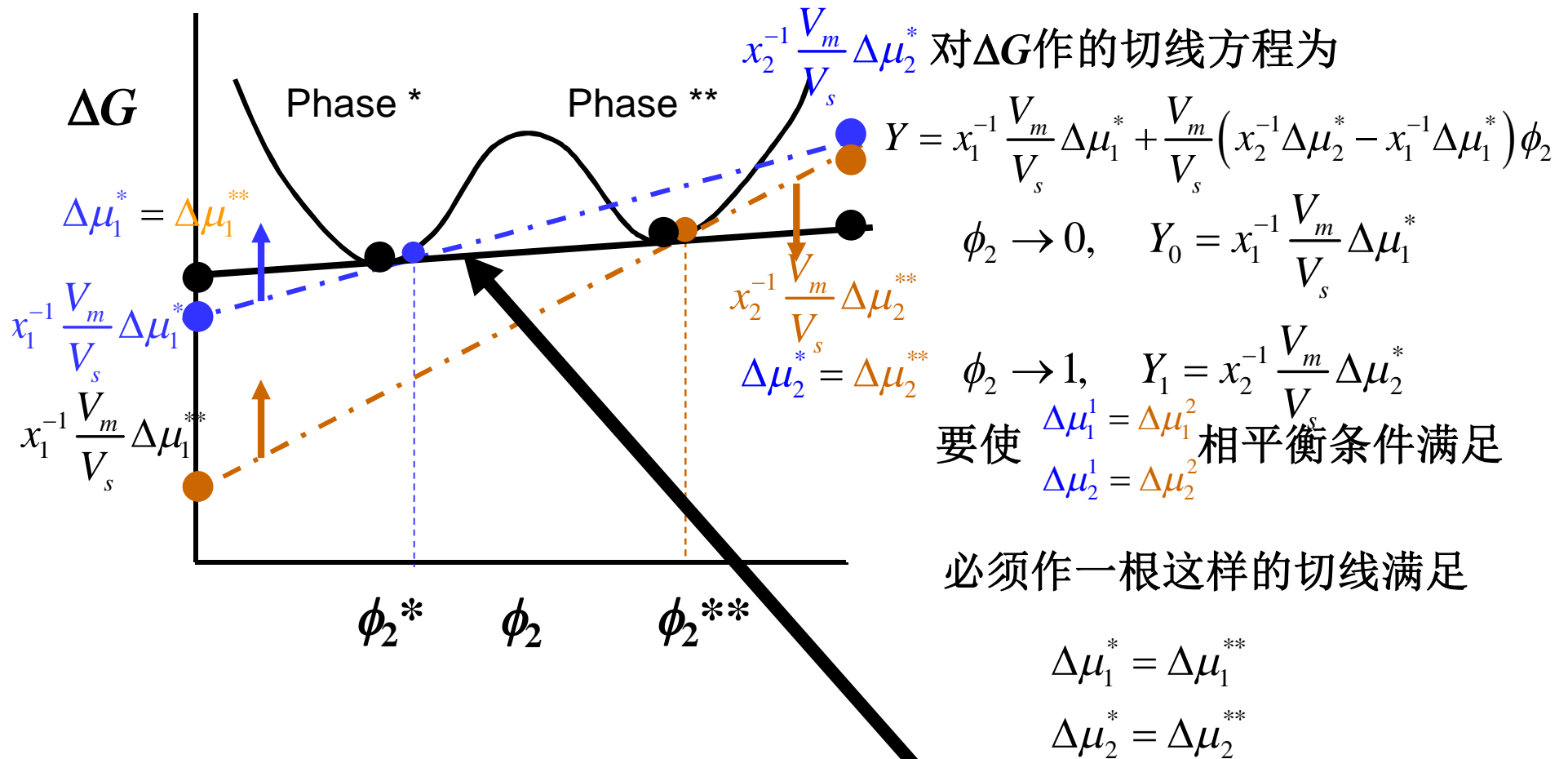
$$= \frac{V_m}{V_s} \left[x_1^{-1} \Delta\mu_1 + \phi_2 \left(x_2^{-1} \Delta\mu_2 - x_1^{-1} \Delta\mu_1 \right) \right]$$

对 ΔG 作切线 $Y=A+B\phi_2$, 切点 ϕ_2^*

斜率 B $B = \left(\frac{\partial \Delta G}{\partial \phi_2} \right)^* = \frac{V_m}{V_s} \left(x_2^{-1} \Delta\mu_2^* - x_1^{-1} \Delta\mu_1^* \right)$

$$\Delta G^* = A + B\phi_2^* \rightarrow A = x_1^{-1} \frac{V_m}{V_s} \Delta\mu_1^*$$

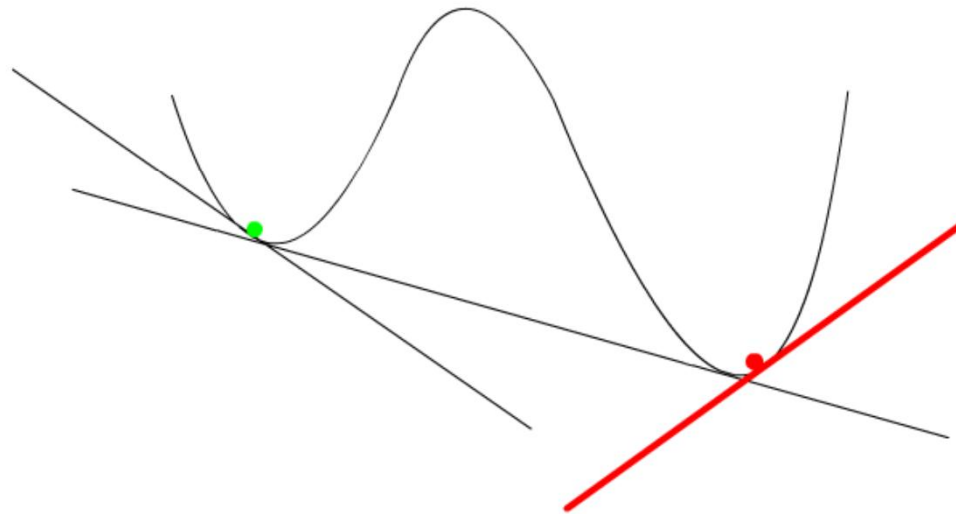
Finding the phase equilibrium conditions



唯有同时通过两个切点的共切线才能满足相平衡条件

Search the phase equilibrium point

$$\Delta\mu_1^* = \Delta\mu_1^{**}$$

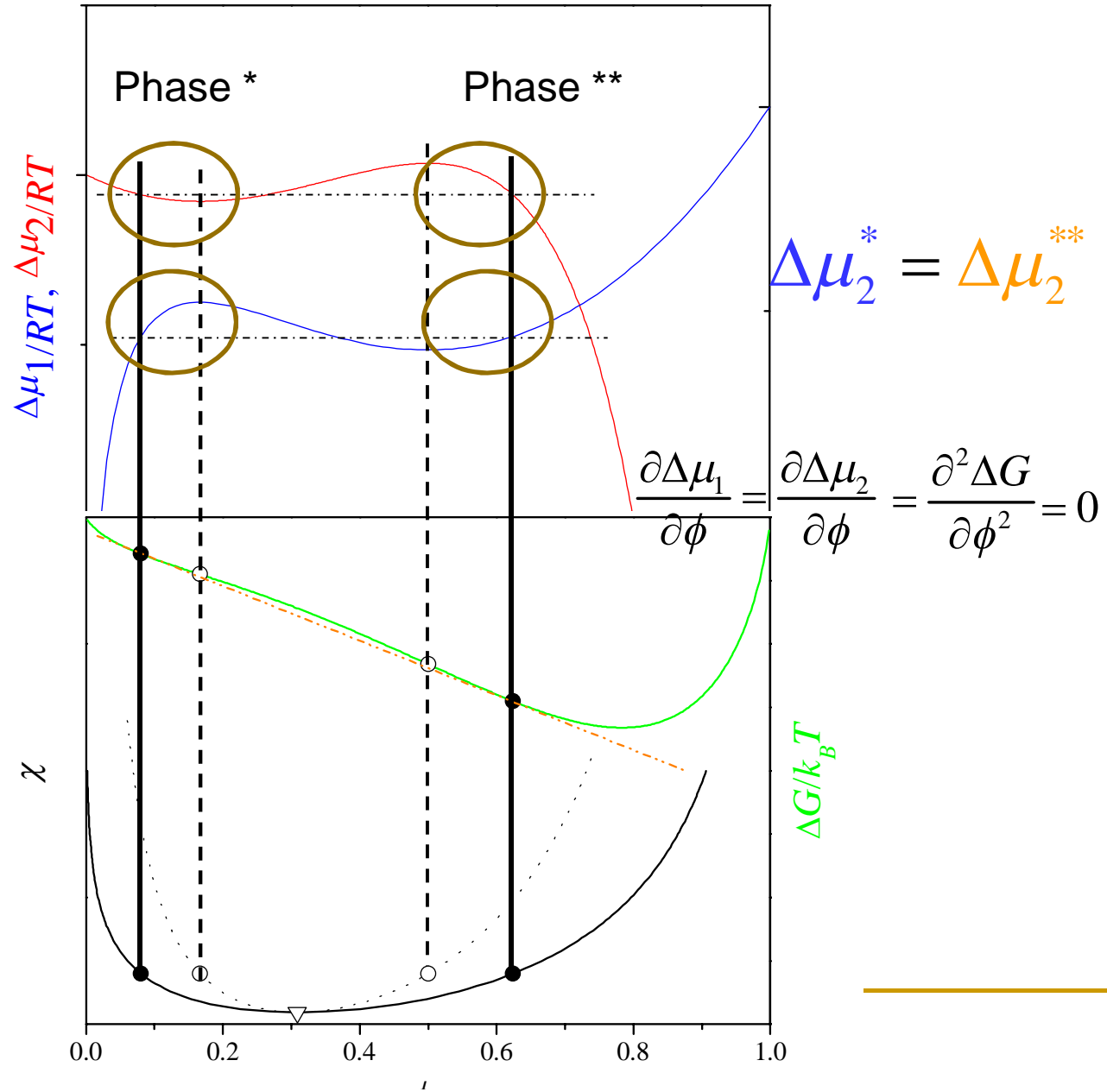


$$\mu_2^* = \Delta\mu_2^{**}$$

Relations between Free Energy, Chemical Potentials and Phase Diagram

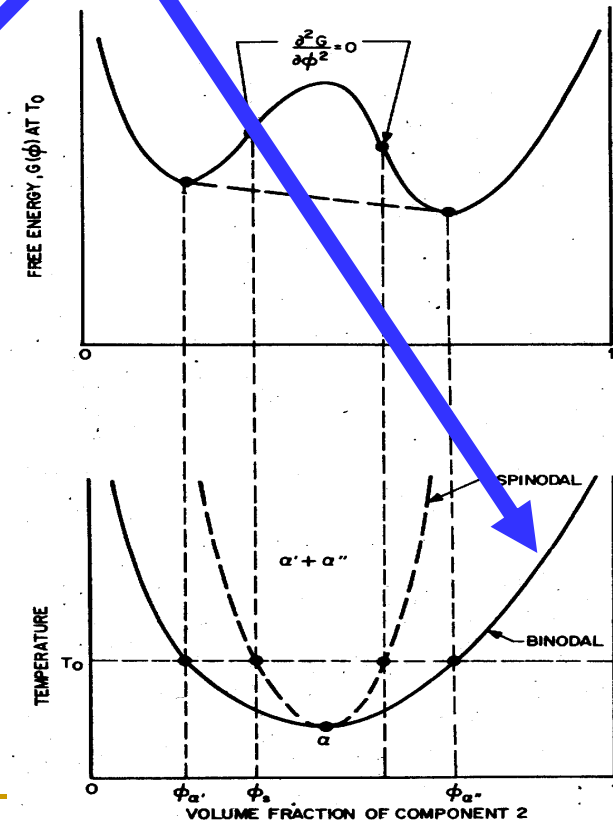
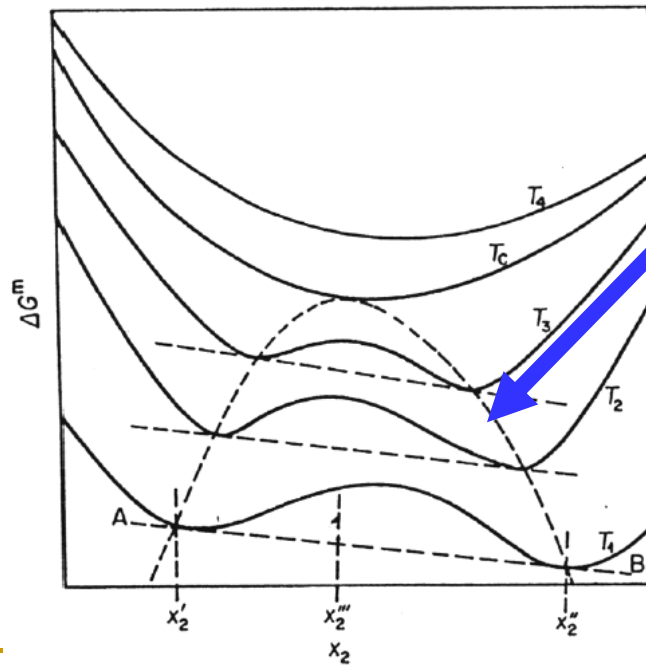
$$\Delta\mu_1^* = \Delta\mu_1^{**}$$

$$\Delta\mu_2^* = \Delta\mu_2^{**}$$

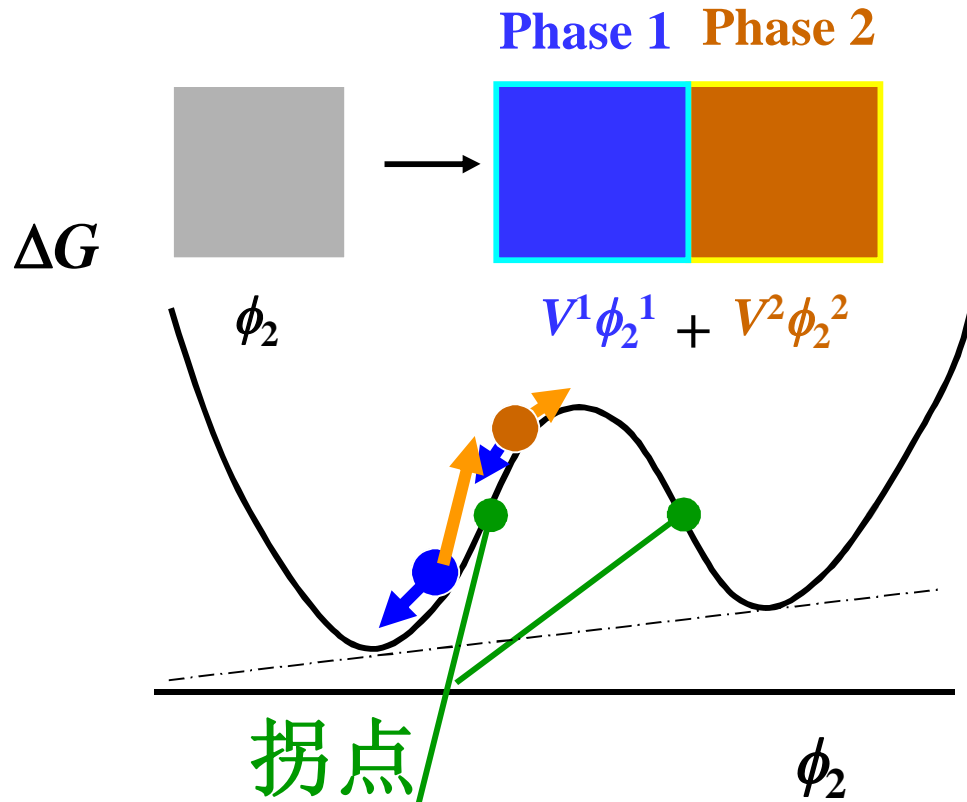


(1) Phase equilibrium curve – binodal

作 $T(x) \sim [\phi_2^*(T), \phi_2^{**}(T)] \longrightarrow$ binodal curve

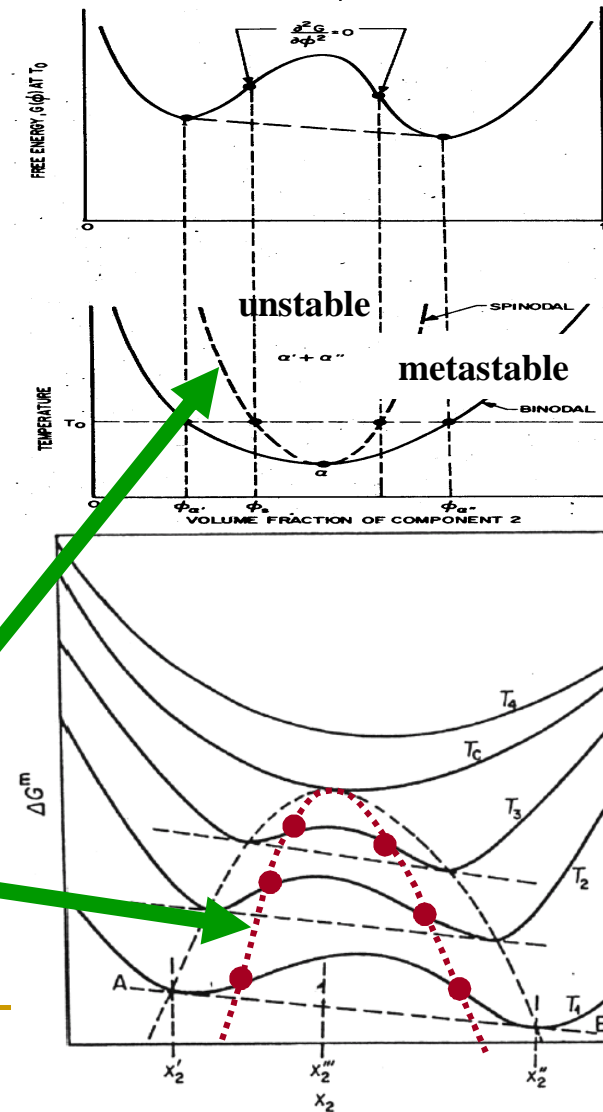


(2) Metastable/unstable limits - spinodal



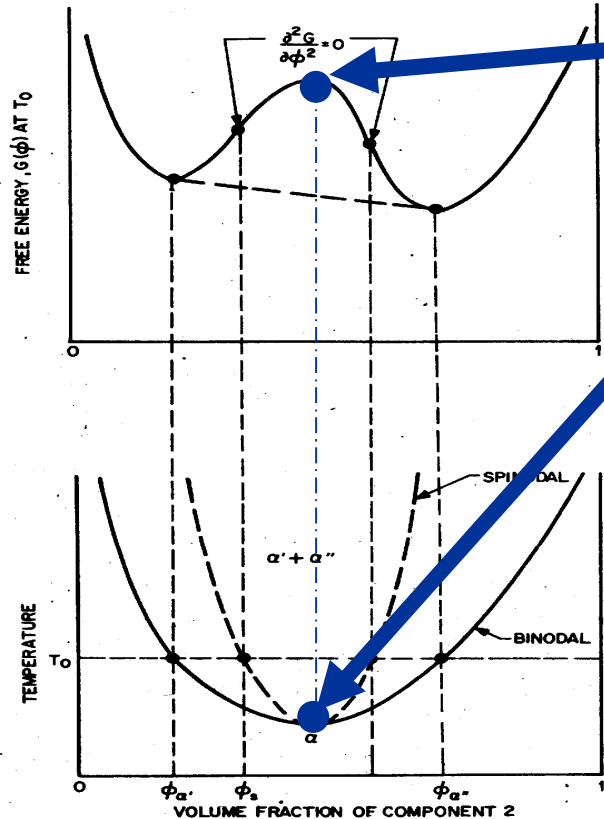
$$\frac{\partial^2 \Delta G}{\partial \phi_2^2} = 0 \quad \text{Spinodal curve}$$

$$\frac{\partial^2 \Delta G}{\partial \phi_2^2} = \frac{1}{x_1(1-\phi_2)} + \frac{1}{x_2\phi_2} - 2\chi = 0$$



(3) Critical point

Spinodal 和 binodal的交点: Critical point



$$\frac{\partial^3 \Delta G}{\partial \phi_2^3} = \frac{\partial}{\partial \phi_2} \left[\frac{1}{x_1(1-\phi_2)} + \frac{1}{x_2\phi_2} - 2\chi \right] = 0$$

$$\phi_{2,c} = \frac{x_1^{1/2}}{x_1^{1/2} + x_2^{1/2}}, \quad \chi_c = \frac{1}{2} \left(\frac{1}{x_1^{1/2}} + \frac{1}{x_2^{1/2}} \right)^2$$

For symmetric blends $x_1=x_2$

$$\chi_c N = 2$$

For polymer solutions

$$\chi_c \rightarrow \frac{1}{2}$$

For symmetric di-blocks $f=0.5$

$$\chi_c N = 10.5$$

Critical points dependence of N

For blends

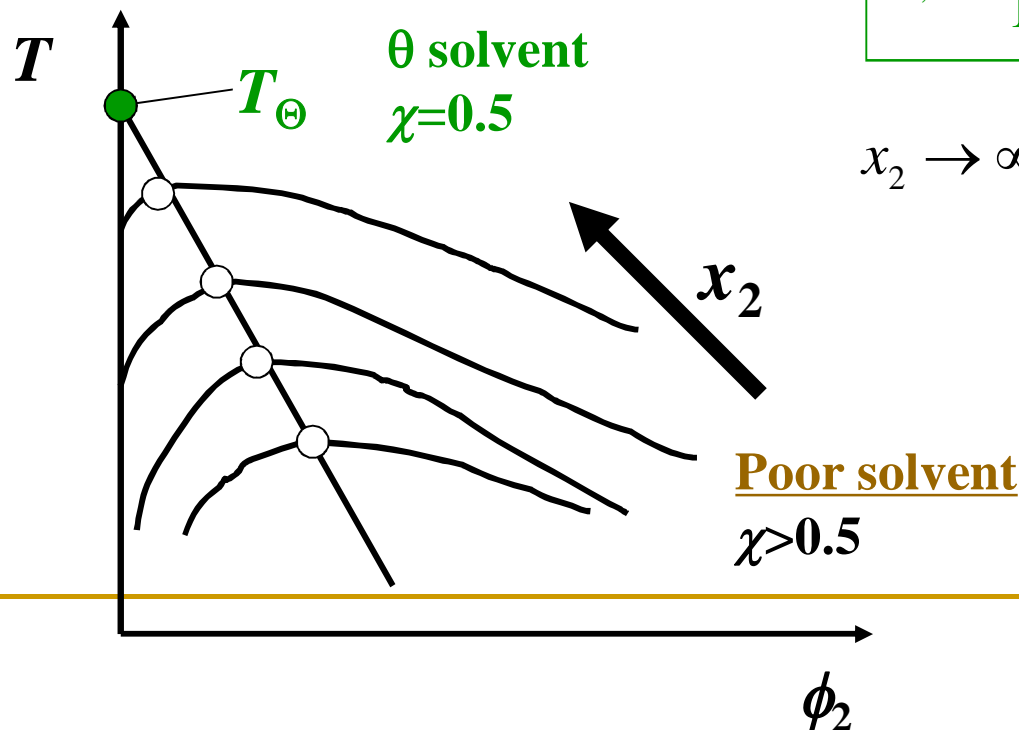
$$\phi_{2,c} = \frac{x_1^{1/2}}{x_1^{1/2} + x_2^{1/2}}, \quad \chi_c = \frac{1}{2} \left(\frac{1}{x_1^{1/2}} + \frac{1}{x_2^{1/2}} \right)^2$$

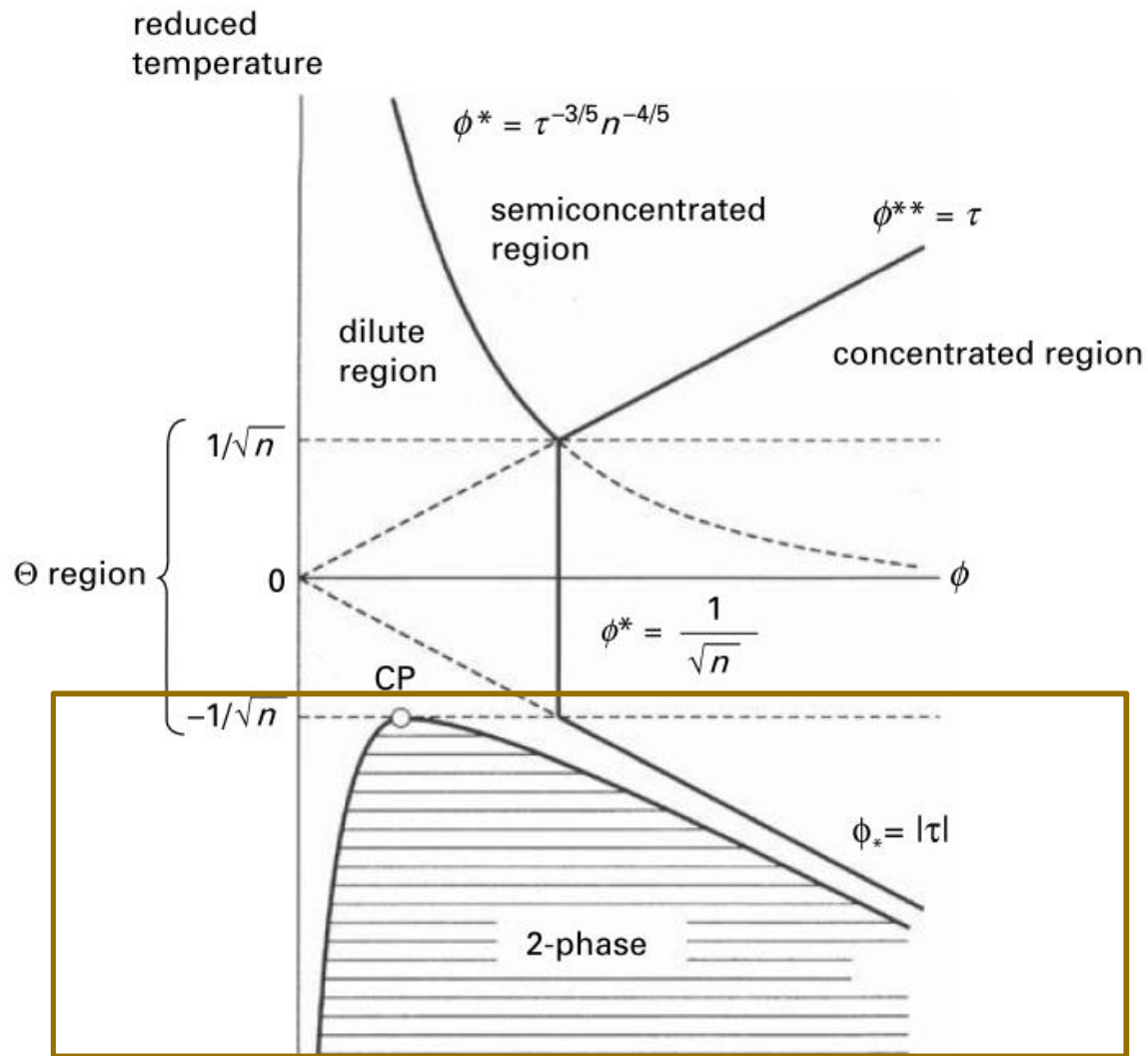
$$x \uparrow \rightarrow \chi_c \downarrow, \quad T_c \uparrow$$

For solutions

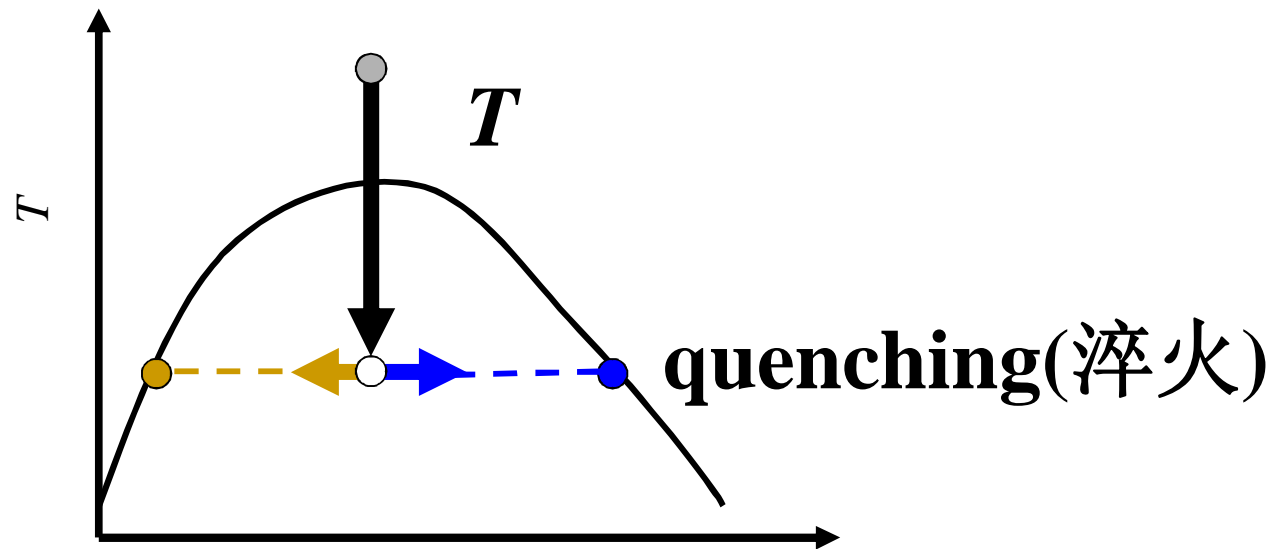
$$\phi_{2,c} = \frac{1}{1 + x_2^{1/2}}, \quad \chi_c = \frac{1}{2} \left(1 + \frac{1}{x_2^{1/2}} \right)^2$$

$$x_2 \rightarrow \infty, \quad \phi_{2,c} \rightarrow 0, \quad \chi_c \rightarrow \frac{1}{2}$$





Phase Separation Dynamics



达到两相最终平衡的动力学过程

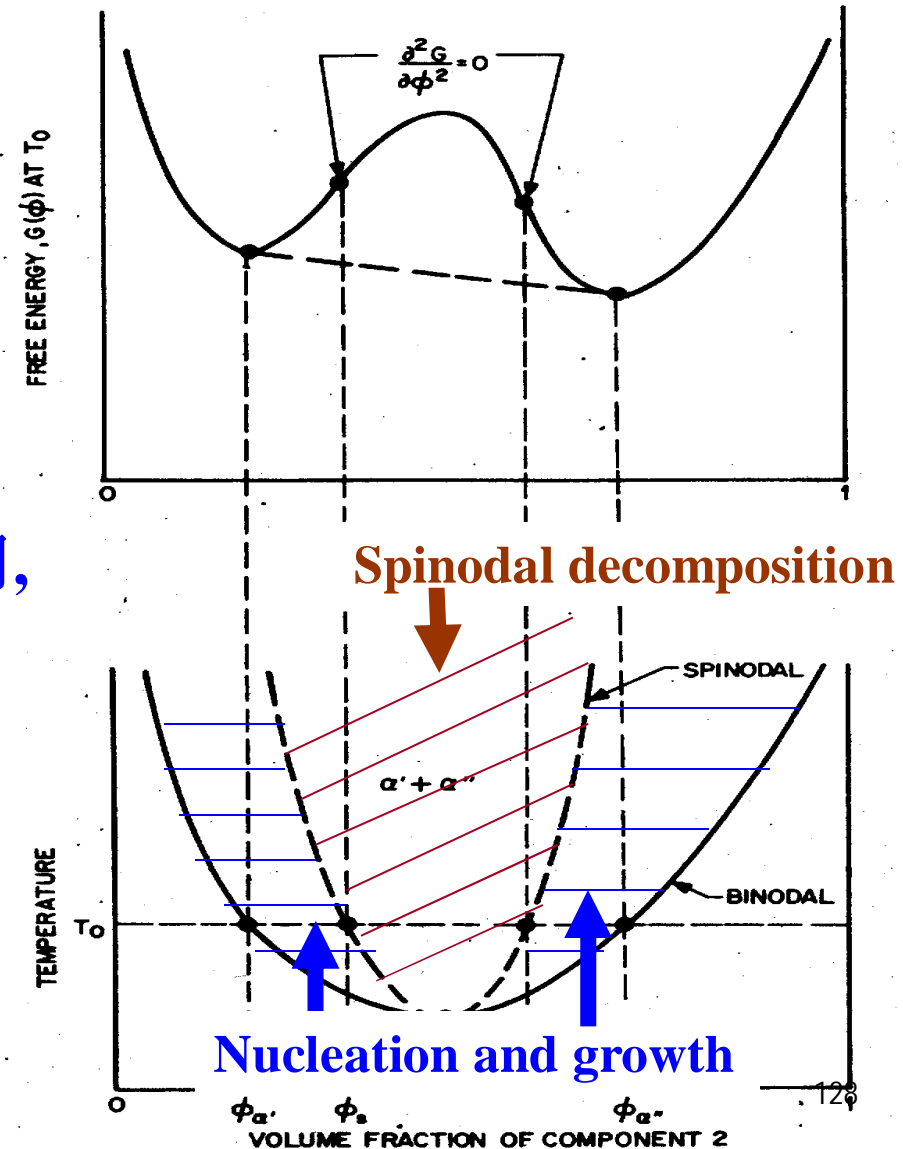
与初始状态的浓度有关

- (1) 在临界组成附近, 不稳区, **spinodal decomposition**
- (2) 在相平衡线和spinodal线之间, 亚稳区, **nucleation and growth**

Phase diagram and phase separation mechanisms

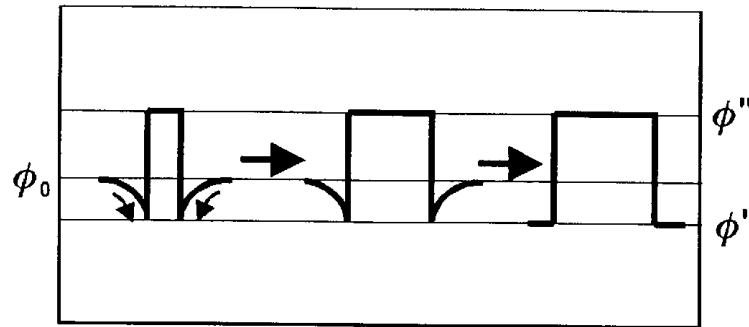
(1) 在临界组成附近, 不稳区,
spinodal decomposition

(2) 在相平衡线和spinodal线之间,
亚稳区, **nucleation and growth**

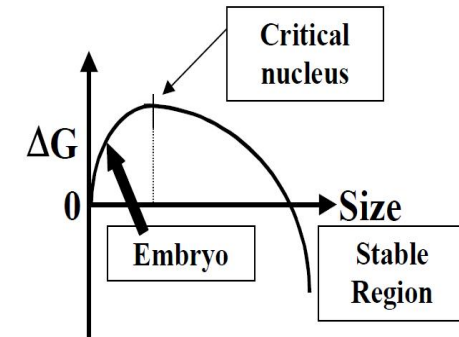


Phase Separation Mechanisms

1. Nucleation and growth (成核生长) mechanism

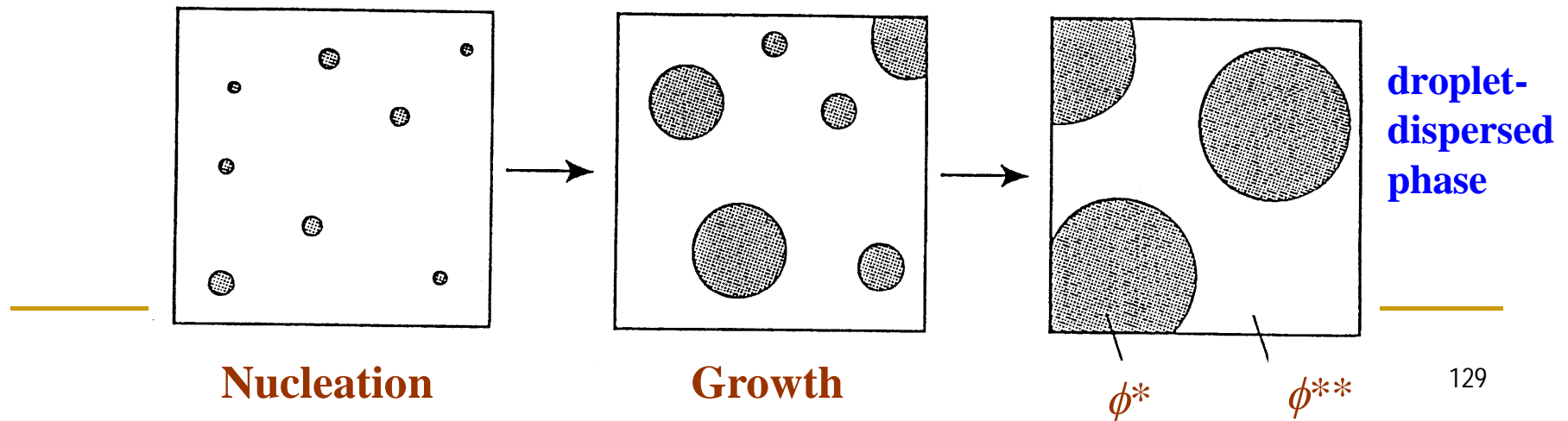


In metastable region, separation can proceed only by overcoming the barrier with a large fluctuation in composition.



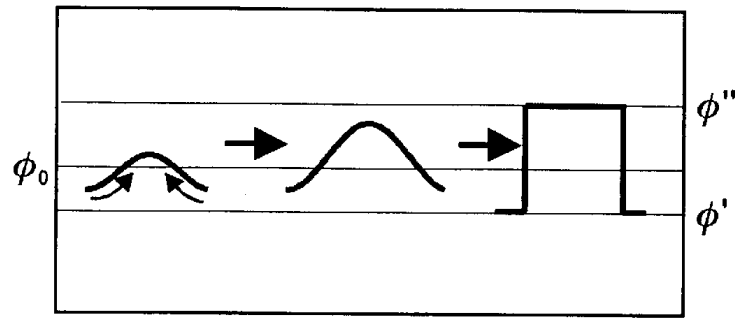
Nucleation barrier: $\Delta G(r) = -\frac{4\pi}{3}r^3\Delta g + 4\pi r^2\gamma$ with $\Delta g = \Delta g(\phi_0) - \Delta g(\phi'')$

r : radius of the nuclear; γ : excess free energy per unit surface area.

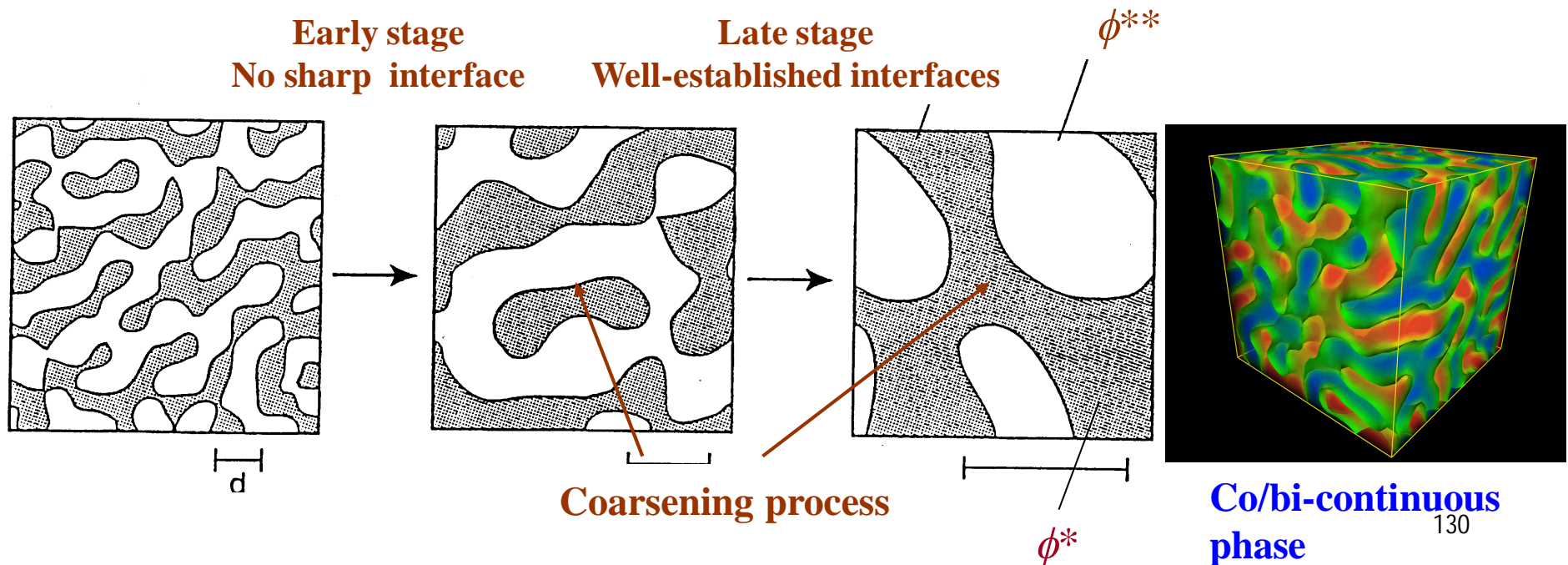


Phase Separation Mechanisms

2. Spinodal decomposition (亚稳极限分解) mechanism



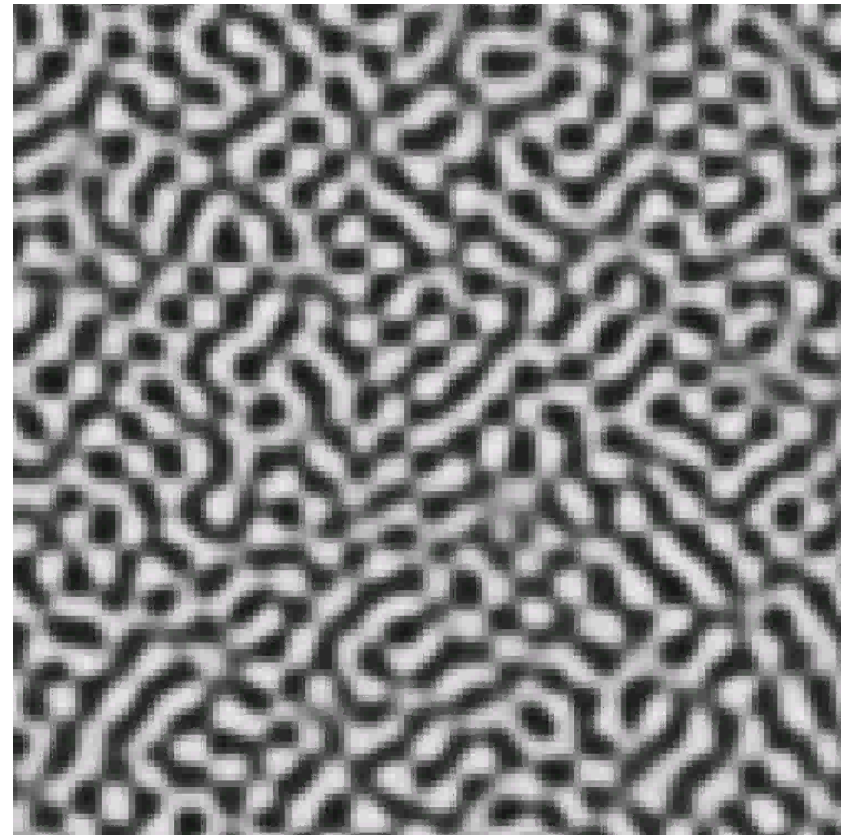
In unstable region, separation can occur spontaneously and continuously without any thermodynamic barrier.



Examples of Phase Separation Dynamics

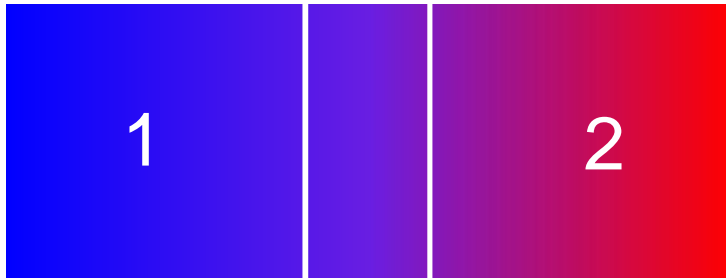


Nucleation & Growth



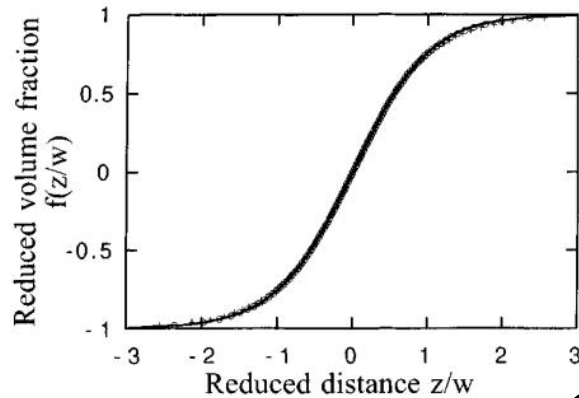
Spinodal Decomposition

Interfaces between weakly immiscible polymers



A-rich

B-rich



interfacial tension is defined as the increase in Gibbs free energy of the whole system per unit increase in interfacial area

$$\gamma = \left(\frac{\partial G}{\partial A} \right)_{T,p,n}$$

for each i phase

$$dG^i = -S^i dT + V^i dp + \mu_A dn_A^i + \mu_B dn_B^i$$

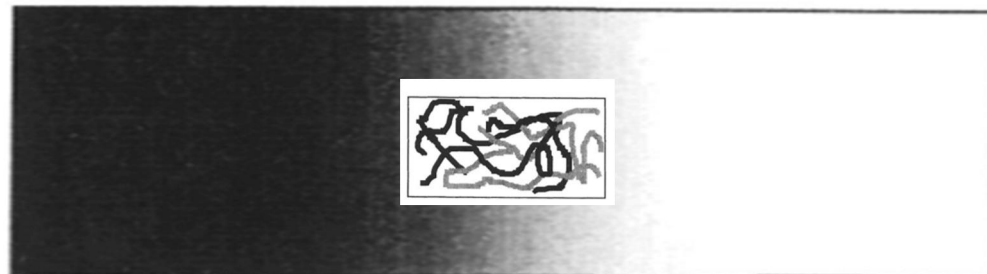
$$G^i = \mu_A n_A^i + \mu_B n_B^i \quad \mu_A^1 = \mu_A^2 = \mu_A^{\text{int}}$$

$$\mu_B^1 = \mu_B^2 = \mu_B^{\text{int}}$$

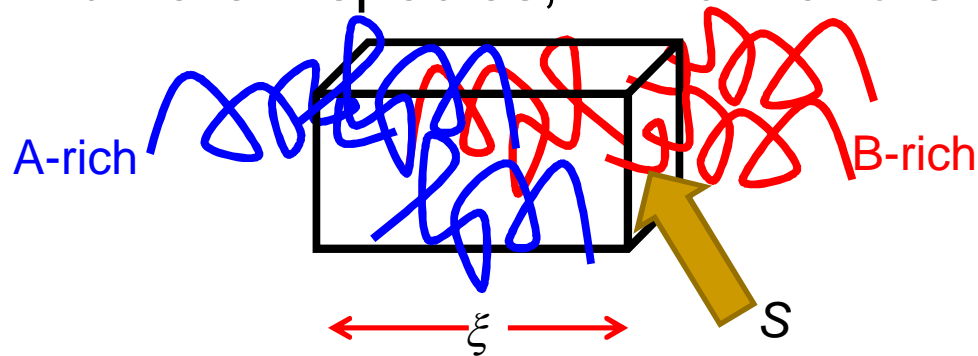
for interfacial region

$$G^{\text{int}} = \gamma A + n_A^{\text{int}} \mu_A + n_B^{\text{int}} \mu_B$$

$$\gamma = \frac{G^{\text{int}}}{A} - (\Gamma_A \mu_A + \Gamma_B \mu_B) \quad \Gamma_A = \frac{n_A^{\text{int}}}{A} \quad \Gamma_B = \frac{n_B^{\text{int}}}{A}$$



The width of the interface is determined by a balance of **chain entropy**, favoring a wider interface, and the unfavorable energy of **interaction** between the two different species, which favors a narrow interface.



Suppose a loop of the **A** polymer with N_{loop} units protrudes into the **B** side of the interface

$$G_{loop} \approx N_{loop} \chi_{AB} k_B T \approx k_B T \quad N_{loop} \chi_{AB} \approx 1$$

$$\text{Interfacial width: } \xi \approx 2R_{g,loop} = \frac{2bN_{loop}^{1/2}}{\sqrt{6}} \quad \xi \approx \frac{2b}{\sqrt{6\chi_{AB}}} \quad b: \text{Kuhn segment}$$

$$\gamma_{AB} = \rho_A V \chi_{AB} k_B T / S \quad V = S\xi / 2 \quad \text{Segment density: } \rho_A = \frac{N}{Nb^3}$$

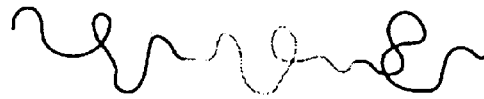
$$\gamma_{AB} \approx \frac{k_B T}{b^2} \sqrt{\frac{\chi_{AB}}{6}}$$

(Helfand, E.; Tagami, Y. *JPS, PL*, 1971, 9, 741)

4.3 Thermodynamics of Block Copolymers



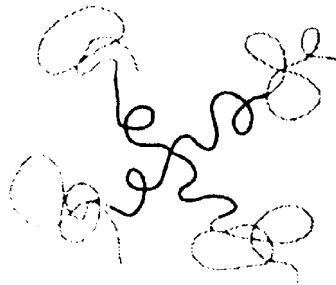
diblock



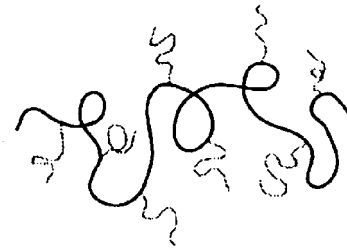
triblock



random multiblock



four arm starblock



graft copolymer

Applications:

Thermoplastics (热塑性弹性体): PU, SBS

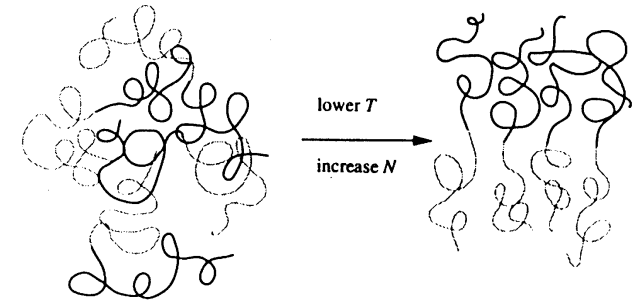
Compabilizier (相容剂) of Polymer Blends

Nanotechnology, Biomaterials...

Self-assembly of Diblock Copolymers

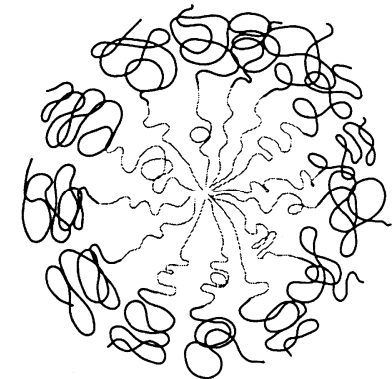
➤ Melts

Microphase (mesophase, nanophase) separation (微相分离) is driven by chemical incompatibilities between the different blocks that make up block copolymer molecules.



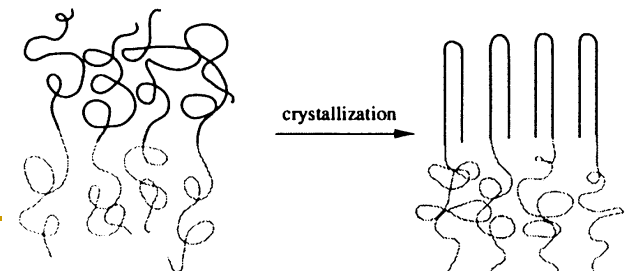
➤ Solutions

Micellization (胶束化) occurs when block copolymer chains associate into, often spherical, micelles (胶束) in dilute solution in a selective solvent (选择性溶剂). In concentrated solution, micelles can order into gels (凝胶).



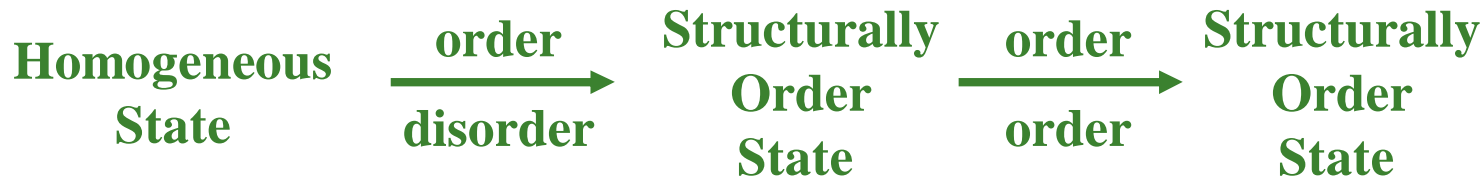
➤ Solids

Crystallization of the crystalline block from melt often leads to a distinct (usually lamellar (片晶)) structure, with a different periodicity from the melt .

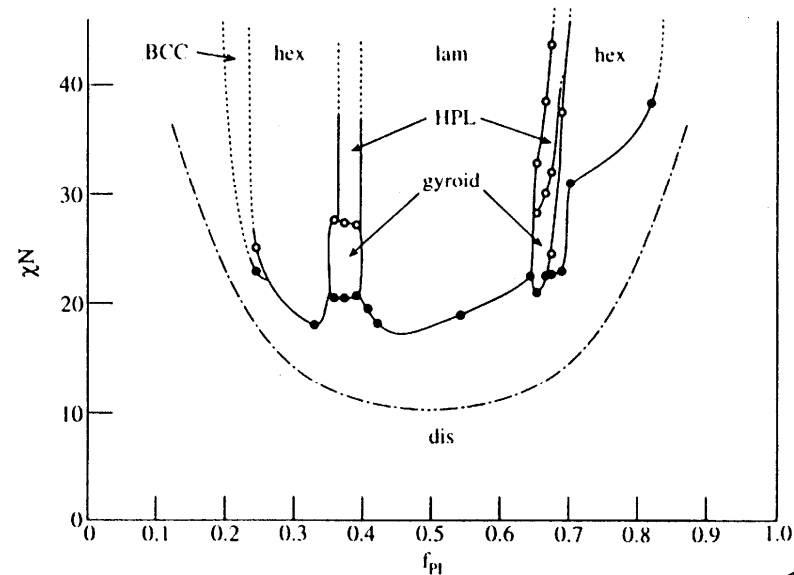
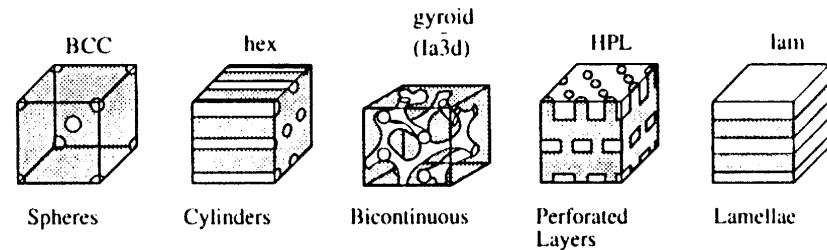


Microphase Separation of Diblock Copolymers (BCPs)

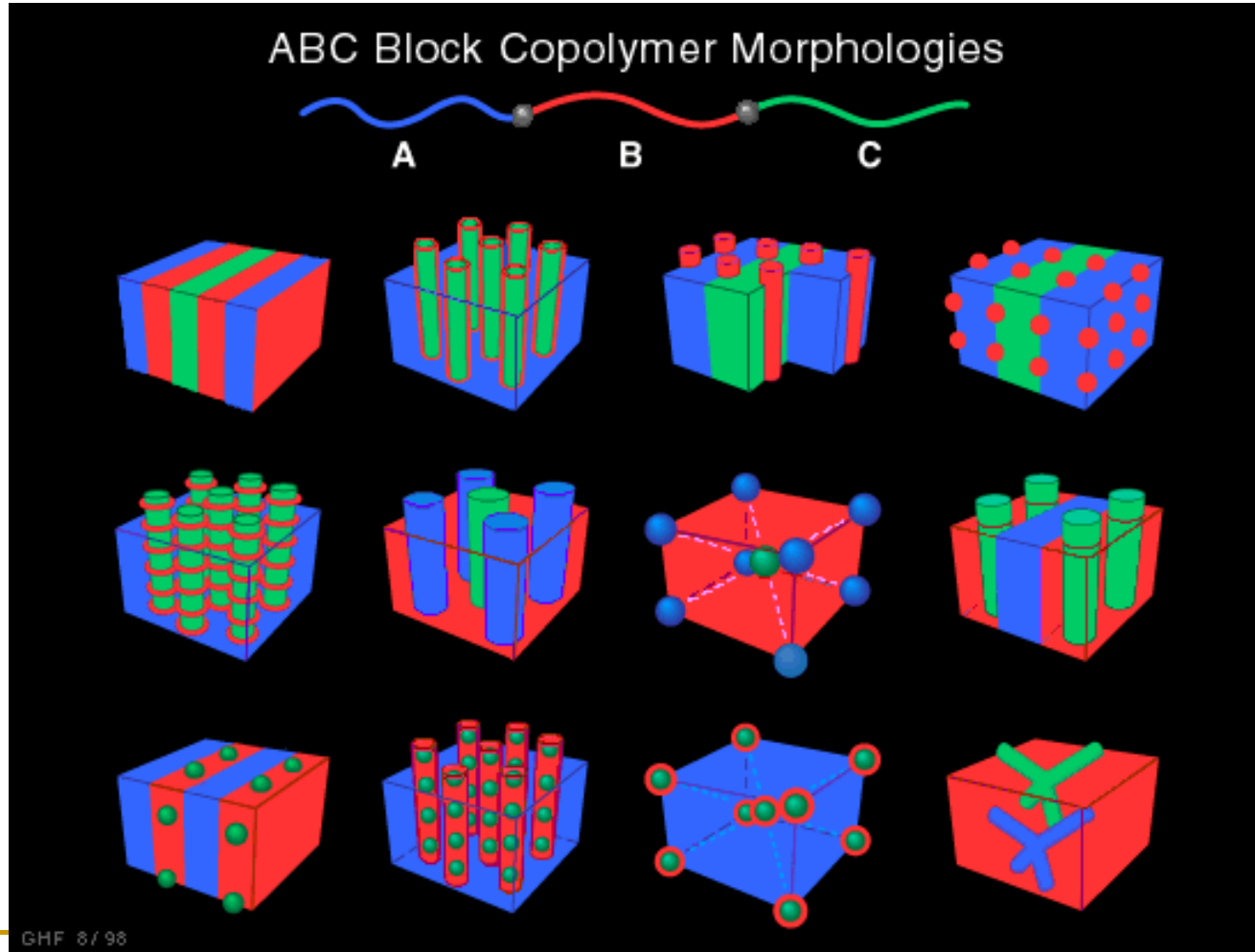
➤ Phase diagram



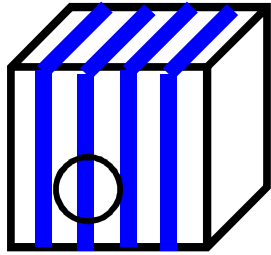
- f is the volume fraction of one component. f controls which ordered structures are accessed beneath the order-disorder transition.
- χN expresses the enthalpic-entropic balance. It is used to parameterize block copolymer phase behavior, along with the composition of the copolymer.



Microphase Separation of Triblock Copolymers

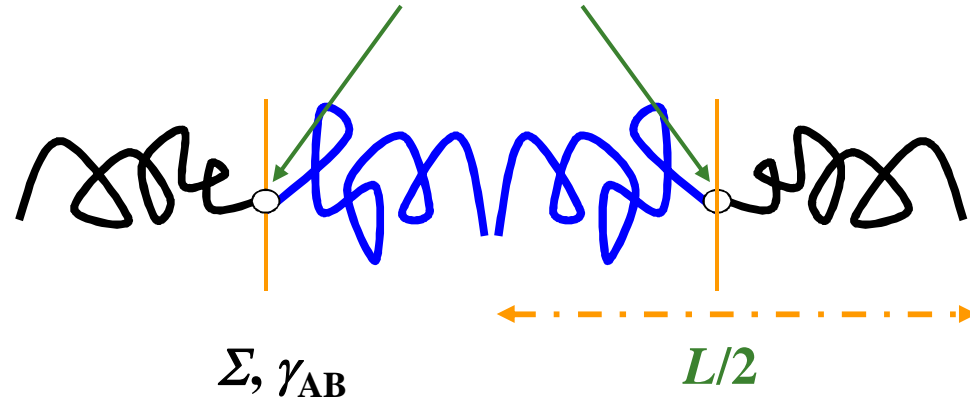


Thermodynamics of Microphase Separation



Lamellar structure

- **Minimize interfacial area and Maximize chain conformational entropy (MIN-MAX Principle)**



F : free energy per chain

N : number of segments ($=N_A + N_B$)

b : Kuhn length $\nu_b \sim b^3, b_A \sim b_B$

L : domain periodicity

Σ : interfacial area per chain

γ_{AB} : interfacial energy per area

χ_{AB} : segment-segment interaction parameter

$$\gamma_{AB} = \frac{kT}{b^2} \sqrt{\frac{\chi_{AB}}{6}}$$

$$\chi_{AB} = \frac{Z-2}{kT} \left(\epsilon_{AB} - \frac{1}{2} (\epsilon_{AA} + \epsilon_{BB}) \right) \quad \text{or} \quad \chi_{AB} \approx \frac{A}{T} + B$$

Thermodynamics of Microphase Separation

➤ **Free energy of lamellae:** $F_{LAM} = \underbrace{\gamma_{AB}\Sigma}_{\text{enthalpic term}} + \underbrace{\frac{3}{2}kT \frac{(L/2)^2}{Nb^2}}_{\text{entropic spring term}}$ See [Appendix](#)

Using $Nb^3 = V = \frac{L}{2}\Sigma$

we have $F_{LAM} = \frac{kT}{b^2} \sqrt{\frac{\chi_{AB}}{6} \frac{Nb^3}{(L/2)}} + \frac{3}{2}kT \frac{(L/2)^2}{Nb^2} = \frac{\alpha}{L} + L^2\beta$

$$\frac{\partial F_{LAM}}{\partial L} = 0 \longrightarrow -\frac{\alpha}{L_{opt}^2} + 2L_{opt}\beta = 0$$

Thus, the optimum period of the lamellae and the lamellar free energy are:

$$L_{opt} = \sqrt[3]{\frac{\alpha}{2\beta}} \cong bN^{2/3} \chi_{AB}^{1/6} \quad \text{and} \quad F_{LAM}(L_{opt}) = \frac{\alpha}{L_{opt}} + L_{opt}^2\beta \quad F_{LAM} \cong 1.2kTN^{1/3} \chi_{AB}^{1/3}$$

Assume $F_{disorder} \approx \frac{\widetilde{V}_m}{\widetilde{V}} \chi_{AB} \phi_A \phi_B kT = N \chi_{AB} \phi_A \phi_B kT$

At the order-disorder transition: $F_{LAM} = F_{disordered}$

For a 50/50 volume fraction, $\phi_A \phi_B = 1/4$, so: $-1.2kTN^{1/3} \chi_{AB}^{1/3} = \frac{1}{4} N \chi_{AB} kT$

BCPs $(\chi N)_c = (4.8)^{3/2} \sim 10.5$

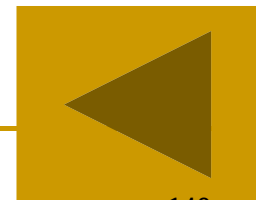
Critical point Symmetric blends

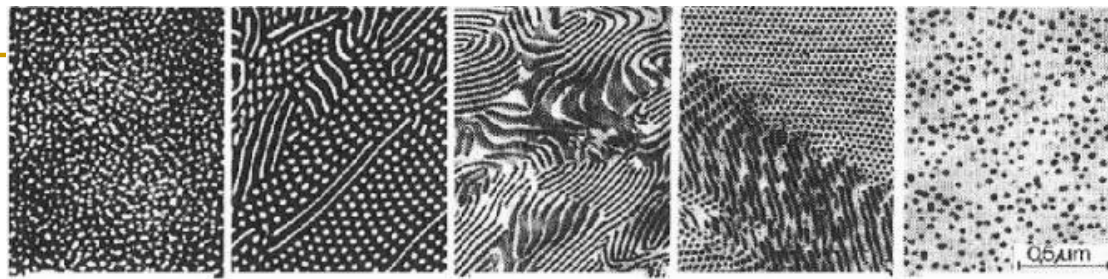
$\chi_c N = 2$

Appendix

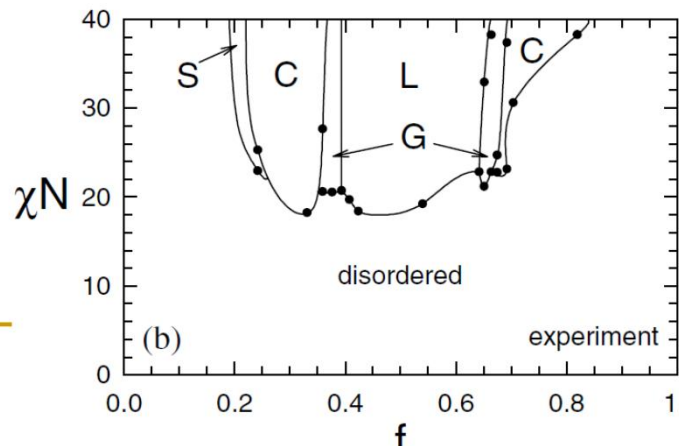
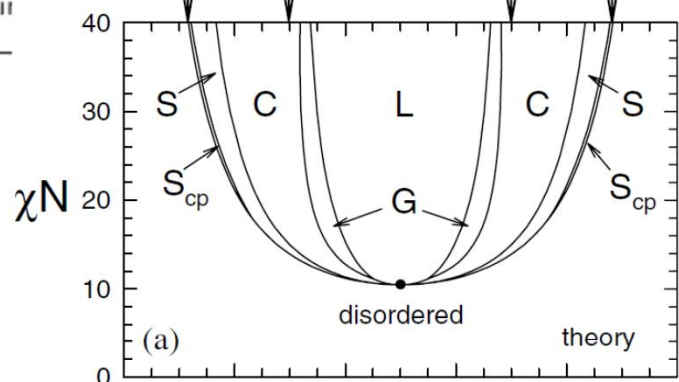
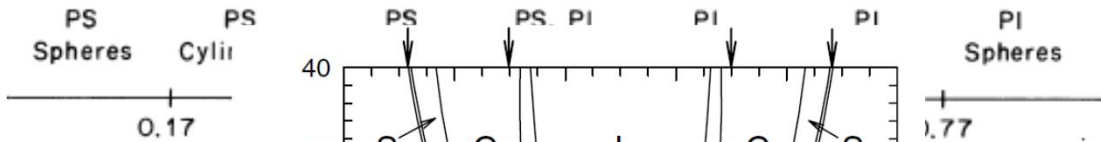
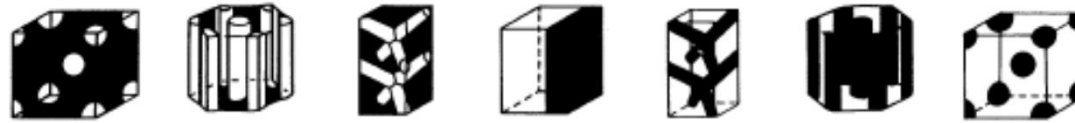
$$\begin{aligned} S_{el}(h) &= k \ln \Omega = k \ln \Phi(h, N) \int \Phi(h, N) dh \approx k \ln \left[\left(\frac{3}{2\pi Nb^2} \right)^{3/2} \exp\left(-\frac{3h^2}{2Nb^2} \right) \right] \\ &= k \ln \left(\frac{3}{2\pi Nb^2} \right)^{3/2} + k \ln \left[\exp\left(-\frac{3h^2}{2Nb^2} \right) \right] \\ &= -k \frac{3h^2}{2Nb^2} + \text{const.} \end{aligned}$$

$$F_{el}(h = L/2) = \frac{3}{2} kT \frac{(L/2)^2 - Nb^2}{Nb^2} = \frac{3}{2} kT \left(\frac{(L/2)^2}{Nb^2} - 1 \right) \approx \frac{3}{2} kT \frac{(L/2)^2}{Nb^2}$$





A Spheres 0-20% A
 A Cylinders 20-40% A
 Lamellae 40-64% A
 B Cylinders 64-84% A
 B Spheres >84% A



总结: 结构层次

链段(segment)

$$l_e = h_0^2 / L$$

热串滴 (Thermal Blob)

$$g_T \approx \left(\frac{u}{l^3}\right)^{-2} \quad \xi_T \approx \left(\frac{u}{l^3}\right)^{-1} l \quad \bar{E} \approx kT g_T^2 \frac{u}{\xi_T^3} \approx k_B T$$

单链(Single Chain)和稀溶液 $h = N^\nu l_e$

亚浓溶液

从热串滴到大串滴(相关长度)再到链

浓溶液, θ 溶液和熔体

嵌段共聚物

共混物

从自由能到化学势

高分子链构象的重要作用

高斯链模型代表构象熵的最大状态，高分子链总是要尽可能地实现这种构象熵的最大状态。溶液中链构象状态的实现概率要通过焓与构象熵最大化效应两者之间的竞争和平衡来决定。

χ 参数的重要作用

- (1) 溶液中链的构象(χ 与构象熵的相互制约)
- (2) 凝胶的体积相变(χ 与混合熵、构象熵的相互制约)
- (3) 高分子溶液和共混物的相平衡和相分离(χ 与混合熵的相互制约)
- (4) 高分子混合界面 (与 χ 有关的界面能与构象熵的相互制约)
- ~~(5) 高分子嵌段共聚物的微相分离 (与 χ 有关的界面能与构象熵的相互制约)~~

高分子溶液热力学

$$\Delta G = \Delta H - T\Delta S \quad \frac{\partial \Delta G}{\partial h} = 0 \quad \text{or} \quad \Delta G = 0$$

焓

排斥体积

熵

高斯链:

$$H = 0$$

$$\ln P(h) = 0$$

$$S_{conf} = -\frac{3}{2}k_B \frac{h^2}{xl^2}$$

稀溶液:

良溶剂, θ 溶剂

$$H = -\frac{x^2 v_c}{h^3} \chi$$

$$\ln P(h) \approx -\frac{x^2 v_c}{2h^3}$$

$$S_{conf} = -\frac{3}{2}k_B \frac{h^2}{xl^2}$$

不良溶剂

$$H/h^3 \sim \left[-\frac{\chi}{v_c} \left(\frac{xv_c}{h^3} \right)^2 + w \left(\frac{xv_v}{h^3} \right)^3 \right]$$

构象熵可忽略

$$S_{conf} \approx 0$$

三体相互作用

也可用标度理论+blob model处理

亚浓溶液:

两体 + 三体相互作用

排斥体积部分屏蔽

$$S_{conf} = -\frac{3}{2}k_B \frac{h^2}{xl^2}$$

只能用标度理论+blob model处理

焓 熵

聚电解质:

or

$$H_{electr}(R_e) \approx k_B T \frac{l_B (fN)^2}{R_e} \quad (\text{圆球})$$

$$H_{electr}(R_e) \approx k_B T \frac{l_B (fN)^2}{R_e} \ln \left(\frac{R_e}{N^{1/2} b} \right) \quad (\text{椭球})$$

$$S = -\frac{3}{2} k_B \frac{h^2}{Nl^2}$$

良溶剂下 χ 相互作用可忽略 排斥体积作用可忽略

浓溶液: $\Delta H_M = k_B T \frac{V_m}{V_s} \chi \phi_1 \phi_2$ 排斥体积被屏蔽 $\Delta S_M = -k_B \frac{V_m}{V_s} \left(\frac{\phi_1}{x_1} \ln \phi_1 + \frac{\phi_2}{x_2} \ln \phi_2 \right)$

$\Delta S_{conf} = 0$

Flory-Huggins Theory

凝胶: $\Delta H_M = k_B T \frac{V_m}{V_s} \chi \phi_1 \phi_2$ $\Delta S = -k_B \frac{V_m}{V_s} \left(\frac{\phi_1}{1} \ln \phi_1 + \frac{\phi_2}{x} \ln \phi_2 \right)$

$$-\frac{3}{2} N_0 k_B \frac{\Delta(h^2)}{h_0^2} \quad N_0: \text{单位体积内的网链数目}$$

高分子共混物和嵌段共聚物热力学

共混物:

$$\Delta H_M = k_B T \frac{V_m}{V_s} \chi \phi_1 \phi_2 \quad \Delta S_M = -k_B \frac{V_m}{V_s} \left(\frac{\phi_1}{x_1} \ln \phi_1 + \frac{\phi_2}{x_2} \ln \phi_2 \right) \quad \Delta S_{conf} = 0$$

$$\Delta G_M = \Delta H_M - T \Delta S_M \quad \rightarrow \quad \Delta \mu_{i,1} = \Delta \mu_{i,2} \quad i = 1, 2 \quad \text{Phase equilibrium (binodal)}$$

Phase Diagram

$$\frac{\partial^2 \Delta G_M}{\partial \phi^2} = 0$$

Phase stability (spinodal)

$$\frac{\partial^3 \Delta G_M}{\partial \phi^3} = 0$$

Critical Point

对称的嵌段共聚物:

$$\text{Symmetric Blends: } \chi_c N = 2 \quad \text{Solutions: } \chi_c = 1/2$$

$$\text{有序相: } \Delta H_{interface} = \gamma_{AB} \Sigma \quad \Delta S_{conf} \approx -\frac{3}{2} kT \frac{(L/2)^2}{Na^2} \frac{\partial \Delta F}{\partial L} = 0 \quad \rightarrow \quad L_{opt}$$

$$\text{无序相: } \Delta H \approx \frac{\tilde{V}_m}{V_s} \chi_{AB} \phi_A \phi_B kT = N \chi_{AB} \phi_A \phi_B kT \quad \Delta S_{conf} \approx 0$$

$$\text{相平衡: } \quad \rightarrow \quad \Delta F_{disorder} = \Delta F_{order} \quad \rightarrow \quad \text{Critical Point: } \chi_c N = 10.5$$